

Catalogue

# Check valves for Industrial Refrigeration

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# Check & stop valve, SCA-X, 52 bar (754 psi) Check valve, CHV-X, 52 bar (754 psi)

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## Check & stop valve, SCA-X, 52 bar (754 psi) Check valve, CHV-X, 52 bar (754 psi)



SCA-X are check valves with a built-in shut-off valve function. SCA-X valves are available in angleway versions.

CHV-X are check valves only. CHV-X are available in both angleway and straightway versions.

The valves are designed to open at very low differential pressures, allow favourable flow conditions and are easy to disassemble for inspection and service.

The SCA-X is equipped with vented cap and has internal backseating enabling the spindle seal to be replaced whilst the valve still under pressure.

Laser cut V-ports provide excellent opening characteristics (SCA-X/CHV-X 50-125).

The valve cone has a built-in flexibility to ensure a precise and tight closing towards the valve seat.

A well balanced dampening effect between the piston and the cylinder gives an optimal protection during low loads and against pulsations.

### Features

- Applicable to HCFC, HFC, R717 (Ammonia), R744 (CO<sub>2</sub>), Propane, Butane, Iso-Butane and Ethane.  
R717 Heat Pump and Propylene applications with replaced O-ring.
- Modular Concept:
  - Each valve housing is available with several different connection types and sizes.
  - Possible to convert SCA-X or CHV-X to any other product in the Flexline™ SVL family (Hand operated regulating valve, shut-off valve or strainer) just by replacing the complete top part.
- Fast and easy valve overhaul service. It is easy to replace the top part and no welding is needed.
- Designed to open at a very low differential pressure of 0.04 bar / 0.58 psig.
- Designed with a built-in damping chamber preventing valve flutter in case of low refrigerant velocity and/or low density.
- Each valve is clearly marked with type, size and performance range.  
Additional ID ring to be installed when preparing for Ammonia Heat Pump or Propylene application.
- Easy to disassemble for inspection and service.
- Internal backseating enables replacement of the spindle seal whilst the valve is active, i.e. under pressure.
- Optimal flow characteristics ensuring quick opening to the fully open position.
- Protection against pulsation by built-in damping facility.
- Housing and bonnet material is low temperature steel according to requirements of the Pressure Equipment Directive and other international classification authorities.
- Equipped with Stainless steel bolts.
- Max. working pressure:  
52 bar g / 754 psi g
- Temperature range:  
-60 – 150 °C / -76 – 302 °F
- Classification: DNV, CRN, BV, EAC etc.  
To get an updated list of certification on the products please contact your local Danfoss Sales Company.

Check & stop valve, type SCA-X, 52 bar (754 psi) - Check valve, type CHV-X, 52 bar (754 psi)

**Design**

*Connections*

Available with the following connections:

- Butt-weld DIN (EN 10220)  
DN 15 - 125 (½ - 5 in.)
- Butt-weld ANSI (B 36.10 Schedule 80),  
DN 15 - 40 (½ - 1½ in.)
- Butt-weld ANSI (B 36.10 Schedule 40),  
DN 50 - 125 (2 - 5 in.)
- Butt-weld GOST, (8734-75 and 8732-78)  
DN 15 - 125 (½ - 5 in.)
- Socket-weld ANSI (B 16.11),  
DN 50 (2 in.)

*Housing*

The housing is made from special, cold resistant steel.

*Valve cone*

Valve cone with built in metallic stop - prevents damage to teflon ring in case of overtightening.

*Damping chamber*

The chamber is filled with refrigerants (gas or liquid), which provides a damping effect when the valve opens and closes.

*Spindle (SCA-X)*

Made of polished stainless steel, which is ideal for O-ring sealing.

*Packing Gland (SCA-X)*

The "full temperature range" packing gland is the standard for the entire SVL platform.

This ensures perfect tightness throughout the whole temperature range:  
-60/+150°C (-76/+302°F).

*Pressure Equipment Directive (PED)*

The SCA-X/CHV-X valves are approved according to the European standard specified in the Pressure Equipment Directive and are CE marked.

For further details / restrictions - see the product instruction.

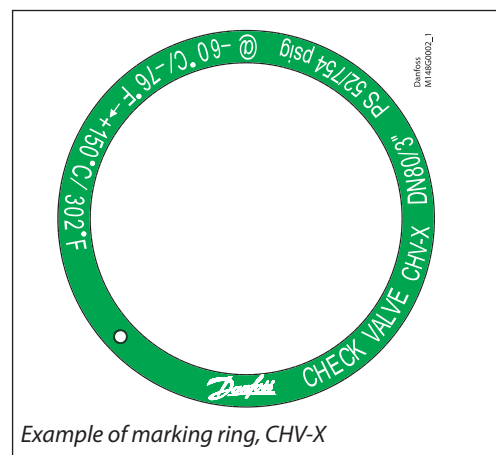
*Installation*

The valve must be mounted vertically with the cone downwards.

The valve is designed to resist very high internal pressure. However, the piping system in general should be designed to avoid liquid traps and reduce the risk of hydraulic pressure caused by thermal expansion.

For further information refer to installation instructions for SCA-X/CHV-X.

If cold refrigeration oil having low viscosity enters and settles in the damping chamber, problems with the check valve may arise. Consequently, it may be necessary to modify the valve for more viscous liquids by enlarging the hole to the damping chamber.



SCA-X/CHV-X valves			
Nominal bore	DN = < 25 mm (1 in.)	DN32-80 mm (1¼ - 3 in.)	DN100 - 125 mm (4 - 5 in.)
Classified for	Fluid group I		
Category	Article 3, paragraph 3	II	III

**Application**

Figure 3 shows the check & stop valve SCA-X in the discharge line of a screw compressor unit. The SCA-X valve in the discharge line prevents "back condensation" in the oil separator as well as pressure equalising through the compressor.

Compared to an ordinary shut-off and check valve arrangement the combined check & stop valve solution, as shown, is easier to install and has lower flow resistance.

Installation of the SCA-X/CHV-X in the economizer line is **not** recommended.

For horizontal installation of the function module; please contact Danfoss.

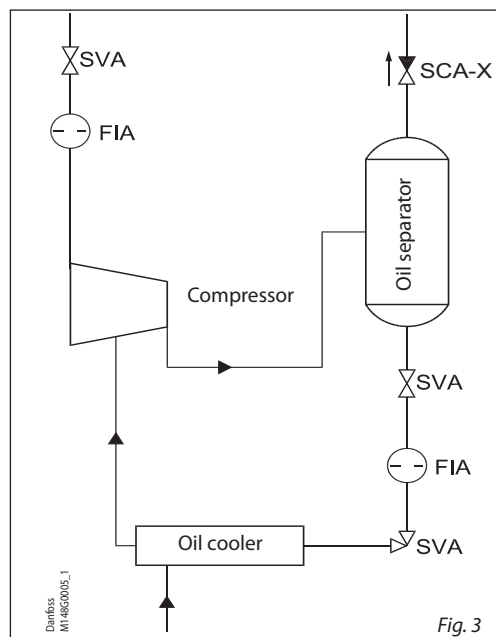


Fig. 3

Check & stop valve, type SCA-X, 52 bar (754 psi) - Check valve, type CHV-X, 52 bar (754 psi)

**Technical data**

- *Refrigerants*  
Applicable to HCFC, HFC, R717 (Ammonia), R744 (CO<sub>2</sub>), Propane, Butane, Iso-Butane and Ethane.  
R717 Heat Pump and Propylene applications with replaced O-ring.
- *Temperature range*  
-60 – 150 °C / -76 – 302 °F.
- *Max. working pressure*  
52 bar g / 754 psig.

**Computation and selection**

*Introduction*

When dimensioning SCA-X/CHV-X, it is important to select a valve that is best suited to all operating conditions. Therefore, it is necessary to consider both the nominal and part load working conditions.

The SCA-X/CHV-X valve can be calculated in two ways:

- Using the tables below.
- Using Coolselector®2

*Example*

*SI-Units*

Assumed working conditions:  
Maximum flow  $\dot{V} = 1000 \text{ m}^3/\text{h}$   
Density  $\rho = 3.0 \text{ kg/m}^3$   
Minimum part load = 33%

*US-Units*

Assumed working conditions:  
Maximum flow  $\dot{V} = 1160 \text{ gpm}$   
Density  $\rho = 0.187 \text{ lb/ft}^3$   
Minimum part load = 33%

Used expressions:

- Recommended velocity -  $C_{rec}$  [m/s]
- Minimum recommended velocity -  $C_{min, rec}$  [m/s]
- Maximum velocity -  $C_{max}$  [m/s]
- Part load velocity -  $C_{part}$  [m/s]

Used expressions:

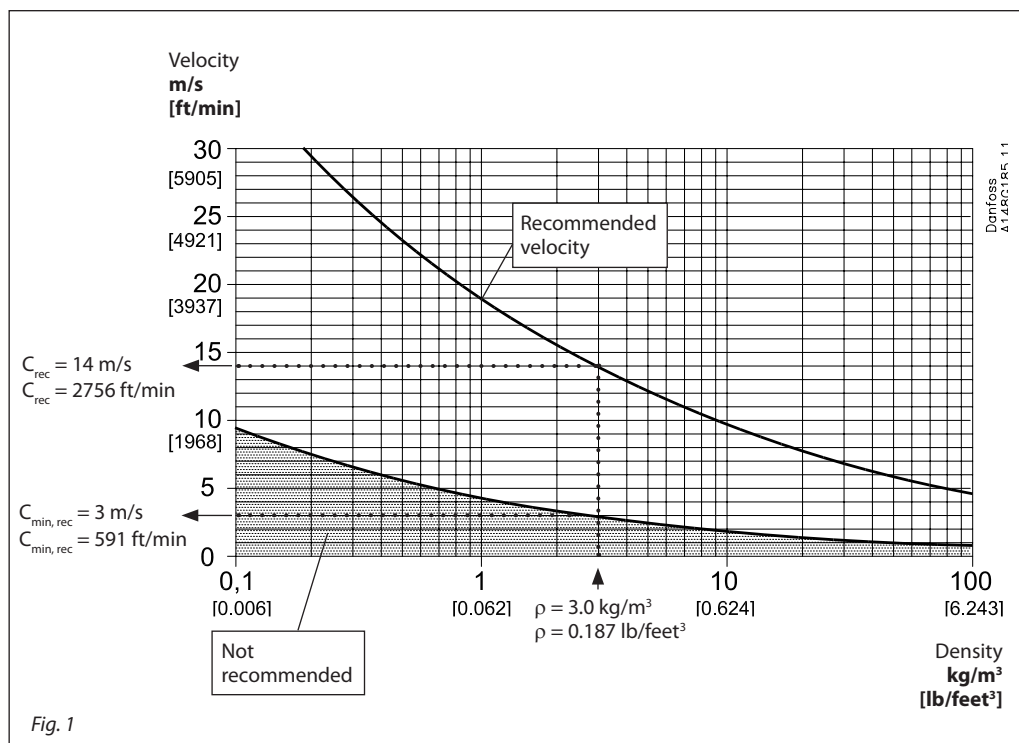
- Recommended velocity -  $C_{rec}$  [ft/min]
- Minimum recommended velocity -  $C_{min, rec}$  [ft/min]
- Maximum velocity -  $C_{max}$  [ft/min]
- Part load velocity -  $C_{part}$  [ft/min]

We know the density  $\rho \approx 3.0 \text{ kg/m}^3$ , consequently  $C_{rec}$  as well as  $C_{min, rec}$  can be found in the figure below (standard valve).

We know the density  $\rho \approx 0.187 \text{ lb/ft}^3$ , consequently  $C_{rec}$  as well as  $C_{min, rec}$  can be found in the figure (standard valve).

$C_{rec} \approx 14 \text{ m/s}$   
 $C_{min, rec} \approx 3 \text{ m/s}$

$C_{rec} \approx 2756 \text{ ft/min}$   
 $C_{min, rec} \approx 591 \text{ ft/min}$



Selection example continued on following page.

Check & stop valve, type SCA-X, 52 bar (754 psi) - Check valve, type CHV-X, 52 bar (754 psi)

**Computation and selection**  
(continued)

Knowing that  $\dot{V} = 1000 \text{ m}^3/\text{h}$  (1160 gpm) fig. 2 gives the following choices:

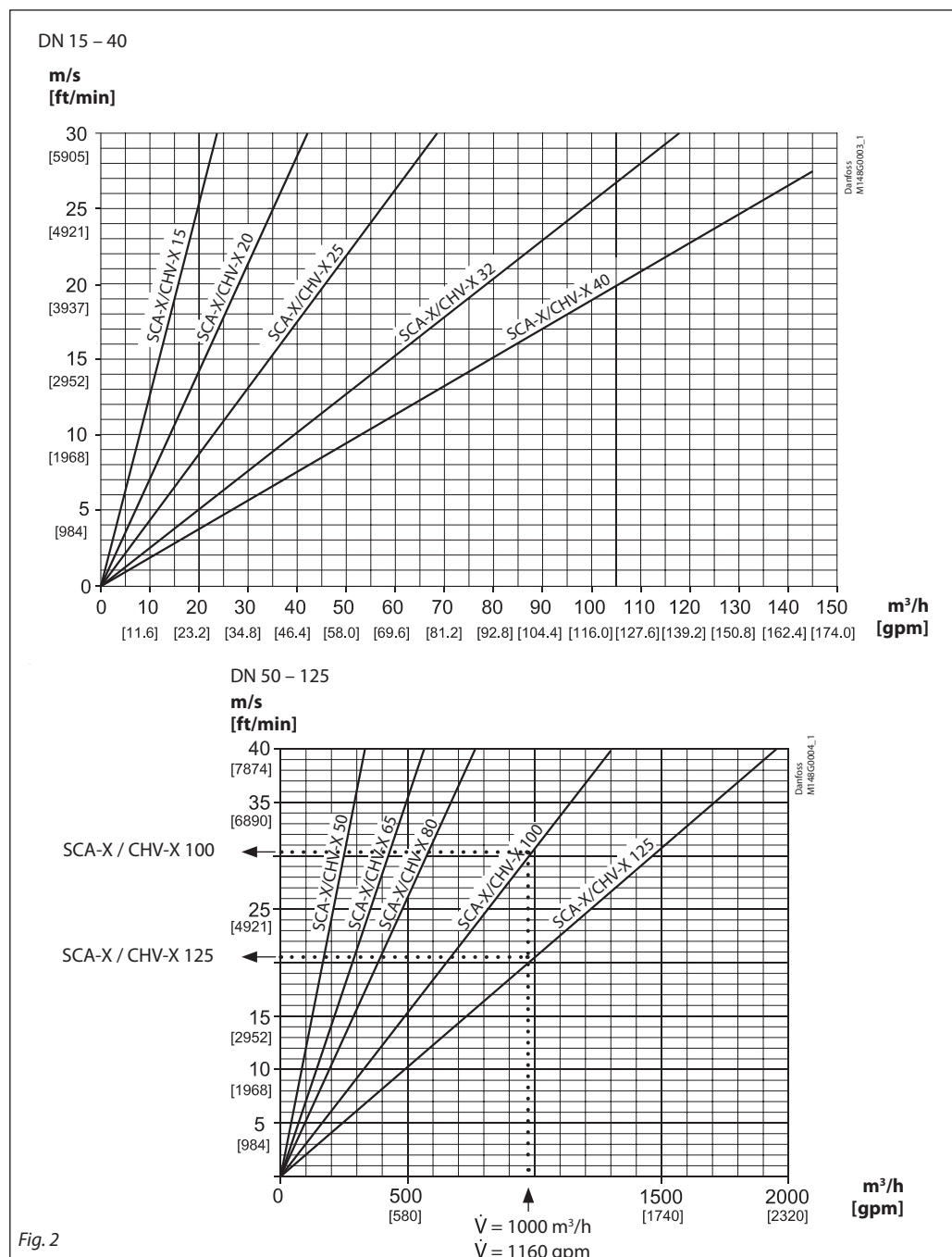
For SCA-X / CHV-X in size DN 100 the maximum velocity  $C_{\text{max}} \approx 31 \text{ m/s}$  (6100 ft/min)

For SCA-X / CHV-X in size DN 125 the maximum velocity  $C_{\text{max}} \approx 20 \text{ m/s}$  (3900 ft/min)

In conclusion SCA-X in size DN 125 is selected because  $C_{\text{max}} \approx 20 \text{ m/s}$  (3900 ft/min) comes nearest to the recommended velocity  $C_{\text{rec}} \approx 14 \text{ m/s}$  (2756 ft/min) and at the same time part load conditions fulfil the requirements, as described:

If the valve in question (for instance under part load conditions) provides a velocity less than  $C_{\text{min, rec}}$  the valve might start hammering and become noisy. As a result the valve may wear prematurely.

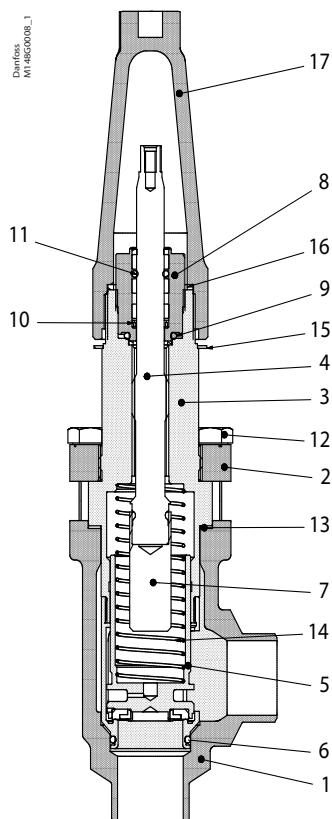
We know that  $C_{\text{max}} \approx 20 \text{ m/s}$  (3900 ft/min) and that minimum part load is 33%. It follows that  $C_{\text{part}} \approx 6.5 \text{ m/s}$  (1290 ft/min). Thus,  $C_{\text{part}}$  (6.5 m/s) >  $C_{\text{min, rec}}$  (3.0 m/s) and the selected SCA-X model DN125 is the perfect choice.



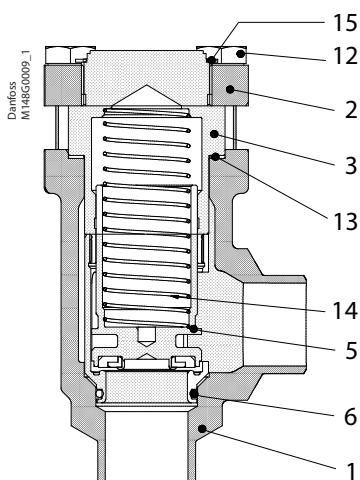


Check & stop valve, type SCA-X, 52 bar (754 psi) - Check valve, type CHV-X, 52 bar (754 psi)

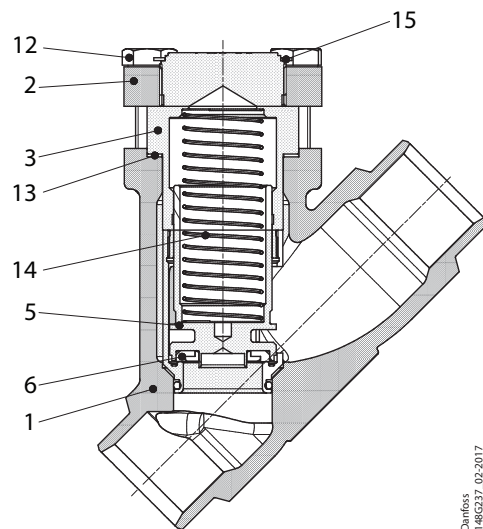
Material specification



SCA-X 15 - 40



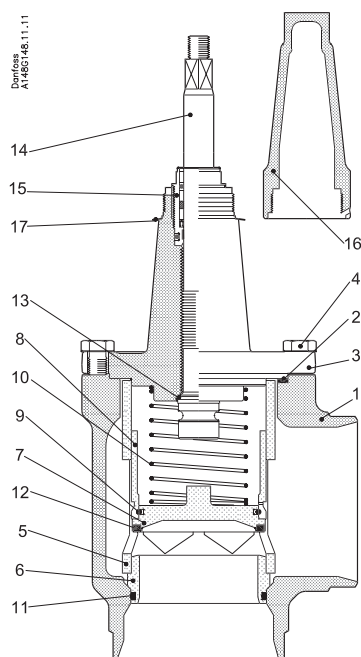
CHV-X 15 - 40



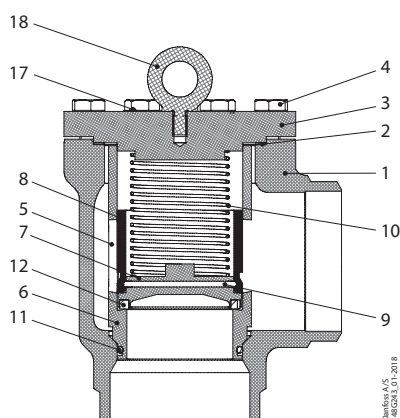
CHV-X 15 - 40

No.	Part	Material	DIN/EN	ISO	ASTM
1	Housing	Steel	P285QH EN10222-4		LF2A350
2	Bonnet, Flange	Steel	P275NL1 EN10028-3		
3	Bonnet, Insert	Steel			
4	Spindle	Stainless steel	X 10CrNiS18-9	Type 17, 17440	AISI 303, 683/13
5	Cone	Steel Teflon (PTFE)			
6	O-ring	Cloroprene (Neoprene)			
7	Spindle extension	Steel			
8	Packing gland O-rings	Steel Cloroprene (Neoprene)			
9	Packing washer	Aluminium			
10	Spring loaded seal	Teflon (PTFE)			
11	O-ring	Cloroprene (Neoprene)			
12	Bolts	Stainless steel	A2-70	A2-70	Type 308
13	Gasket	Fiber, non-asbestos			
14	Spring	Steel			
15	Identification ring	Stainless steel			
16	Seal cap gasket	Nylon			
17	Spindle seal cap	Aluminium			

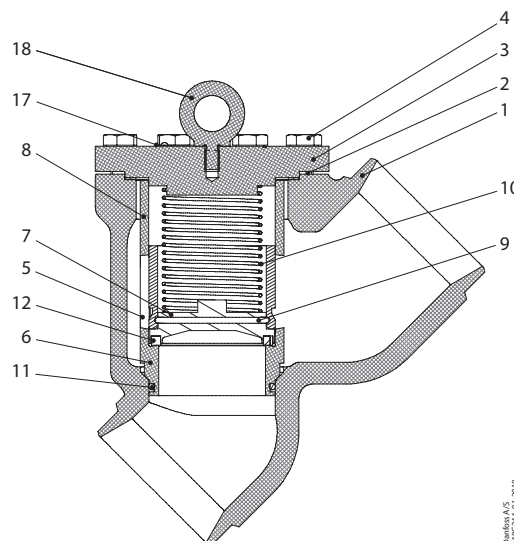
**Material specification**



SCA-X 50 - 125



CHV-X 50 - 125



CHV-X 50 - 125

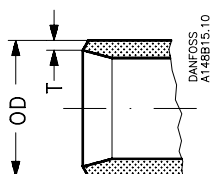
No.	Part	Material	DIN/EN	ISO	ASTM
1	Housing DN 50-65	Steel	P285 QH EN 10222-4		LF2A350
	Housing DN 80-125	Steel	G20Mn5 QT SEW 685		LCC, A352
2	Gasket	Fiber, Non-asbestos			
3	SCA-X: Valve bonnet CHV-X: End cover	Steel	P285 QH EN 10222-4		LF2A350
4	Bolts	Stainless steel	A2-70	A2-70	A-276
5	Tube	Steel			
6	Seat	Steel			
7	Valve plate	Steel			
8	Guide sleeve	Steel			
9	Spring ring	Steel			
10	Spring	Steel			
11	O-ring	Cloroprene (Neoprene)			
12	Teflon ring	Teflon (PTFE)			
13	Soft back seal	Teflon (PTFE)			
14	Spindle DN 50-65	Stainless steel	X8CrNiS18-9 17440	Type 17 R 683/13	AISI 303
	Spindle DN 80-125	Stainless steel	X5CrNi1810 17440	Type 11 683/13	AISI 304 A-276
15	Packing gland	Steel	9Mn28, 1651	Type 2, R 683/9	1213, SAE J403
16	Spindle seal cap and gasket	Aluminium			
17	Marking label	Stainless steel			
18	Eye bolt DIN 580	Steel			

Check & stop valve, type SCA-X, 52 bar (754 psi) - Check valve, type CHV-X, 52 bar (754 psi)

Connections

Size mm	Size in.	OD mm	T mm	OD in.	T in.			$k_v$ Angleway m <sup>3</sup> /h	$C_v$ Angleway USgal/min	$K_v$ Straightway m <sup>3</sup> /h	$C_v$ Straightway USgal/min
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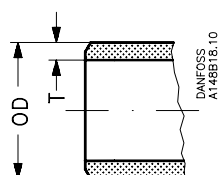
DIN



Butt-weld DIN (EN 10220)

15	1/2	21.3	2.3	0.839	0.091			8	9.3	4	4.6
20	3/4	26.9	2.3	1.059	0.091			10	11.6	7	8.1
25	1	33.7	2.6	1.327	0.102			24	27.8	16	18.6
32	1 1/4	42.4	2.6	1.669	0.102			30	34.8	21	24.4
40	1 1/2	48.3	2.6	1.902	0.102			30	34.8	21	24.4
50	2	60.3	2.9	2.37	0.11			45	53	28	34
65	2 1/2	76.1	2.9	3.00	0.11			72	85	41	48
80	3	88.9	3.2	3.50	0.13			103	129	81	94
100	4	114.3	3.6	4.50	0.14			196	232	157	182
125	5	139.7	4.0	5.50	0.16			301	356	250	290

ANSI



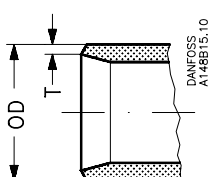
Butt-weld ANSI (B 36.10 Schedule 80)

15	1/2	21.3	3.7	0.839	0.146			8	9.3	4	4.6
20	3/4	26.9	4.0	1.059	0.158			10	11.6	7	8.1
25	1	33.7	4.6	1.327	0.181			24	27.8	16	18.6
32	1 1/4	42.4	4.9	1.669	0.193			30	34.8	21	24.4
40	1 1/2	48.3	5.1	1.902	0.201			30	34.8	21	24.4

Butt-weld ANSI (B 36.10 Schedule 40)

50	2	60.3	3.9	2.37	0.15			45	53	28	34
65	2 1/2	73.0	5.2	2.87	0.20			72	85	41	48
80	3	88.9	5.5	3.50	0.22			103	129	81	94
100	4	114.3	6.0	4.50	0.24			196	232	157	182
125	5	141.3	6.6	5.56	0.26			301	356	250	290

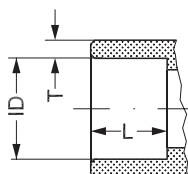
GOST



Butt-weld GOST (8734-75 and 8732-78)

15	1/2	18	2	0.709	0.079			8	9.3	4	4.6
20	3/4	25	2.5	0.984	0.098			10	11.6	7	8.1
25	1	32	3	1.260	0.118			24	28.8	16	18.6
32	1 1/4	38	3	1.496	0.118			30	49.4	21	24.4
40	1 1/2	45	3	1.772	0.118			30	52.4	21	24.4
50	2	57	3.5	2.244	0.138			45	53	28	34
65	2 1/2	76.1	2.9	3	0.11			72	85	41	48
80	3	88.9	3.2	3.50	0.13			103	129	81	94
100	4	108	4	4.252	0.157			196	232	157	182
125	5	133	4	5.236	0.157			301	356	250	290

SOC



Size mm	Size in.	ID mm	T mm	ID in.	T in.	L mm	L in.				
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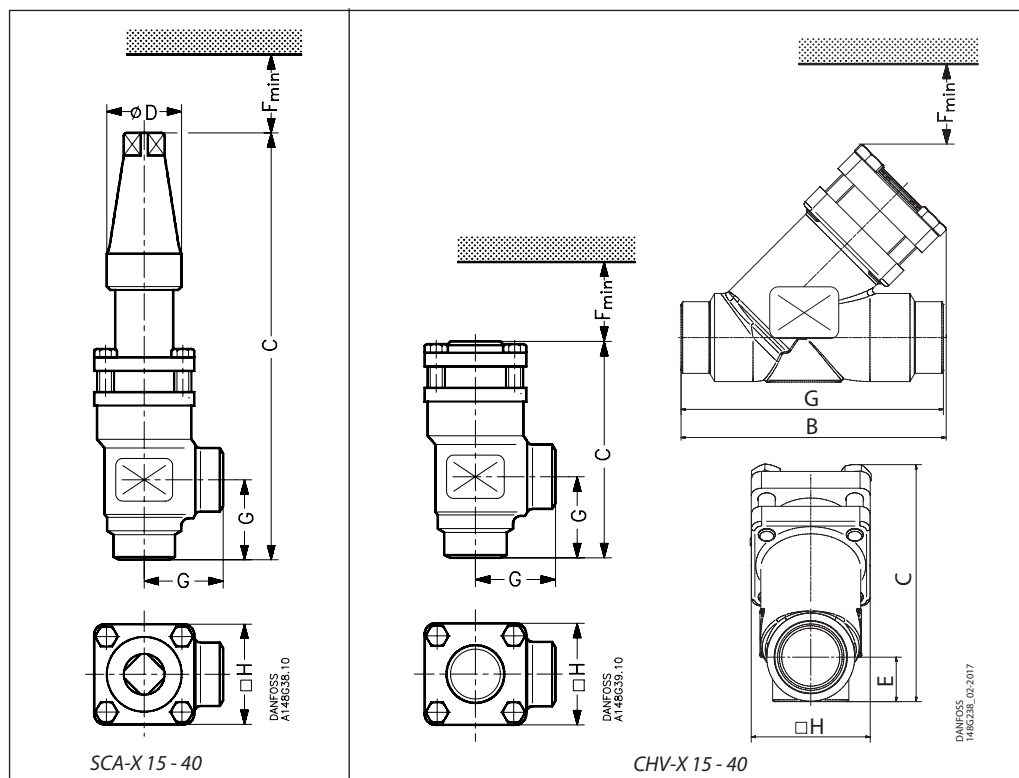
Socket welding ANSI (B 16.11)

15	1/2	21.8	6	0.858	0.235	10	0.39				
20	3/4	27.2	4.6	1.071	0.181	13	0.51				
25	1	33.9	7.2	1.335	0.284	13	0.51				
32	1 1/4	42.7	6.1	1.743	0.240	13	0.51				
40	1 1/2	48.8	6.6	1.921	0.260	13	0.51				
50	2	61.2	6.2	2.41	0.24	16	0.63				

Check & stop valve, type SCA-X, 52 bar (754 psi) - Check valve, type CHV-X, 52 bar (754 psi)

Dimensions and weights

SCA-X/CHV-X 15 - 40 (½- 1½ in.)



Valve size		C	G	ØD	F <sub>min</sub>	□H	Weight
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SCA-X 15 - 40

SCA-X 15 (½ in.)	mm	212	45	38	60	60	1.6 kg
	in.	8.35	1.77	1.50	2.36	2.36	3.53 lb
SCA-X 20 (¾ in.)	mm	212	45	38	60	60	1.6 kg
	in.	8.35	1.77	1.50	2.36	2.36	3.53 lb
SCA-X 25 (1 in.)	mm	295	55	50	85	70	3.2 kg
	in.	11.61	2.17	1.97	3.35	2.76	7.05 lb
SCA-X 32 (1¼ in.)	mm	295	55	50	85	70	3.2 kg
	in.	11.61	2.17	1.97	3.35	2.76	7.05 lb
SCA-X 40 (1½ in.)	mm	295	55	50	85	70	3.2 kg
	in.	11.61	2.17	1.97	3.35	2.76	7.05 lb

CHV-X 15 - 40 Angleway

CHV-X 15 (½ in.)	mm	103	45		60	60	1.2 kg
	in.	4.06	1.77		2.36	2.36	2.65 lb
CHV-X 20 (¾ in.)	mm	103	45		60	60	1.2 kg
	in.	4.06	1.77		2.36	2.36	2.65 lb
CHV-X 25 (1 in.)	mm	143	55		85	70	2.3 kg
	in.	5.63	2.17		3.35	2.76	5.07 lb
CHV-X 32 (1¼ in.)	mm	143	55		85	70	2.3 kg
	in.	5.63	2.17		3.35	2.76	5.07 lb
CHV-X 40 (1½ in.)	mm	143	55		85	70	2.3 kg
	in.	5.63	2.17		3.35	2.76	5.07 lb

Valve size		C	B	E	G	F <sub>min</sub>	□H	Weight
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CHV-X 15 - 40 Straightway

CHV-X 15 (½ in.)	mm	99	114	19	120	60	60	1.3kg
	in.	3.90	4.49	0.75	4.72	2.36	2.36	2.87lb
CHV-X 20 (¾ in.)	mm	99	114	19	120	60	60	1.3kg
	in.	3.90	4.49	0.75	4.72	2.36	2.36	2.87lb
CHV-X 25 (1 in.)	mm	141	157	26	155	85	70	2.6kg
	in.	5.55	6.18	1.02	6.10	3.35	2.76	5.73lb
CHV-X 32 (1¼ in.)	mm	141	157	26	155	85	70	2.6kg
	in.	5.55	6.18	1.02	6.10	3.35	2.76	5.73lb
CHV-X 40 (1½ in.)	mm	141	157	26	155	85	70	2.6kg
	in.	5.55	6.18	1.02	6.10	3.35	2.76	5.73lb

CHV-X 32-40 Straightway, Socket weld

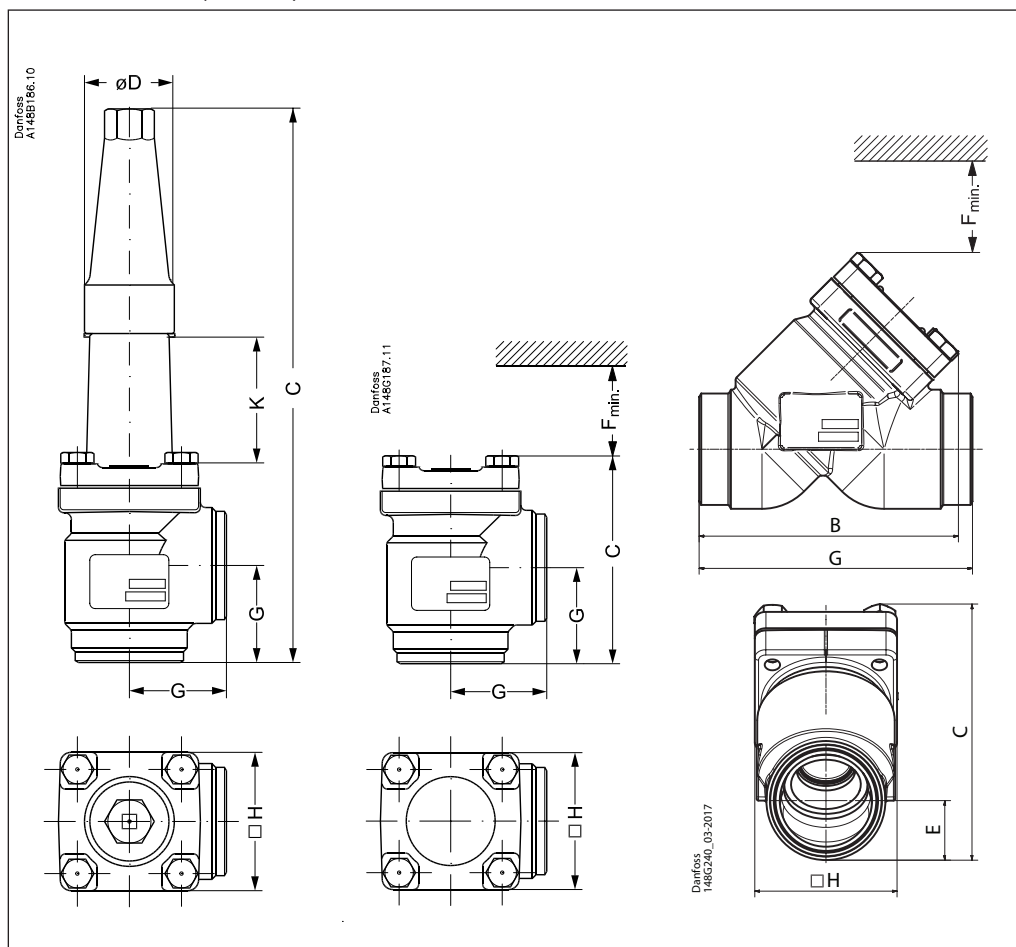
CHV-X 32-40 (1¼ - 1½ in.)	mm	132	156	26	155	85	70	2.8kg
	in.	5.20	6.14	1.02	6.10	3.35	2.76	6.11lb

Specified weights are approximate values only.

Check & stop valve, type SCA-X, 52 bar (754 psi) - Check valve, type CHV-X, 52 bar (754 psi)

Dimensions and weights

SCA-X/CHV-X 50 - 65 (2 - 2½ in.)



Valve size	K	C	G	ØD	□H	Weight
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SCA-X

SCA-X 50	mm	70	315	60	50	77	3.8 kg
SCA-X (2)	in.	2.76	12.40	2.36	1.97	3.03	8.40 lb
SCA-X 65	mm	70	335	70	50	90	5.5 kg
SCA-X (2½)	in.	2.76	13.19	2.76	1.97	3.54	12.16 lb

Valve size	C	G	F <sub>min.</sub>	□H	Weight
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CHV-X Angleway

CHV-X 50	mm	132	60	92	77	3.2 kg
CHV-X (2)	in.	5.20	2.36	3.62	3.03	7.10 lb
CHV-X 65	mm	152	70	107	90	4.5 kg
CHV-X (2½)	in.	5.98	2.76	4.21	3.54	9.95 lb

Valve size	C	B	E	G	F <sub>min.</sub>	□H	Weight
------------	---	---	---	---	-------------------	----	--------

CHV-X Straightway

CHV-X 50	mm	139	140	32	148	92	77	3 kg
CHV-X (2)	in.	5.47	5.51	1.26	5.83	3.62	3.03	6.72 lb
CHV-X 65	mm	163	164	40	176	107	90	4.3 kg
CHV-X (2½)	in.	6,4	6,4	1,6	6,9	4.21	3.54	9.44 lb

CHV-X Straightway, Socket weld

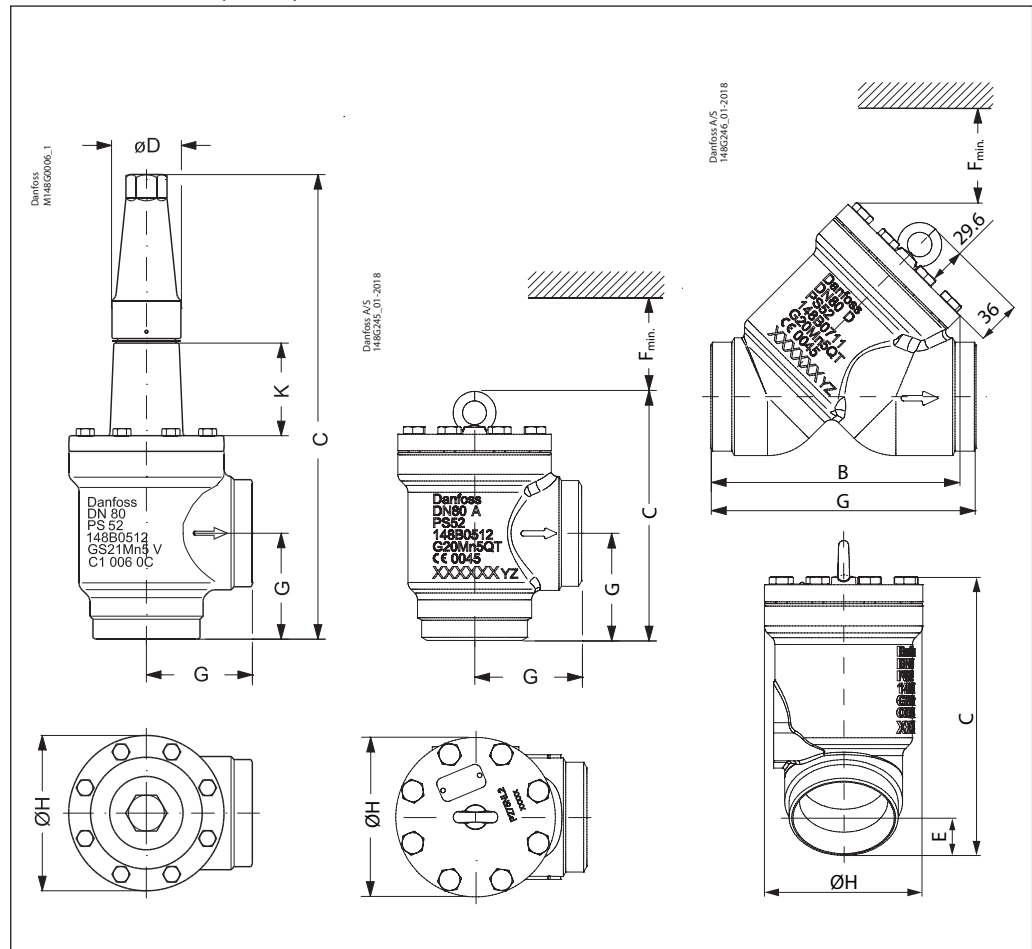
CHV-X 50	mm	142	147	37	162	92	77	3.8 kg
CHV-X (2)	in.	5.59	5.79	1.46	6.38	3.62	3.03	8.33 lb

Specified weights are approximate values only.

Check & stop valve, type SCA-X, 52 bar (754 psi) - Check valve, type CHV-X, 52 bar (754 psi)

Dimensions and weights

SCA-X/CHV-X 80 - 125 (3 - 5 in.)



Valve size	K	C	G	ØD	ØH	Weight
------------	---	---	---	----	----	--------

SCA-X

SCA-X 80	mm	76	388	90	58	129	9.7 kg
SCA-X (3)	in.	3.00	15.28	3.54	2.28	5.08	21.4 lb
SCA-X 100	mm	90	437	106	58	156	15.3 kg
SCA-X (4)	in.	3.54	17.20	4.17	2.28	6.14	33.7 lb
SCA-X 125	mm	90	533	128	74	193	28.1 kg
SCA-X (5)	in.	3.54	20.98	5.04	2.91	7.60	61.9 lb

Valve size	C	G	F <sub>min.</sub>	ØH	Weight
------------	---	---	-------------------	----	--------

CHV-X Angleway

CHV-X 80	mm	218.6	90	103.4	129	8.7 kg
CHV-X (3)	in.	8.61	3.54	4.07	5.08	19.23 lb
CHV-X 100	mm	252.6	106	133.4	156	14.3 kg
CHV-X (4)	in.	9.94	4.17	5.25	6.14	31.60 lb
CHV-X 125	mm	297.6	128	160.4	193	25.6 kg
CHV-X (5)	in.	11.72	5.04	6.31	7.60	56.58 lb

Valve size	C	B	E	G	F <sub>min.</sub>	ØH	Weight
------------	---	---	---	---	-------------------	----	--------

CHV-X Straightway

CHV-X 80	mm	206	204	48	216	133	129	9.3 kg
CHV-X (3)	in.	8.11	8.03	1.89	8.50	5.24	5.08	20.4 lb
CHV-X 100	mm	256	248	62	264	163	156	14.6 kg
CHV-X (4)	in.	10.08	9.76	2.44	10.39	6.43	6.14	32.29 lb
CHV-X 125	mm	314	302	74	322	190	193	32.5 kg
CHV-X (5)	in.	12.36	11.89	2.91	12.68	7.48	7.60	71.65 lb

Specified weights are approximate values only.

Check & stop valve, type SCA-X, 52 bar (754 psi) - Check valve, type CHV-X, 52 bar (754 psi)

**Ordering complete valves**

*How to order*

The table below is used to identify the valve required.

For further information please contact your local Danfoss Sales Company.

Please note that the type codes only serve to identify the valves, some of which may not form part of the standard product range.

Valve type	SCA-X CHV-X	Check & stop valve Check Valve				
(valve size measured on the connection diameter)	<b>15</b> <b>20</b> <b>25</b> <b>32</b> <b>40</b> <b>50</b> <b>65</b> <b>80</b> <b>100</b> <b>125</b>	DN 15 DN 20 DN 25 DN 32 DN 40 DN 50 DN 65 DN 80 DN 100 DN 125	<b>A</b> x x x x x x x x x x	<b>D</b> x x x x x x x x x x	<b>G</b> x x x x x x x x x x	<b>SOC</b> x x x x x x x x x x
Connections	<b>A</b> <b>D</b> <b>G</b> <b>SOC</b>	Welding branches: ANSI B 31.5 schedule 80 DN 15 - 40 (½ - 1½ in.) Welding branches: ANSI B 31.5 schedule 40 DN 50 - 125 (2 - 5 in.) Welding branches: EN 10220 Butt-weld connection: GOST (8734-75 and 8732-78) Socket weld: ANSI B 16.11				
Valve housing	<b>ANG</b> <b>STR</b>	Angle flow Straight flow				

**Important!**

Where products need to be certified according to specific certification societies the relevant information should be included at the time of order.

**Angleway**

*SCA-X Butt-weld DIN (EN 10220)*

Size		Type	Code No.
mm	in.		
15	½	SCA-X 15 D ANG	<b>148B5208</b>
20	¾	SCA-X 20 D ANG	<b>148B5308</b>
25	1	SCA-X 25 D ANG	<b>148B5408</b>
32	1¼	SCA-X 32 D ANG	<b>148B5508</b>
40	1½	SCA-X 40 D ANG	<b>148B5608</b>
50	2	SCA-X 50 D ANG	<b>148B5702</b>
65	2½	SCA-X 65 D ANG	<b>148B5803</b>
80	3	SCA-X 80 D ANG	<b>148B5902</b>
100	4	SCA-X 100 D ANG	<b>148B6002</b>
125	5	SCA-X 125 D ANG	<b>148B6102</b>

**Angleway**

*CHV-X Butt-weld DIN (EN 10220)*

Size		Type	Code No.
mm	in.		
15	½	CHV-X 15 D ANG	<b>148B5236</b>
20	¾	CHV-X 20 D ANG	<b>148B5336</b>
25	1	CHV-X 25 D ANG	<b>148B5436</b>
32	1¼	CHV-X 32 D ANG	<b>148B5536</b>
40	1½	CHV-X 40 D ANG	<b>148B5636</b>
50	2	CHV-X 50 D ANG	<b>148B5736</b>
65	2½	CHV-X 65 D ANG	<b>148B5838</b>
80	3	CHV-X 80 D ANG	<b>148B5936</b>
100	4	CHV-X 100 D ANG	<b>148B6036</b>
125	5	CHV-X 125 D ANG	<b>148B6136</b>

*SCA-X Butt-weld ANSI (B 36.10 Schedule 80)*

Size		Type	Code No.
mm	in.		
15	½	SCA-X 15 A ANG	<b>148B5209</b>
20	¾	SCA-X 20 A ANG	<b>148B5309</b>
25	1	SCA-X 25 A ANG	<b>148B5409</b>
32	1¼	SCA-X 32 A ANG	<b>148B5509</b>
40	1½	SCA-X 40 A ANG	<b>148B5609</b>

*CHV-X Butt-weld ANSI (B 36.10 Schedule 80)*

Size		Type	Code No.
mm	in.		
15	½	CHV-X 15 A ANG	<b>148B5237</b>
20	¾	CHV-X 20 A ANG	<b>148B5337</b>
25	1	CHV-X 25 A ANG	<b>148B5437</b>
32	1¼	CHV-X 32 A ANG	<b>148B5537</b>
40	1½	CHV-X 40 A ANG	<b>148B5637</b>

*SCA-X Butt-weld ANSI (B 36.10 Schedule 40)*

Size		Type	Code No.
mm	in.		
50	2	SCA-X 50 A ANG	<b>148B5703</b>
65	2½	SCA-X 65 A ANG	<b>148B5802</b>
80	3	SCA-X 80 A ANG	<b>148B5903</b>
100	4	SCA-X 100 A ANG	<b>148B6004</b>
125	5	SCA-X 125 A ANG	<b>148B6103</b>

*CHV-X Butt-weld ANSI (B 36.10 Schedule 40)*

Size		Type	Code No.
mm	in.		
50	2	CHV-X 50 A ANG	<b>148B5737</b>
65	2½	CHV-X 65 A ANG	<b>148B5837</b>
80	3	CHV-X 80 A ANG	<b>148B5937</b>
100	4	CHV-X 100 A ANG	<b>148B6037</b>
125	5	CHV-X 125 A ANG	<b>148B6137</b>

*SCA-X Socket welding ANSI (B 16.11)*

Size		Type	Code No.
mm	in.		
50	2	SCA-X 50 SOC ANG	<b>148B5704</b>

*CHV-X Socket welding ANSI (B 16.11)*

Size		Type	Code No.
mm	in.		
32	1¼	CHV 32 SOC ANG	<b>148B5539</b>
50	2	CHV 50 SOC ANG	<b>148B5740</b>

ANG = Angleway

**Ordering complete valves**  
(continued)

**Straightway**

*CHV-X Butt-weld DIN (EN 10220)*

Size		Type	Code No.
mm	in.		
15	½	CHV-X 15 D STR	<b>148B6581</b>
20	¾	CHV-X 20 D STR	<b>148B6583</b>
25	1	CHV-X 25 D STR	<b>148B6585</b>
32	1¼	CHV-X 32 D STR	<b>148B6587</b>
40	1½	CHV-X 40 D STR	<b>148B6589</b>
50	2	CHV-X 50 D STR	<b>148B6591</b>
65	2½	CHV-X 65 D STR	<b>148B6593</b>
80	3	CHV-X 80 D STR	<b>148B6595</b>
100	4	CHV-X 100 D STR	<b>148B6597</b>
125	5	CHV-X 125 D STR	<b>148B6599</b>

*CHV-X Butt-weld ANSI (B 36.10 Schedule 80)*

Size		Type	Code No.
mm	in.		
15	½	CHV-X 15 A STR	<b>148B6582</b>
20	¾	CHV-X 20 A STR	<b>148B6584</b>
25	1	CHV-X 25 A STR	<b>148B6586</b>
32	1¼	CHV-X 32 A STR	<b>148B6588</b>
40	1½	CHV-X 40 A STR	<b>148B6590</b>

*CHV-X Butt-weld ANSI (B 36.10 Schedule 40)*

Size		Type	Code No.
mm	in.		
50	2	CHV-X 50 A STR	<b>148B6592</b>
65	2½	CHV-X 65 A STR	<b>148B6594</b>
80	3	CHV-X 80 A STR	<b>148B6596</b>
100	4	CHV-X 100 A STR	<b>148B6598</b>
125	5	CHV-X 125 A STR	<b>148B6600</b>

*CHV-X Socket welding ANSI (B 16.11)*

Size		Type	Code No.
mm	in.		
15	½	CHV-X 15 SOC STR	<b>148B6601</b>
20	¾	CHV-X 20 SOC STR	<b>148B6602</b>
25	1	CHV-X 25 SOC STR	<b>148B6603</b>
32	1¼	CHV-X 32 SOC STR	<b>148B6604</b>
40	1½	CHV-X 40 SOC STR	<b>148B6605</b>
50	2	CHV-X 50 SOC STR	<b>148B6606</b>

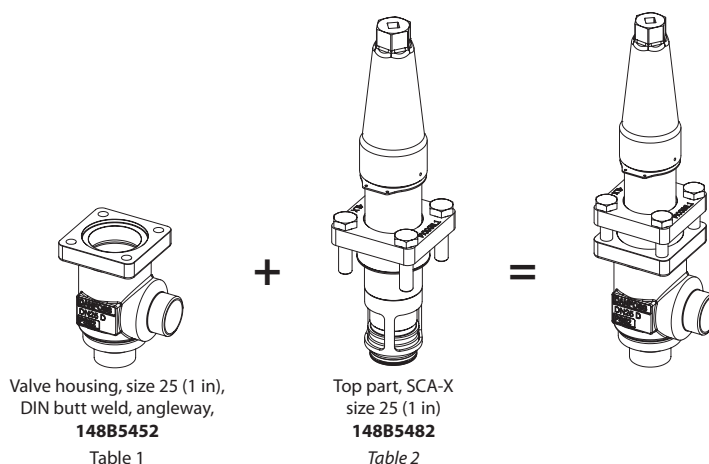
STR = Straightway



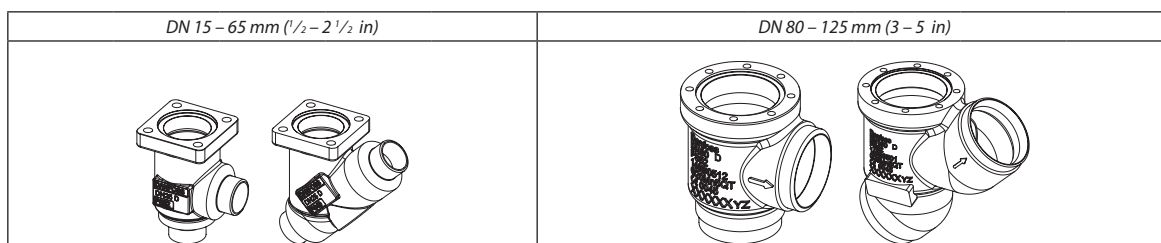
Check & stop valve, type SCA-X, 52 bar (754 psi) - Check valve, type CHV-X, 52 bar (754 psi)

Ordering SVA-X from the parts programme

**Example**  
(select from  
table 1 and 2)

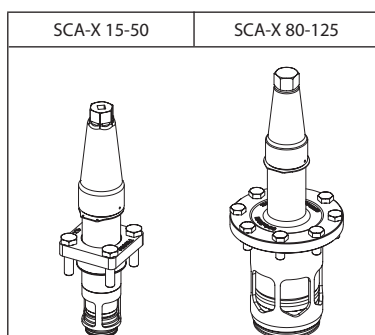


**Table 1**  
SVL valve housings  
w/different  
connections



Sizes [DN]		Valve Housing SVL										
[mm]	[in]	DIN-Butt weld		ANSI-Butt weld		GOST-Butt-weld		SOC		FPT		T
		ANG	STR	ANG	STR	ANG	STR	ANG	STR	ANG	STR	ANG
15	1/2	148B5252	148B5253	148B5254	148B5255	148B5391	148B5392	148B5256	148B5257	148B5258	148B5259	
20	3/4	148B5352	148B5353	148B5354	148B5355	148B5393	148B5394	148B5356	148B5357	148B5358	148B5359	
25	1	148B5452	148B5453	148B5454	148B5455	148B5498	148B5499	148B5456	148B5457	148B5458	148B5459	
32	1 1/4	148B5576	148B5577	148B5578	148B5579	148B5593	148B5594	148B5580	148B5581	148B5582	148B5583	
40	1 1/2	148B5652	148B5653	148B5654	148B5655	148B5681	148B5682	148B5656	148B5657			
50	2	148B5741	148B5742	148B5743	148B5744	148B5759	148B5760	148B5745	148B5746			
65	2 1/2	148B5816	148B5817	148B5818	148B5819	148B5816	148B5817					
80	3	148B5912	148B5913	148B5914	148B5915	148B5912	148B5913					
100	4	148B6014	148B6015	148B6016	148B6017	148B6033	148B6034					
125	5	148B6112	148B6113	148B6114	148B6115	148B6133	148B6134					

**Table 2**  
SCA-X complete top part  
including gaskets and  
bolts



Sizes [DN]		Complete top part
[mm]	[in]	SCA-X
15	1/2	148B5282
20	3/4	
25	1	
32	1 1/4	
40	1 1/2	148B5482
50	2	148B5735
65	2 1/2	148B5825
80	3	148B5918
100	4	148B6019
125	5	148B6118

Replacement kit (O-ring replacement) for R717 Ammonia Heat Pump\* and Propylene applications (including ID tag)

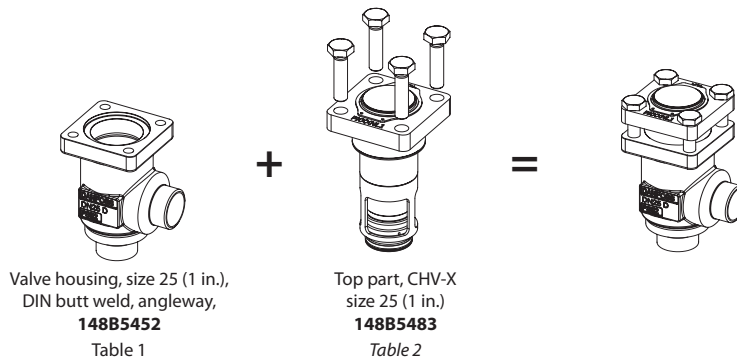
Size (DN)		O-ring kit for	
mm	in.	R717 Heat pump	R1270 Propylene
15	1/2	148B6070	148B6077
20	3/4		
25	1	148B6071	148B6078
32	1 1/4		
40	1 1/2		
50	2	148B6072	148B6079
65	2 1/2	148B6073	148B6080
80	3	148B6074	148B6081
100	4	148B6075	148B6082
125	5	148B6076	148B6083

\* Replacement kits for R717 Ammonia Heat Pump is applicable for continuous operating temperature between +100°C to 150°C (212°F to 302°F)

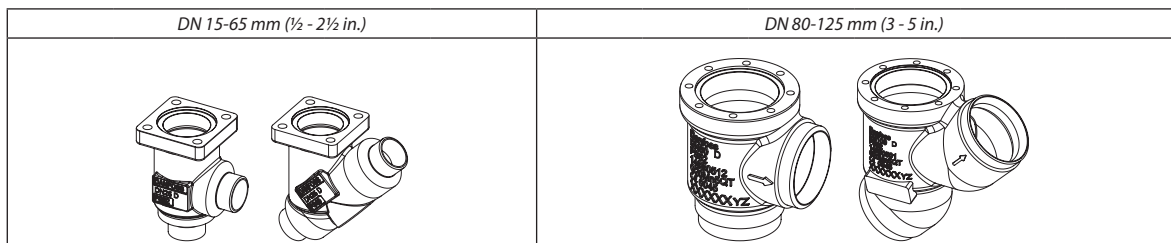
Check & stop valve, type SCA-X, 52 bar (754 psi) - Check valve, type CHV-X, 52 bar (754 psi)

Ordering CHV-X from the parts programme

**Example**  
(select from  
table 1 and 2)

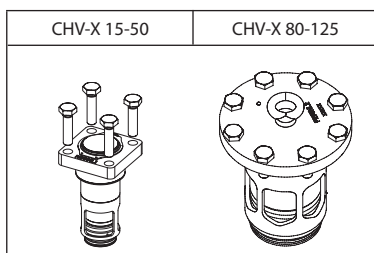


**Table 1**  
SVL valve housings  
w/different  
connections



Sizes [DN]		Valve Housing SVL										
		DIN-Butt weld		ANSI-Butt weld		GOST-Butt-weld		SOC		FPT		T
mm	in.	ANG	STR	ANG	STR	ANG	STR	ANG	STR	ANG	STR	ANG
15	1/2	148B5252	148B5253	148B5254	148B5255	148B5391	148B5392	148B5256	148B5257	148B5258	148B5259	
20	3/4	148B5352	148B5353	148B5354	148B5355	148B5393	148B5394	148B5356	148B5357	148B5358	148B5359	
25	1	148B5452	148B5453	148B5454	148B5455	148B5498	148B5499	148B5456	148B5457	148B5458	148B5459	
32	1 1/4	148B5576	148B5577	148B5578	148B5579	148B5593	148B5594	148B5580	148B5581	148B5582	148B5583	
40	1 1/2	148B5652	148B5653	148B5654	148B5655	148B5681	148B5682	148B5656	148B5657			
50	2	148B5741	148B5742	148B5743	148B5744	148B5759	148B5760	148B5745	148B5746			
65	2 1/2	148B5816	148B5817	148B5818	148B5819	148B5816	148B5817					
80	3	148B5912	148B5913	148B5914	148B5915	148B5912	148B5913					
100	4	148B6014	148B6015	148B6016	148B6017	148B6033	148B6034					
125	5	148B6112	148B6113	148B6114	148B6115	148B6133	148B6134					

**Table 2**  
CHV-X complete top part  
including gaskets and  
bolts



Sizes [DN]		Complete top part
mm	in.	CHV-X
15	1/2	<b>148B5283</b>
20	3/4	
25	1	
32	1 1/4	
40	1 1/2	<b>148B5483</b>
50	2	
65	2 1/2	<b>148B5747</b>
80	3	<b>148B5827</b>
100	4	<b>148B5919</b>
125	5	<b>148B6022</b>
		<b>148B6119</b>

Replacement kit (O-ring replacement) for R717 Ammonia Heat Pump\* and Propylene applications (including ID tag)

Size (DN)		O-ring kit for	
mm	in.	R717 Heat pump	R1270 Propylene
15	1/2	<b>148B6070</b>	<b>148B6077</b>
20	3/4		
25	1	<b>148B6071</b>	<b>148B6078</b>
32	1 1/4		
40	1 1/2		
50	2	<b>148B6072</b>	<b>148B6079</b>
65	2 1/2	<b>148B6073</b>	<b>148B6080</b>
80	3	<b>148B6074</b>	<b>148B6081</b>
100	4	<b>148B6075</b>	<b>148B6082</b>
125	5	<b>148B6076</b>	<b>148B6083</b>

\* Replacement kits for R717 Ammonia Heat Pump is applicable for continuous operating temperature between +100°C to 150°C (212°F to 302°F)

# Check & stop valve, SCA-X, 65 bar (943 psi) Check valve, CHV-X, 65 bar (943 psi)

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## Check & stop valve, SCA-X, 65 bar (943 psi)

### Check valve, CHV-X, 65 bar (943 psi)



SCA-X are check valves with a built-in stop valve function. CHV-X are check valves only. SCA-X/CHV-X are available in angleway and straightway versions.

The valves are designed to open at very low differential pressures, allow favourable flow conditions and are easy to disassemble for inspection and service.

The SCA-X is equipped with vented cap and has internal backseating enabling the spindle seal to be replaced whilst the valve still under pressure.

Laser cut V-ports provide excellent opening characteristics (SCA-X/CHV-X 50-125).

The valve cone has a built-in flexibility to ensure a precise and tight closing towards the valve seat.

A well balanced dampening effect between the piston and the cylinder gives an optimal protection during low loads and against pulsations.

#### Features

- Modular Concept:
  - Each valve housing is available with DIN and ANSI butt weld connection and in several different sizes.
  - Possible to convert SCA-X or CHV-X to any other product in the Flexline™ SVL family (regulating valve, shut-off valve or strainer) just by replacing the complete top part.
- Fast and easy valve overhaul service. It is easy to replace the top part and no welding is needed.
- Designed to open at a very low differential pressure of 0.04 bar (0.58 psig).
- Designed with a built-in damping chamber preventing valve flutter in case of low refrigerant velocity and/or low density.
- Each valve is clearly marked with type, size and performance range.  
At replacement of the O-ring for special application, an additional ID ring is fixed to the valve.
- Easy to disassemble for inspection and service.
- Internal backseating enables replacement of the spindle seal whilst the valve is active, i.e. under pressure.
- Optimal flow characteristics ensuring quick opening to the fully open position.
- Protection against pulsation by built-in damping facility.
- Housing and bonnet material is low temperature steel according to requirements of the Pressure Equipment Directive and other international classification authorities.
- Equipped with 42 CrMo5 bolts to withstand high pressure.
- Classification: DNV, CRN, BV, EAC etc.  
To get an updated list of certification on the products please contact your local Danfoss Sales Company.
- Service kits with replacement O-rings for R717 Heat Pump and R1270 Propylene include separate ID-ring for ID of application.

Check & stop valve, type SCA-X, 65 bar (943 psi) - Check valve, type CHV-X, 65 bar (943 psi)

**Technical data**

- *Refrigerants*  
Applicable to HCFC, HFC, R717 (Ammonia), R744 (CO<sub>2</sub>) and flammable refrigerants.  
For further information please see the installation guide for SCA-X/CHV-X.
- *Temperature range*  
-60/+150°C (-76/+302°F).
- *Max. working pressure*  
65 bar (943 psig)  
*With O-ring replaced (Service kit):*  
Heat pump configuration: R717 - 65 bar (943 psi) @ +100°C to +150°C (+212°F to +302°F) continuous.  
Propylene configuration: R1270 - 65 bar (943 psi) @ -60°C to 150°C (-76°F to 302°F)

**Design**

*Housing*

The housing is made from special, cold resistant steel.

*Valve cone*

Valve cone with built in metallic stop - prevents damage to teflon ring in case of overtightening.

Teflon ring made of reinforced teflon

*Damping chamber*

The chamber is filled with refrigerants (gas or liquid), which provides a damping effect when the valve opens and closes.

*Spindle (SCA-X)*

Made of polished stainless steel, which is ideal for O-ring sealing.

*Packing Gland (SCA-X)*

The "full temperature range" packing gland is the standard for the entire SVL platform.

This ensures perfect tightness throughout the whole temperature range:  
-60/+150°C (-76/+302°F).

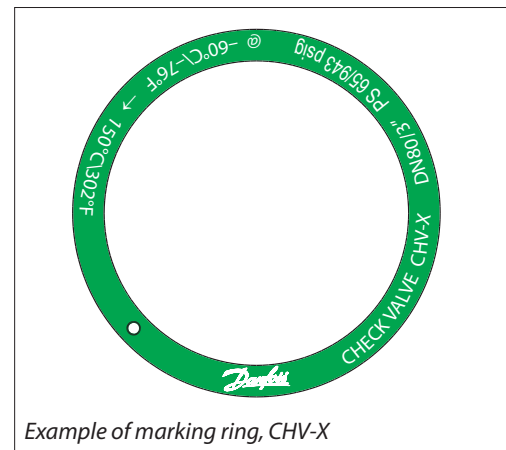
*Installation*

The valve must be mounted vertically with the cone downwards.

The valve is designed to resist very high internal pressure. However, the piping system in general should be designed to avoid liquid traps and reduce the risk of hydraulic pressure caused by thermal expansion.

For further information refer to installation guide for SCA-X/CHV-X.

If cold refrigeration oil having low viscosity enters and settles in the damping chamber, problems with the check valve may arise. Consequently, it may be necessary to modify the valve for more viscous liquids by enlarging the hole to the damping chamber.

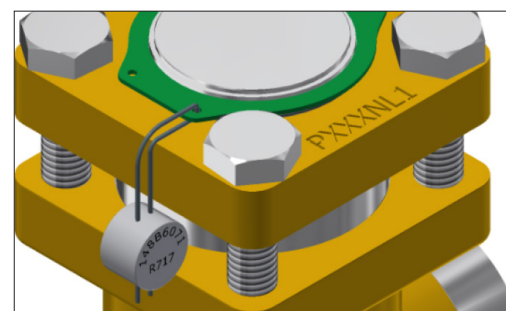


Example of marking ring, CHV-X

*ID ring for special application*

After converting a SCA or CHV valve for Heat Pump/Propylene applications (replacing O-ring) the color marked ID tag included in the service kit must be fixed to the valve as shown in figure to the right.

The ID tag indicates the special application and identifies the installed O-ring.



Check & stop valve, type SCA-X, 65 bar (943 psi) - Check valve, type CHV-X, 65 bar (943 psi)

Pressure Equipment Directive (PED)  
 SVL valves are approved according to the European standard specified in the Pressure Equipment Directive and are CE marked.

For further details / restrictions - see Installation guide.



SVL			
Nominal bore	DN ≤ 25 mm (1 in.)	DN32-80 mm (1¼ - 3 in.)	DN100 - 200 mm (4-8 in.)
Classified for	Fluid group I		
Category	Article 3, paragraph 3	II	III

Computation and selection

Introduction

When dimensioning SCA-X/CHV-X, it is important to select a valve that is best suited to all operating conditions. Therefore, it is necessary to consider both the nominal and part load working conditions.

The SCA-X/CHV-X valve can be calculated in two ways:

- Using the tables below.
- Using Coolselector™

Example

SI-Units

Assumed working conditions:  
 Maximum flow  $\dot{V} = 1000 \text{ m}^3/\text{h}$   
 Density  $\rho = 3.0 \text{ kg/m}^3$   
 Minimum part load = 33%

US-Units

Assumed working conditions:  
 Maximum flow  $\dot{V} = 1160 \text{ gpm}$   
 Density  $\rho = 0.187 \text{ lb/feet}^3$   
 Minimum part load = 33%

Used expressions:

Recommended velocity -  $C_{rec}$  [m/s]  
 Minimum recommended velocity -  $C_{min, rec}$  [m/s]  
 Maximum velocity -  $C_{max}$  [m/s]  
 Part load velocity -  $C_{part}$  [m/s]

Used expressions:

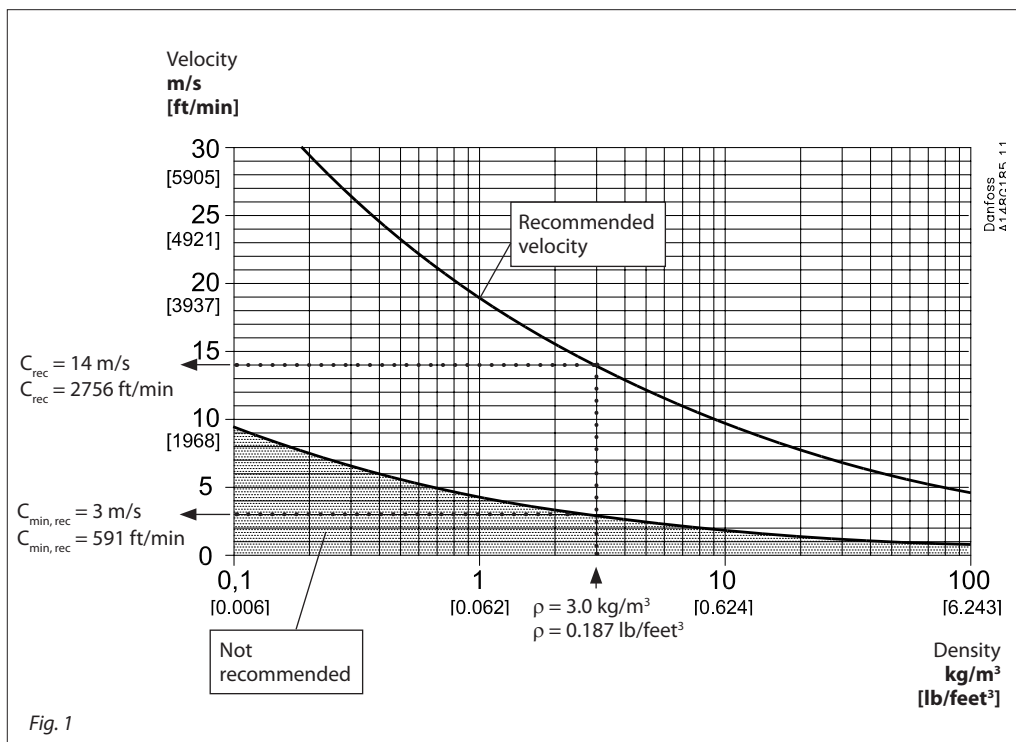
Recommended velocity -  $C_{rec}$  [ft/min]  
 Minimum recommended velocity -  $C_{min, rec}$  [ft/min]  
 Maximum velocity -  $C_{max}$  [ft/min]  
 Part load velocity -  $C_{part}$  [ft/min]

We know the density  $\rho \approx 3.0 \text{ kg/m}^3$ , consequently  $C_{rec}$  as well as  $C_{min, rec}$  can be found in the figure below (standard valve).

We know the density  $\rho \approx 0.187 \text{ lb/feet}^3$ , consequently  $C_{rec}$  as well as  $C_{min, rec}$  can be found in the figure (standard valve).

$C_{rec} \approx 14 \text{ m/s}$   
 $C_{min, rec} \approx 3 \text{ m/s}$

$C_{rec} \approx 2756 \text{ ft/min}$   
 $C_{min, rec} \approx 591 \text{ ft/min}$



Selection example continued on following page.

Check & stop valve, type SCA-X, 65 bar (943 psi) - Check valve, type CHV-X, 65 bar (943 psi)

**Computation and selection**  
(continued)

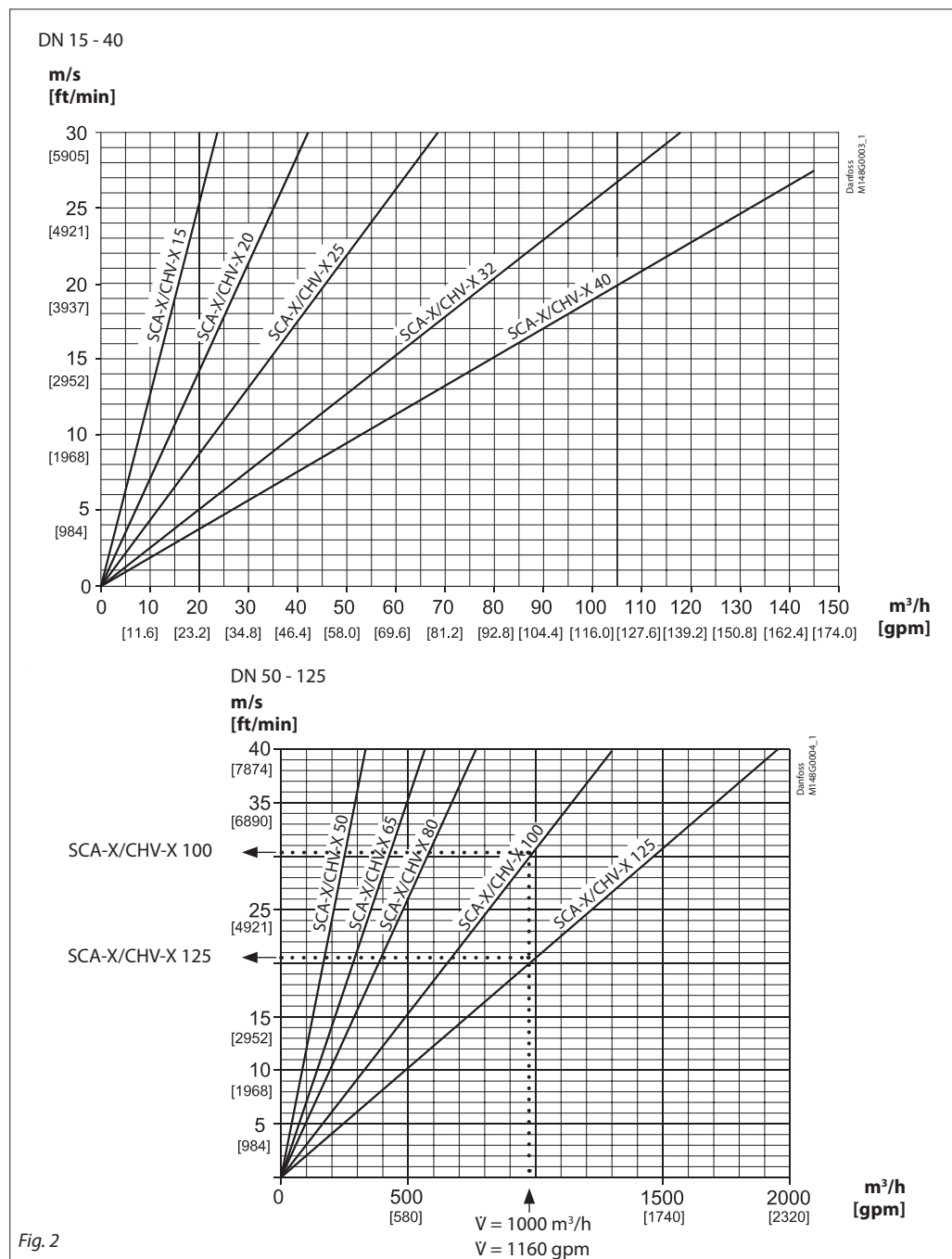
Knowing that  $\dot{V} = 1000 \text{ m}^3/\text{h}$  (1160 gpm) fig. 2 gives the following choices:

For SCA-X/CHV-X in size DN 100 the maximum velocity  $C_{\text{max}} \approx 31 \text{ m/s}$  (6100 ft/min)  
 For SCA-X/CHV-X in size DN 125 the maximum velocity  $C_{\text{max}} \approx 20 \text{ m/s}$  (3900 ft/min)

In conclusion SCA-X in size DN 125 is selected because  $C_{\text{max}} \approx 20 \text{ m/s}$  (3900 ft/min) comes nearest to the recommended velocity  $C_{\text{rec}} \approx 14 \text{ m/s}$  (2756 ft/min) and at the same time part load conditions fulfil the requirements, as described:

If the valve in question (for instance under part load conditions) provides a velocity less than  $C_{\text{min, rec}}$  the valve might start hammering and become noisy. As a result the valve may wear prematurely.

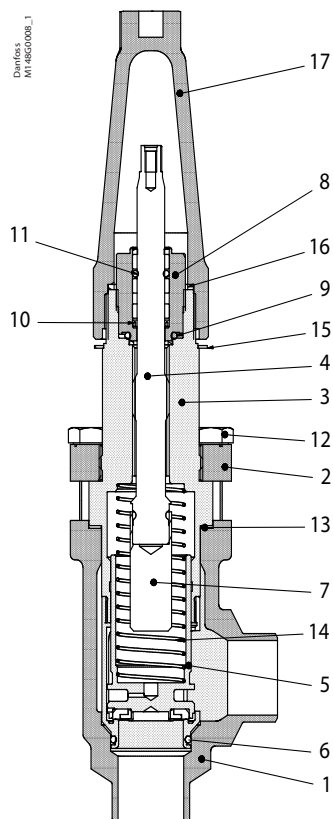
We know that  $C_{\text{max}} \approx 20 \text{ m/s}$  (3900 ft/min) and that minimum part load is 33%. It follows that  $C_{\text{part}} \approx 6.5 \text{ m/s}$  (1290 ft/min). Thus,  $C_{\text{part}}$  (6.5 m/s) >  $C_{\text{min, rec}}$  (3.0 m/s) and the selected SCA-X model DN125 is the perfect choice.



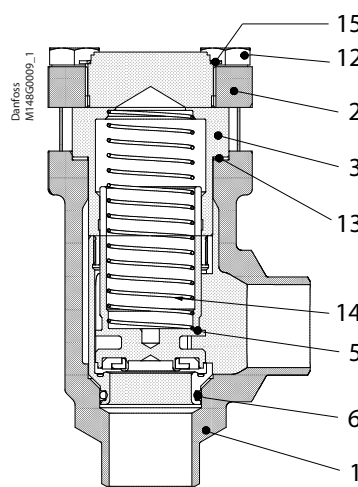


Check & stop valve, type SCA-X, 65 bar (943 psi) - Check valve, type CHV-X, 65 bar (943 psi)

Material specification



SCA-X 15 - 40



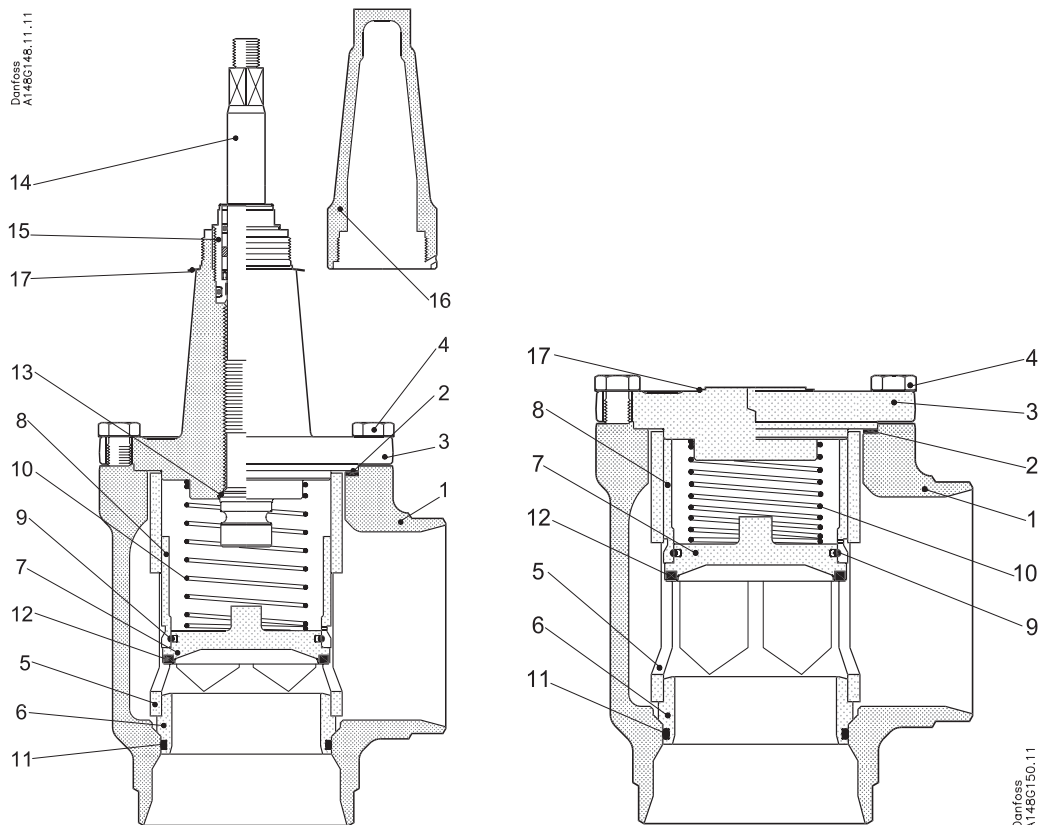
CHV-X 15 - 40

No.	Part	Material	DIN/EN	ISO	ASTM
1	Housing	Steel	G20Mn5QT, 10213-3 P285QH+QT, 10222-4		LCC, A352 LF2, A350
2	Bonnet, Flange	Steel	P275NL1 EN10028-3		LF2, A350
3	Bonnet, Insert	Steel	115Mn30 10087	Type 2 R 683/9	AISI 1213
4	Spindle	Stainless steel	X8CrNiS18-9, EN 10088-3	Type 17 683/13	AISI 303
5	Cone	Steel Teflon (PTFE)			
6	O-ring	Cloroprene (Neoprene)*			
7	Spindle extension	Steel			
8	Packing gland O-rings	Stainless steel Cloroprene (Neoprene)	X8CrNiS18-9 10088	Type 17 683/13	AISI 303
9	Packing washer	Aluminium			
10	Spring loaded seal	Teflon (PTFE)			
11	O-ring	Cloroprene (Neoprene)			
12	Bolts	High temperature steel	42CrMo5 10269		A193
13	Gasket	Fiber, non-asbestos			
14	Spring	Steel			
15	Identification ring	Stainless steel			
16	Seal cap gasket	Nylon			
17	Spindle seal cap	Aluminium			

\*To be replaced in R717 Heat Pump and R1270 Propylene applications.

Check & stop valve, type SCA-X, 65 bar (943 psi) - Check valve, type CHV-X, 65 bar (943 psi)

Material specification



SCA-X 50 - 125

CHV-X 50 - 125

No.	Part	Material	DIN/EN	ISO	ASTM
1	Housing DN 50-65	Steel	G20Mn5QT, 10213-3 ----- P285QH+QT, 10222-4		LCC, A352 ----- LF2, A350
	Housing DN 80-125	Steel	G20Mn5 QT SEW 685		LCC, A352
2	Gasket	Fiber, Non-asbestos			
3	SCA-X: Valve bonnet CHV-X: End cover	Steel	P285 QH EN 10222-4 ----- P275NL1 or 2 EN10028-3		LF2, A350 ----- A, A662
4	Bolts	High temperature steel	42CrMo5 10269		A193
5	Tube	Steel			
6	Seat	Steel			
7	Valve plate	Steel			
8	Guide sleeve	Steel			
9	Spring ring	Steel			
10	Spring	Steel			
11	O-ring	Cloroprene (Neoprene)*			
12	Teflon ring	Teflon (PTFE)			
13	Soft back seal	Teflon (PTFE)			
14	Spindle DN 50-65	Stainless steel	X8CrNiS18-9 17440	Type 17 R 683/13	AISI 303
	Spindle DN 80-125	Stainless steel	X5CrNi1810 17440	Type 11 683/13	AISI 304 A-276
15	Packing gland	Stainless steel	X8CrNiS18-9, EN 10088-3,	Type 17 R 683/13	AISI 303
16	Spindle seal cap and gasket	Aluminium			
17	Marking label	Stainless steel			

\*To be replaced in R717 Heat Pump and R1270 Propylene applications.

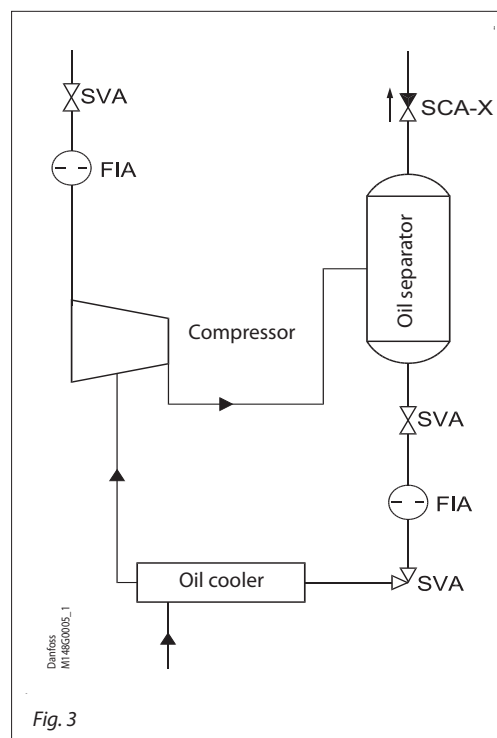
**Application**

Figure 3 shows the check & stop valve SCA-X in the discharge line of a screw compressor unit. The SCA-X valve in the discharge line prevents "back condensation" in the oil separator as well as pressure equalising through the compressor.

Compared to an ordinary stop and check valve arrangement the combined stop/check valve solution, as shown, is easier to install and has lower flow resistance.

Installation of the SCA-X/CHV-X in the economizer line is **not** recommended.

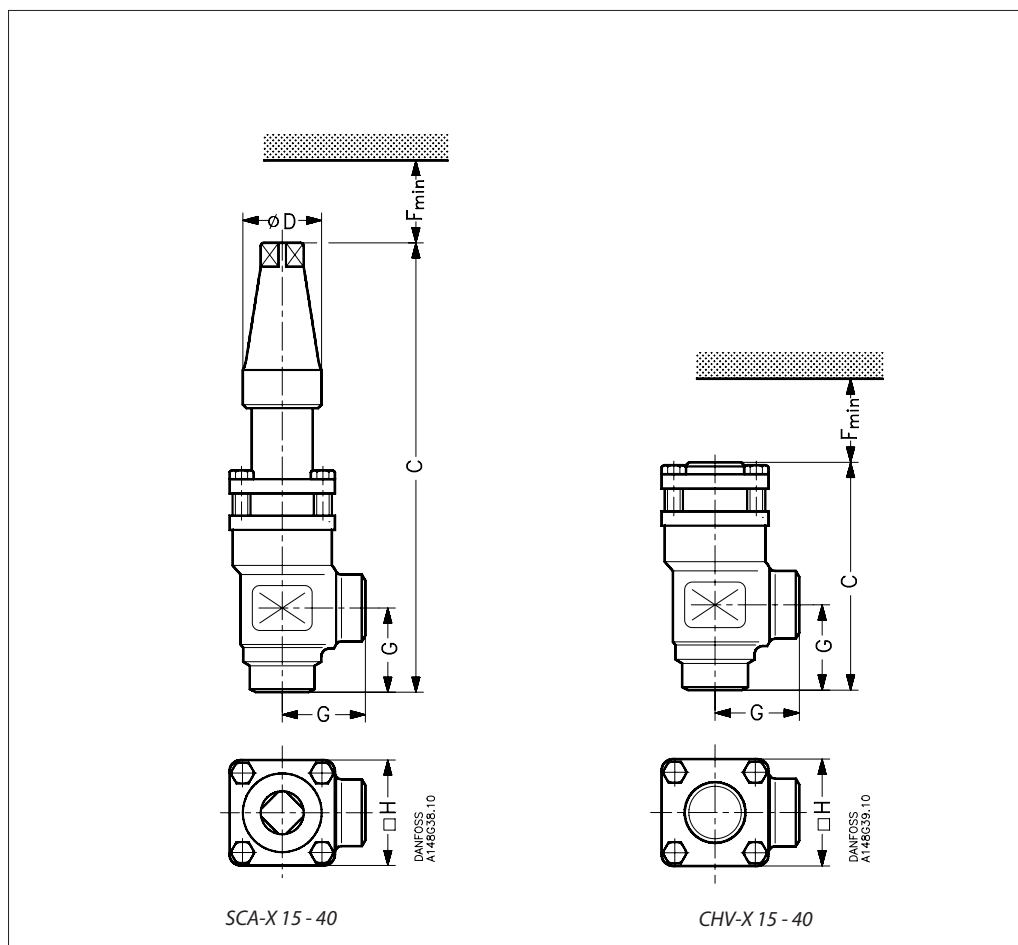
For horizontal installation of the function module; please contact Danfoss.



Check & stop valve, type SCA-X, 65 bar (943 psi) - Check valve, type CHV-X, 65 bar (943 psi)

Dimensions and weights

SCA-X/CHV-X 15 - 40 (½- 1½ in.)



Valve size	C	G	ØD	F <sub>min</sub>	H	Weight
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SCA-X 15 - 40

Valve size	mm	in.	C	G	ØD	F <sub>min</sub>	H	Weight
SCA-X 15 (½ in.)	212	8.35	45	38	60	60	1.6 kg	
			1.77	1.50	2.36	2.36	3.53 lb	
SCA-X 20 (¾ in.)	212	8.35	45	38	60	60	1.6 kg	
			1.77	1.50	2.36	2.36	3.53 lb	
SCA-X 25 (1 in.)	295	11.61	55	50	85	70	3.2 kg	
			2.17	1.97	3.35	2.76	7.05 lb	
SCA-X 32 (1¼ in.)	295	11.61	55	50	85	70	3.2 kg	
			2.17	1.97	3.35	2.76	7.05 lb	
SCA-X 40 (1½ in.)	295	11.61	55	50	85	70	3.2 kg	
			2.17	1.97	3.35	2.76	7.05 lb	

Valve size	C	G	F <sub>min</sub>	H	Weight
------------	---	---	------------------	---	--------

CHV-X 15 - 40

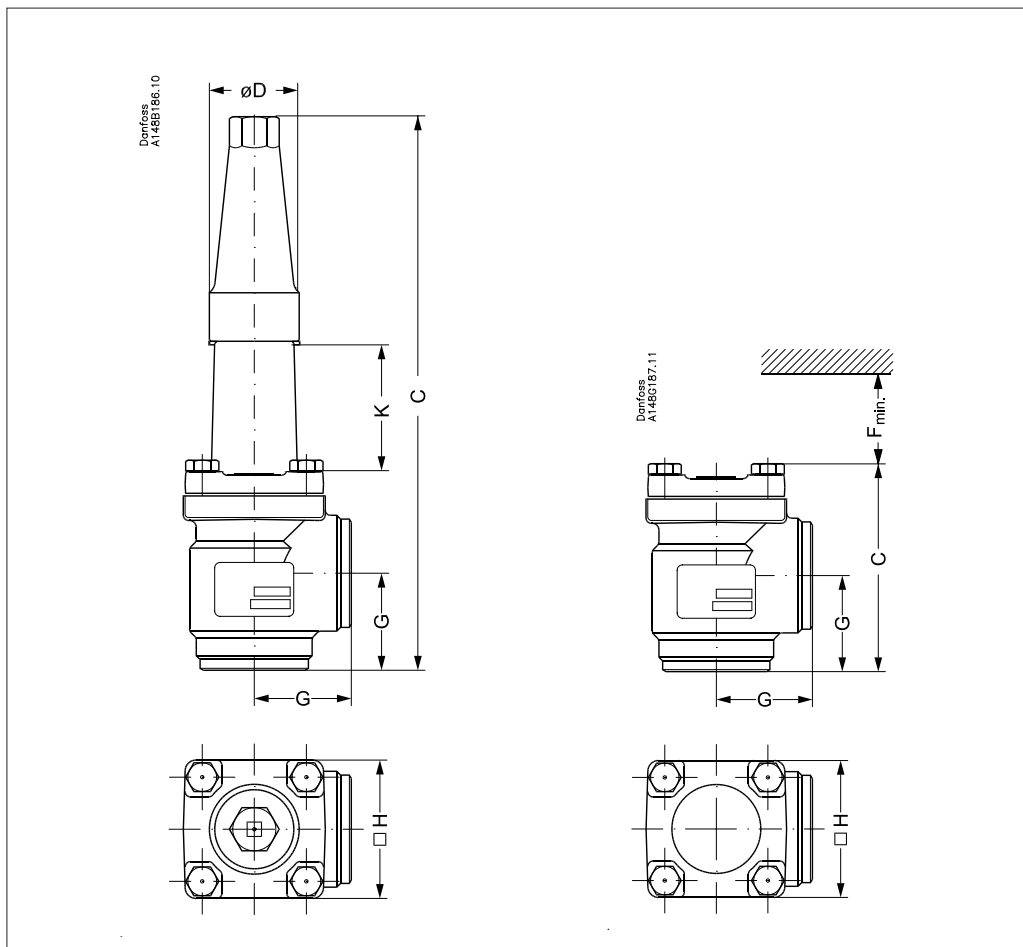
Valve size	mm	in.	C	G	F <sub>min</sub>	H	Weight
CHV-X 15 (½ in.)	103	4.06	45	60	60	1.2 kg	
			1.77	2.36	2.36	2.65 lb	
CHV-X 20 (¾ in.)	103	4.06	45	60	60	1.2 kg	
			1.77	2.36	2.36	2.65 lb	
CHV-X 25 (1 in.)	143	5.63	55	85	70	2.3 kg	
			2.17	3.35	2.76	5.07 lb	
CHV-X 32 (1¼ in.)	143	5.63	55	85	70	2.3 kg	
			2.17	3.35	2.76	5.07 lb	
CHV-X 40 (1½ in.)	143	5.63	55	85	70	2.3 kg	
			2.17	3.35	2.76	5.07 lb	

Specified weights are approximate values only.

Check & stop valve, type SCA-X, 65 bar (943 psi) - Check valve, type CHV-X, 65 bar (943 psi)

Dimensions and weights

SCA-X/CHV-X 50 - 65 (2 - 2½ in.)



Valve size	K	C	G	ØD	□H	Weight
------------	---	---	---	----	----	--------

SCA-X

SCA-X 50	mm	70	315	60	50	77	3.8 kg
SCA-X (2)	in.	2.76	12.40	2.36	1.97	3.03	8.40 lb
SCA-X 65	mm	70	335	70	50	90	5.5 kg
SCA-X (2½)	in.	2.76	13.19	2.76	1.97	3.54	12.16 lb

Valve size	C	G	F <sub>min.</sub>	□H	Weight
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CHV-X

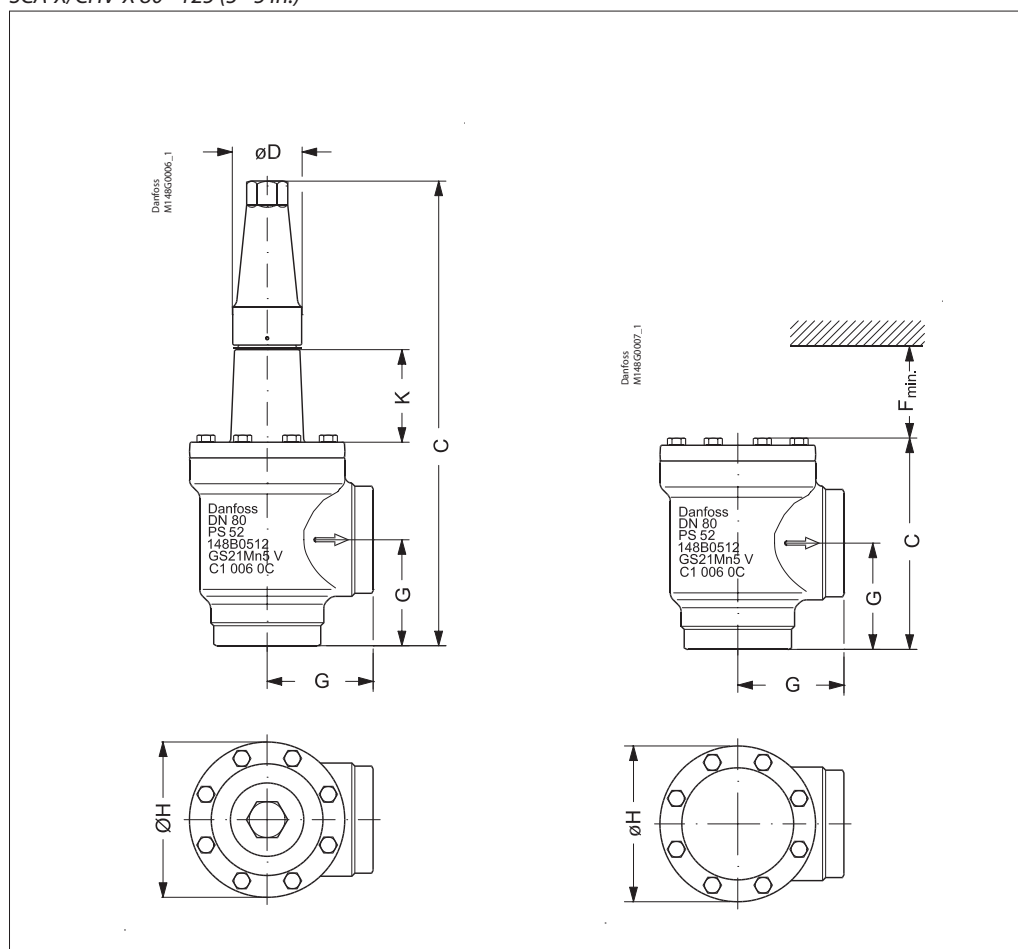
CHV-X 50	mm	132	60	92	77	3.2 kg
CHV-X (2)	in.	5.20	2.36	3.62	3.03	7.10 lb
CHV-X 65	mm	152	70	107	90	4.5 kg
CHV-X (2½)	in.	5.98	2.76	4.21	3.54	9.95 lb

Specified weights are approximate values only.

Check & stop valve, type SCA-X, 65 bar (943 psi) - Check valve, type CHV-X, 65 bar (943 psi)

Dimensions and weights

SCA-X/CHV-X 80 - 125 (3 - 5 in.)



Valve size	K	C	G	ØD	ØH	Weight
------------	---	---	---	----	----	--------

SCA-X

SCA-X 80	mm	76	388	90	58	129	9.7 kg
SCA-X (3)	in.	3.00	15.28	3.54	2.28	5.08	21.4 lb
SCA-X 100	mm	90	437	106	58	156	15.3 kg
SCA-X (4)	in.	3.54	17.20	4.17	2.28	6.14	33.7 lb
SCA-X 125	mm	90	533	128	74	193	28.1 kg
SCA-X (5)	in.	3.54	20.98	5.04	2.91	7.60	61.9 lb

Valve size	C	G	F <sub>min.</sub>	ØH	Weight
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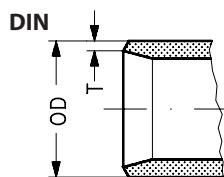
CHV-X

CHV-X 80	mm	189	90	133	129	8.7 kg
CHV-X (3)	in.	7.44	3.54	5.24	5.08	19.23 lb
CHV-X 100	mm	223	106	163	156	14.3 kg
CHV-X (4)	in.	8.78	4.17	6.43	6.14	31.60 lb
CHV-X 125	mm	268	128	190	193	25.6 kg
CHV-X (5)	in.	10.55	5.04	7.48	7.60	56.58 lb

Specified weights are approximate values only.

Check & stop valve, type SCA-X, 65 bar (943 psi) - Check valve, type CHV-X, 65 bar (943 psi)

Connections

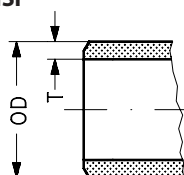


Size mm	Size in.	OD mm	T mm	OD in.	T in.			k <sub>v</sub> -angle m <sup>3</sup> /h	k <sub>v</sub> -straight m <sup>3</sup> /h	C <sub>v</sub> -angle USgal/min	C <sub>v</sub> -straight USgal/min
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Butt-weld DIN (EN 10220)

15	½	21.3	2.3	0.839	0.091			7.0	4.9	8.1	5.7
20	¾	26.9	2.3	1.059	0.091			14.6	10.2	16.9	11.8
25	1	33.7	2.6	1.327	0.103			24.8	17.4	28.8	20.2
32	1¼	42.4	2.6	1.669	0.102			42.6	29.8	49.4	34.6
40	1½	48.3	2.6	1.902	0.103			45.2	31.6	52.4	36.7
50	2	60.3	2.9	2.37	0.11			80	65	93	76
65	2½	76.1	2.9	3	0.11			120	97	140	113
80	3	88.9	3.2	3.50	0.13			182	152	211	176
100	4	114.3	3.6	4.50	0.14			313	278	363	323
125	5	139.7	4.0	5.50	0.16			514	470	596	545

ANSI



Size mm	Size in.	OD mm	T mm	OD in.	T in.			k <sub>v</sub> -angle m <sup>3</sup> /h	k <sub>v</sub> -straight m <sup>3</sup> /h	C <sub>v</sub> -angle USgal/min	C <sub>v</sub> -straight USgal/min
---------	----------	-------	------	--------	-------	--	--	---	--	---------------------------------	------------------------------------

Butt-weld ANSI (B 36.10 Schedule 80)

15	½	21.3	3.7	0.839	0.146			7.0	4.9	8.1	5.7
20	¾	26.9	4.0	1.059	0.158			14.6	10.2	16.9	11.8
25	1	33.7	4.6	1.327	0.181			24.8	17.4	28.8	20.2
32	1¼	42.4	4.9	1.669	0.193			42.6	29.8	49.4	34.6
40	1½	48.3	5.1	1.902	0.201			45.2	31.6	52.4	36.7

Butt-weld ANSI (B 36.10 Schedule 40)

50	2	60.3	3.9	2.37	0.15			80	65	93	76
65	2½	73.0	5.2	2.87	0.20			120	97	140	113
80	3	88.9	5.5	3.50	0.22			182	152	211	176
100	4	114.3	6.0	4.50	0.24			313	278	363	323
125	5	141.3	6.6	5.56	0.26			514	470	596	545

Ordering

Size [DN]	Parts Program					
	Housing				Top complete	
	ANG		STR		SCA-X	CHV-X
	DIN	ANSI	DIN	ANSI		
6						
10						
15	148B6622	148B6612	148B6642	148B6632	148B5769	148B5776
20	148B6623	148B6613	148B6643	148B6633	148B5769	148B5776
25	148B6624	148B6614	148B6644	148B6634	148B5770	148B5777
32	148B6625	148B6615	148B6645	148B6635	148B5770	148B5777
40	148B6626	148B6616	148B6646	148B6636	148B5770	148B5777
50	148B6627	148B6617	148B6647	148B6637	148B5771	148B5778
65	148B6628	148B6618	148B6648	148B6638	148B5772	148B5779
80	148B6629	148B6619	148B6649	148B6639	148B5773	148B5780
100	148B6630	148B6620	148B6650	148B6640	148B5774	148B5781
125	148B6631	148B6621	148B6651	148B6641	148B5775	148B5782
150						
200						

Size [DN]	Service kit*	
	O-ring kit for	
	R717 Heat Pump	R1270 Propylene
6		
10		
15	148B6070	148B6077
20	148B6070	148B6077
25	148B6071	148B6078
32	148B6071	148B6078
40	148B6071	148B6078
50	148B6072	148B6079
65	148B6073	148B6080
80	148B6074	148B6081
100	148B6075	148B6082
125	148B6076	148B6083
150		
200		





# Check & stop valves, type SCA-X SS Check valves, type CHV-X SS

## Contents

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Pressure and temperature range .....	35
Design .....	36
Technical data .....	36
Connections .....	37
Material specification .....	38
Dimensions and weights .....	39
Ordering complete valves .....	40
Important! .....	40



# Check & stop valves, type SCA-X SS Check valves, type CHV-X SS



In certain specific areas such as outdoor applications and corrosive atmospheres, such as coastal installations, there is a need for high surface protection to prevent failure due to corrosion.

Today's food safety standards often call for daily treatment with detergents to protect against bacteria growth, again producing a need for high surface protection.

SCA-X SS are check valves with a built-in stop valve function. CHV-X SS are check valves only.

The valves are designed to open at very low differential pressures, allow favourable flow conditions and are easy to disassemble for inspection and service.

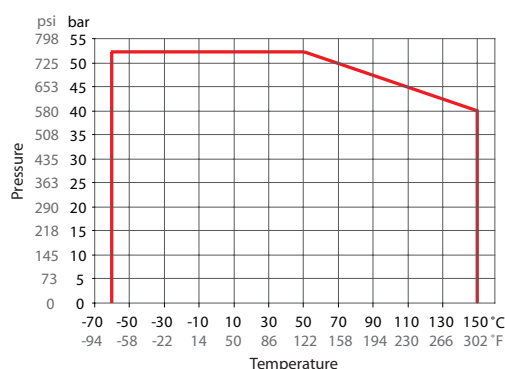
The valve cone has a built-in flexibility to ensure a precise and tight closing towards the valve seat.

A well balanced dampening effect between the piston and the cylinder gives an optimal protection during low loads and against pulsations.

## Features

- Applicable to HCFC, HFC, R717 (Ammonia), R744 (CO<sub>2</sub>), Propane, Butane, Iso-Butane and Ethane.  
R717 Heat Pump and Propylene applications with replaced O-ring.
- Designed to give favourable flow conditions.
- Internal backseating enables replacement of the spindle seal whilst the valve is active, i.e. under pressure (SCA-SS)
- Housing is made of special cold resistant stainless steel approved for low temperature operations.
- Easy to disassemble for inspection and service.
- Butt-weld DIN and ANSI connections.
- Max. operating pressure: 52 bar g (754 psig)
- Temperature range: -60/+150°C (-76 +302°F).
- Compact and light valves for easy handling and installation.
- Classification: DNV, CRN, BV, EAC etc.  
To get an updated list of certification on the products please contact your local Danfoss Sales Company.

## Pressure and temperature range



— SCA-X SS/CHV-X SS DN15-DN40

## Check & stop valves in stainless steel, type SCA-X SS - Check valves in stainless steel, type CHV-X SS

### Design

#### Connections

Available with the following connections:

- Butt-weld DIN (EN 10220)  
DN 15 - 40 (½ - 1½ in.)
- Butt-weld ANSI (B 36.19M)  
DN 20 - 40 (¾ - 1½ in.)

#### Housing

Made of stainless steel approved for low temperature operations.

#### Valve cone

Valve cone with built in metallic stop - prevents damage to teflon ring in case of overtightening.

#### Damping chamber

The chamber is filled with refrigerants (gas or liquid), which provides a damping effect when the valve opens and closes.

#### Spindle (SCA-X SS)

Made of polished stainless steel, which is ideal for O-ring sealing.

#### Packing Gland (SCA-X SS)

The "full temperature range" packing gland is the standard for the entire SVL platform.

This ensures perfect tightness throughout the whole temperature range:  
-60/+150°C (-76/+302°F).

#### Pressure Equipment Directive (PED)

The SCA-X SS/CHV-X SS valves are approved according to the European standard specified in the Pressure Equipment Directive and are CE marked.

For further details / restrictions - see the product instruction.

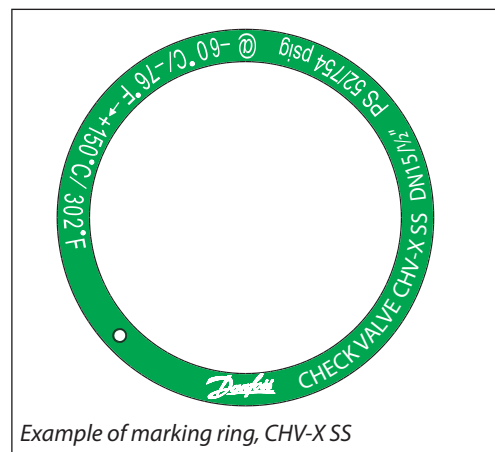
#### Installation

The valve must be mounted vertically with the cone downwards.

The valve is designed to resist very high internal pressure. However, the piping system in general should be designed to avoid liquid traps and reduce the risk of hydraulic pressure caused by thermal expansion.

For further information refer to installation instructions for SCA-X SS/CHV-X SS.

If cold refrigeration oil having low viscosity enters and settles in the damping chamber, problems with the check valve may arise. Consequently, it may be necessary to modify the valve for more viscous liquids by enlarging the hole to the damping chamber.



Example of marking ring, CHV-X SS



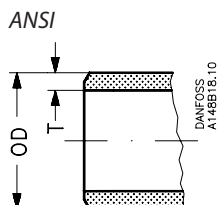
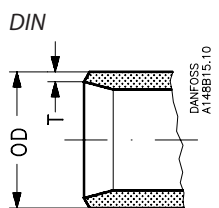
SCA-X SS/CHV-X SS valves		
Nominal bore	DN = < 25 mm (1 in.)	DN32-40 mm (1¼ - 1½ in.)
Classified for	Fluid group I	
Category	Article 3, paragraph 3	II

### Technical data

- **Refrigerants**  
Applicable to HCFC, HFC, R717 (Ammonia), R744 (CO<sub>2</sub>), Propane, Butane, Iso-Butane and Ethane.  
R717 Heat Pump and Propylene applications with replaced O-ring.  
For further information refer to the installation guide for SCA-X SS/CHV-X SS.
- **Temperature range**  
-60/+150°C (-76/+302°F).
- **Max. working pressure**  
52 bar g (754 psig).

Check & stop valves in stainless steel, type SCA-X SS - Check valves in stainless steel, type CHV-X SS

Connections



Size		OD	T
<b>Butt-weld DIN (EN 10220)</b>			
15	mm	21.3	2.3
½	in.	0.839	0.091
20	mm	26.9	2.3
¾	in.	1.059	0.091
25	mm	33.7	2.6
1	in.	1.327	0.103
32	mm	42.4	2.6
1¼	in.	1.669	0.102
40	mm	48.3	2.6
1½	in.	1.902	0.103

Size		OD	T
<b>Butt-weld ANSI (B 36.19M, SCHEDULE 40)</b>			
20	mm	26.9	2.9
¾	in.	1.06	0.11
25	mm	33.7	3.5
1	in.	1.33	0.14
32	mm	42.4	3.6
1¼	in.	1.67	0.14
40	mm	48.3	3.7
1½	in.	1.9	0.15

**Material specification**

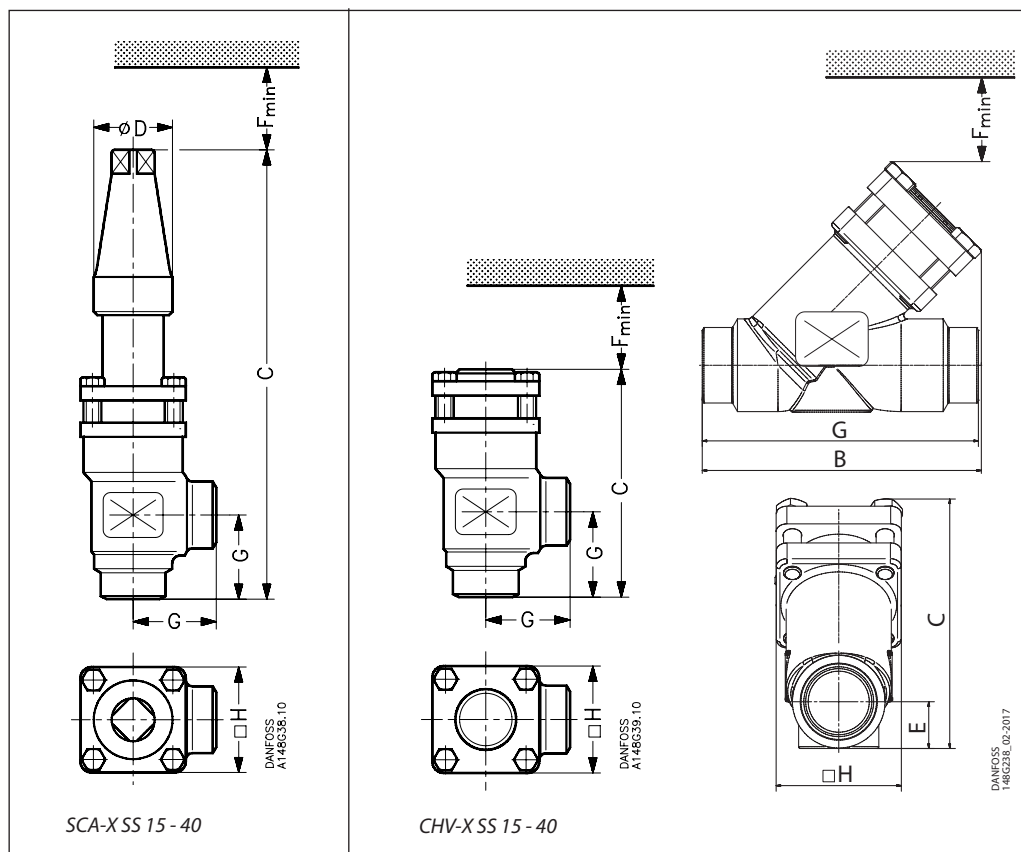
The image contains three technical cross-section drawings of Danfoss valves. The first drawing on the left is for the SCA-X SS 15-40 valve, showing a vertical spindle with a spring and a seal cap. The middle drawing is for the CHV-X SS 15-40 valve, showing a similar design but with a different internal spring mechanism. The third drawing on the right is another view of the CHV-X SS 15-40 valve, showing the bonnet and flange assembly. All drawings include numbered callouts from 1 to 17, corresponding to the parts listed in the table below.

No.	Part	Material	DIN/EN	ISO	ASTM
1	Housing	Stainless steel	GX5CrNi19-10 EN10213-4		AISI 304
2	Bonnet, Flange	Stainless steel	X5CrNi18-10 EN10088		AISI 304
3	Bonnet, Insert	Stainless steel	X8CrNiS18-9 DIN 17440		
4	Spindle	Stainless steel	X8CrNiS18-9 DIN 17440	Type 17, 17440	AISI 303
5	Cone	Steel Teflon (PTFE)			
6	O-ring	Cloroprene (Neoprene)			
7	Spindle extension	Steel			
8	Packing gland O-rings	Stainless steel Cloroprene (Neoprene)			
9	Packing washer	Aluminium			
10	Spring loaded seal	Teflon (PTFE)			
11	O-ring	Cloroprene (Neoprene)			
12	Bolts	Stainless steel	A2-70	A2-70	Type 308
13	Gasket	Fiber, non-asbestos			
14	Spring	Steel			
15	Identification ring	Stainless steel			
16	Seal cap gasket	Nylon			
17	Spindle seal cap	Aluminium			

Check & stop valves in stainless steel, type SCA-X SS - Check valves in stainless steel, type CHV-X SS

Dimensions and weights

SCA-X SS/CHV-X SS 15 - 40 (1/2 - 1 1/2 in.)



Valve size		C		G		ØD		F <sub>min</sub>		□H	Weight
<b>SCA-X SS 15 - 40</b>											
SCA-X SS 15 (1/2 in.)	mm in.	212 8.35		45 1.77		38 1.50		60 2.36		60 2.36	1.6 kg 3.53 lb
SCA-X SS 20 (3/4 in.)	mm in.	212 8.35		45 1.77		38 1.50		60 2.36		60 2.36	1.6 kg 3.53 lb
SCA-X SS 25 (1 in.)	mm in.	295 11.61		55 2.17		50 1.97		85 3.35		70 2.76	3.2 kg 7.05 lb
SCA-X SS 32 (1 1/4 in.)	mm in.	295 11.61		55 2.17		50 1.97		85 3.35		70 2.76	3.2 kg 7.05 lb
SCA-X SS 40 (1 1/2 in.)	mm in.	295 11.61		55 2.17		50 1.97		85 3.35		70 2.76	3.2 kg 7.05 lb

**CHV-X SS 15 - 40 Angleway**

CHV-X SS 15 (1/2 in.)	mm in.	103 4.06		45 1.77				60 2.36		60 2.36	1.2 kg 2.65 lb
CHV-X SS 20 (3/4 in.)	mm in.	103 4.06		45 1.77				60 2.36		60 2.36	1.2 kg 2.65 lb
CHV-X SS 25 (1 in.)	mm in.	143 5.63		55 2.17				85 3.35		70 2.76	2.3 kg 5.07 lb
CHV-X SS 32 (1 1/4 in.)	mm in.	143 5.63		55 2.17				85 3.35		70 2.76	2.3 kg 5.07 lb
CHV-X SS 40 (1 1/2 in.)	mm in.	143 5.63		55 2.17				85 3.35		70 2.76	2.3 kg 5.07 lb

Valve size		C	B	E		G		F <sub>min</sub>		□H	Weight
<b>CHV-X SS 15 - 40 Straightway</b>											
CHV-X SS 15 (1/2 in.)	mm in.	99 3.90	114 4.49	19 0.75		120 4.72		60 2.36		60 2.36	1.3kg 2.87lb
CHV-X SS 20 (3/4 in.)	mm in.	99 3.90	114 4.49	19 0.75		120 4.72		60 2.36		60 2.36	1.3kg 2.87lb
CHV-X SS 25 (1 in.)	mm in.	141 5.55	157 6.18	26 1.02		155 6.10		85 3.35		70 2.76	2.6kg 5.73lb
CHV-X SS 32 (1 1/4 in.)	mm in.	141 5.55	157 6.18	26 1.02		155 6.10		85 3.35		70 2.76	2.6kg 5.73lb
CHV-X SS 40 (1 1/2 in.)	mm in.	141 5.55	157 6.18	26 1.02		155 6.10		85 3.35		70 2.76	2.6kg 5.73lb

Specified weights are approximate values only.

## Check & stop valves in stainless steel, type SCA-X SS - Check valves in stainless steel, type CHV-X SS

### Ordering complete valves

#### How to order

The table below is used to identify the valve required.

For further information please contact your local Danfoss Sales Company.

Please note that the type codes only serve to identify the valves, some of which may not form part of the standard product range.

Valve type	SCA-X SS CHV-X SS	Stop Check Valve Check Valve
(valve size measured on the connection diameter)	<b>15</b>	DN 15
	<b>20</b>	DN 20
	<b>25</b>	DN 25
	<b>32</b>	DN 32
	<b>40</b>	DN 40
Connections	<b>D</b> <b>A</b>	Butt-weld connection: DIN EN 10220 Butt-weld connection: ANSI B 36.19M
Valve housing	<b>ANG</b>	Angle flow
	<b>STR</b>	Straight flow

#### Important!

Where products need to be certified according to specific certification societies the relevant information should be included at the time of order.

### SCA-X SS Angleway

#### Butt-weld DIN (EN 10220)

Size		Type	Code No.
mm	in.		
15	½	SCA-X SS 15 D ANG	148B5293
20	¾	SCA-X SS 20 D ANG	148B5381
25	1	SCA-X SS 25 D ANG	148B5490
32	1¼	SCA-X SS 32 D ANG	148B5585
40	1½	SCA-X SS 40 D ANG	148B5664

#### Butt-weld ANSI (B 36.19M SCHEDULE 40)

Size		Type	Code No.
mm	in.		
20	¾	SCA-X SS 20 A40 ANG	148B6489
25	1	SCA-X SS 25 A40 ANG	148B6480
32	1¼	SCA-X SS 32 A40 ANG	148B6490
40	1½	SCA-X SS 40 A40 ANG	148B5687

### CHV-X SS Angleway

#### Butt-weld DIN (EN 10220)

Size		Type	Code No.
mm	in.		
15	½	CHV-X SS 15 D ANG	148B5294
20	¾	CHV-X SS 20 D ANG	148B5382
25	1	CHV-X SS 25 D ANG	148B5491
32	1¼	CHV-X SS 32 D ANG	148B5586
40	1½	CHV-X SS 40 D ANG	148B5665

#### Butt-weld ANSI (B 36.19M SCHEDULE 40)

Size		Type	Code No.
mm	in.		
20	¾	CHV-X SS 20 A40 ANG	148B6491
25	1	CHV-X SS 25 A40 ANG	148B6481
32	1¼	CHV-X SS 32 A40 ANG	148B6492
40	1½	CHV-X SS 40 A40 ANG	148B5688

### CHV-X SS Straightway

#### Butt-weld DIN (EN 10220)

Size		Type	Code No.
mm	in.		
15	½	CHV-X SS 15 D STR	148B5678
20	¾	CHV-X SS 20 D STR	148B5679
25	1	CHV-X SS 25 D STR	148B5680
32	1¼	CHV-X SS 32 D STR	148B6544
40	1½	CHV-X SS 40 D STR	148B6566

#### Butt-weld ANSI (B 36.19M SCHEDULE 40)

Size		Type	Code No.
mm	in.		
20	¾	CHV-X SS 20 A40 STR	148B6608
25	1	CHV-X SS 25 A40 STR	148B6609
32	1¼	CHV-X SS 32 A40 STR	148B6610
40	1½	CHV-X SS 40 A40 STR	148B6611

ANG = Angleway  
STR = Straightway

Replacement kit (O-ring replacement) for R717 Ammonia Heat Pump\* and Propylene applications (including ID tag)

Size		O-ring kit for	
mm	in.	R717 Heat pump	R1270 Propylene
15	½	148B6070	148B6077
20	¾		
25	1	148B6071	148B6078
32	1¼		
40	1½		

\* Replacement kits for R717 Ammonia Heat Pump is applicable for continuous operating temperature between +100°C to 150°C (212°F to 302°F)



# Check valves

## Type NRVA

### Contents

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# Check valves

## Type NRVA



Check valve type NRVA can be used in liquid, suction and hot gas lines in refrigeration and air conditioning plant with ammonia.

NRVA can also be used in refrigerating systems with fluorinated refrigerants.

When the NRVA is used in liquid lines where cold, thick oil or impurities may be present, it is recommended that the standard spring be replaced by a special spring. See ordering table.

### Features

- Ensures correct direction of flow.
- Valve housing made of steel.
- Available for 40 bar g / 580 psig working pressure.
- Large range of flanges with connection dimensions in accordance with standards: DIN, ANSI, SOC, SA and FPT.
- Fitted with damping piston that makes the valves suitable for installation in lines where pulsation can occur, e.g. in the discharge line from the compressor.
- Classification: DNV, CRN, BV, EAC etc.  
To get an updated list of certification on the products please contact your local Danfoss Sales Company.

### Design

#### Connections

There is a very wide range of connection possibilities with NRVA check valves:

- Welding, DIN (2448)
- Welding, ANSI (B 36.10)
- Welding socket, ANSI (B 16.11)
- Solder connection, DIN (2856)
- Solder connection, ANSI (B 16.22)
- FPT internal thread, NPT (ANSI/ASME B 1.20.1)

#### Gaskets:

Do not contain asbestos.

#### Valve cone:

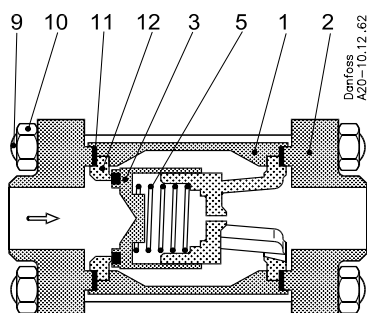
The valve cone has a teflon tightening ring. Teflon tightening ring renders perfect sealing at a minimum closing force.

## Check valves, type NRVA

### Technical data

- Refrigerants**  
 Applicable to HCFC, HFC and R717 (Ammonia).  
 For further information please see installation instruction for NRVA.  
 Use with flammable hydrocarbons cannot be recommended; please contact Danfoss.
- Temperature range**  
 -50 – 140 °C / -58 – 284 °F.
- Pressure range**  
 The valve is designed for:  
 Max. working pressure: 40 bar g / 580 psig.

### Material specification

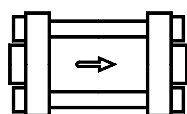


#### Material specification for NRVA check valves

No.	Part	Material	DIN	ISO	ASTM
1	Housing	Steel	G20Mn5QT *) EN10213-3 ----- P285QH EN10222-4		LCC, A352 ----- LF2,A350
2	Flanges	Steel	RSt. 37-2, 10025	Fe360 B, 630	Grade C, A 283
3	Valve cone	Stainless steel Teflon			
5	Spring	Steel			
9	Bolts	Stainless steel	A2-70		
10	Nut	Stainless steel			
11	Gasket	Non asbestos			
12	Valve seat	Steel			

\*) NRVA 40 / NRVA 50 housing material is TTSt 35N until January 2006

### Ordering



#### Complete valves incl. DIN 2448 flange:

Type	Weld flange connection [in]	Code no.		$\Delta p$ <sup>2)</sup>				$k_v$ value <sup>3)</sup> [m <sup>3</sup> /h]	$C_v$ value <sup>4)</sup> [gal/min]
		Valve	Spec. spring <sup>1)</sup>	With standard spring		With spec. spring <sup>1)</sup>			
				[bar]	[psig]	[bar]	[psig]		
NRVA 15	1/2	<b>020-2000</b>	<b>020-2307</b>	0.12	1.7	0.3	4.4	5	6
NRVA 20	3/4	<b>020-2001</b>	<b>020-2307</b>	0.12	1.7	0.3	4.4	6	7
NRVA 25	1	<b>020-2002</b>	<b>020-2317</b>	0.12	1.7	0.3	4.4	19	22
NRVA 32	1 1/4	<b>020-2003</b>	<b>020-2317</b>	0.12	1.7	0.3	4.4	20	23
NRVA 40	1 1/2	<b>020-2004</b>	<b>020-2327</b>	0.07	1.0	0.4	5.8	44	51
NRVA 50	2	<b>020-2005</b>	<b>020-2327</b>	0.07	1.0	0.4	5.8	44	51
NRVA 65	2 1/2	<b>020-2006</b>	<b>020-2337</b>	0.07	1.0	0.4	5.8	75	87

<sup>1)</sup> A special type spring can be supplied to replace the standard valve spring.

<sup>2)</sup>  $\Delta p$  = the minimum pressure differential at which the valve is completely open.

<sup>3)</sup> The  $k_v$  value is the flow of water in m<sup>3</sup>/h at a pressure drop across valve of 1 bar,  $\rho = 1000 \text{ kg/m}^3$ .

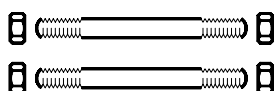
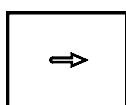
<sup>4)</sup> The  $C_v$  value is the flow of water in gal/min at a pressure drop across valve of 1 psig,  $\rho = 10 \text{ lbs/gal}$ .

#### Valve body without flanges:

Type	Code no.
NRVA 15	<b>020-2020</b>
NRVA 20	<b>020-2020</b>
NRVA 25	<b>020-2022</b>
NRVA 32	<b>020-2022</b>
NRVA 40	<b>020-2024</b>
NRVA 50	<b>020-2024</b>
NRVA 65	<b>020-2026</b>

#### Staybolts and gaskets

Type	Dimensions	Code no.
NRVA 15 / 20	M 12 × 115 mm	<b>006-1107</b>
NRVA 25 / 32	M 12 × 148 mm	<b>006-1135</b>
NRVA 40 / 50	M 12 × 167 mm	<b>006-1137</b>
NRVA 65	M 16 × 200 mm	<b>006-1138</b>



## Check valves, type NRVA

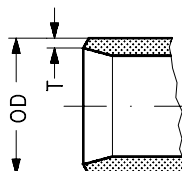
### Flange connections

Danfoss flange sets excluding gaskets, bolts and nuts, are specially made for the Danfoss product range and must only be used for the purpose described.

Select the valve based on capacity and then select the size of flanges most suitable for the application, which can be mounted on the valve.

Size [mm]	Size [in]	OD [mm]	T [mm]	OD [in]	T [in]	Flange type	For use with valve housing size	Code no.
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DIN

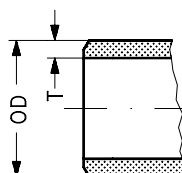


#### Butt welding DIN (2448)

10	3/8	18	2	0.710	0.079	1.3	NRVA 15/20	027N1112
15	1/2	22	2.5	0.866	0.098	1.3	NRVA 15/20	027N1115
20	3/4	26.9	2.3	1.059	0.091	1.3	NRVA 15/20	027N1120
25	1	33.7	2.6	1.327	0.103	4	NRVA 25/32	027N1026
32	1 1/4	42.4	2.6	1.669	0.102	4	NRVA 25/32	027N1033
40	1 1/2	48.3	2.6	1.902	0.103	6	NRVA 40/50	027N1042
50	2	60.3	2.9	2.370	0.110	6	NRVA 40/50	027N1051
65	2 1/2	76.1	2.9	3.000	0.110	8	NRVA 65	027N1055

Size [mm]	Size [in]	OD [mm]	T [mm]	OD [in]	T [in]	Flange type	For use with valve housing size	Code no.
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ANSI

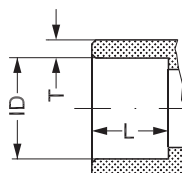


#### Butt welding ANSI B 36.10

10	3/8	17.2	3.2	0.677	0.126	1.3	NRVA 15/20	027N2020
15	1/2	21.3	3.7	0.839	0.146	1.3	NRVA 15/20	027N2021
20	3/4	26.9	4.0	1.059	0.158	1.3	NRVA 15/20	027N2022
25	1	33.7	4.6	1.327	0.181	4	NRVA 25/32	027N2023
32	1 1/4	42.4	4.9	1.669	0.193	4	NRVA 25/32	027N2024
40	1 1/2	48.3	5.1	1.902	0.201	6	NRVA 40/50	027N2025
50	2	60.3	3.9	2.370	0.150	6	NRVA 40/50	027N2026
65	2 1/2	73.0	5.2	3.000	0.200	8	NRVA 65	027N2027

Size [mm]	Size [in]	ID [mm]	T [mm]	ID [in]	T [in]	L [mm]	L [in]	Flange type	For use with valve housing size	Code no.
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SOC

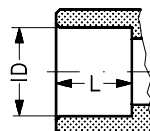


#### Socket welding ANSI (B 16.11)

10	3/8	17.8	4.1	0.701	0.161	10	0.394	1.3	NRVA 15/20	027N2010
15	1/2	22	4.8	0.866	0.189	10	0.394	1.3	NRVA 15/20	027N2011
20	3/4	27.4	5.0	1.079	0.197	13	0.512	4	NRVA 25/32	027N2012
25	1	34.1	5.8	1.343	0.228	13	0.512	4	NRVA 25/32	027N2013
32	1 1/4	42.9	6.0	1.689	0.236	13	0.512	4	NRVA 25/32	027N2016
40	1 1/2	49.0	6.5	1.929	0.254	13	0.512	6	NRVA 40/50	027N2015

Size [mm]	Size [in]	ID [mm]	ID [in]	L [mm]	L [in]	Flange type	For use with valve housing size	Code no.
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SA



#### Soldering DIN (2856)

16		16.07				15		1.3	NRVA 15/20	027L1116
22		22.08				22		1.3	NRVA 15/20	027L1122
35		35.07				25		4	NRVA 25/32	027L2335
54		54.09				33		4	NRVA 40/50	027L2554

#### Soldering (ANSI B 16.22)

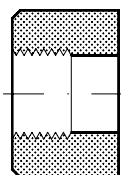
	5/8			0.628			0.807	1.3	NRVA 15/20	027L1117
	7/8			0.878			0.866	1.3	NRVA 15/20	027L1123
	1 3/8			1.375			0.984	4	NRVA 25/32	027L2335
	2 1/8			2.125			1.300	4	NRVA 40/50	027L2554

To be continued next page.

## Check valves, type NRVA

### Flange connections (Continued)

FPT



Size [mm]	Size [in]	Inside pipe thread	Flange type	For use with valve housing size	Code no.
-----------	-----------	--------------------	-------------	---------------------------------	----------

*FPT inside pipe thread, NPT (ANSI/ASME B 1.20.1)*

10	3/8	(3/8 × 18 NPT)	1.3	NRVA 15/20	<b>027G1005</b>
15	1/2	(1/2 × 14 NPT)	1.3	NRVA 15/20	<b>027G1006</b>
20	3/4	(3/4 × 14 NPT)	4	NRVA 25/32	<b>027G1007</b>

#### Example

NRVA 32 with 1 1/4" flanges for ANSI butt welding:

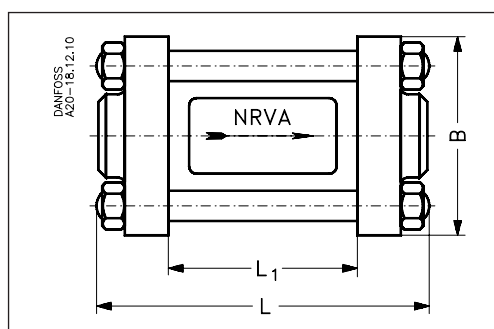
NRVA 32 + bolts + flanges (set) =  
020-2022 + 006-1135 + 027N2024



#### NOTE:

The flanges sets are exclusive gaskets, bolts and nuts.

### Dimensions and weights

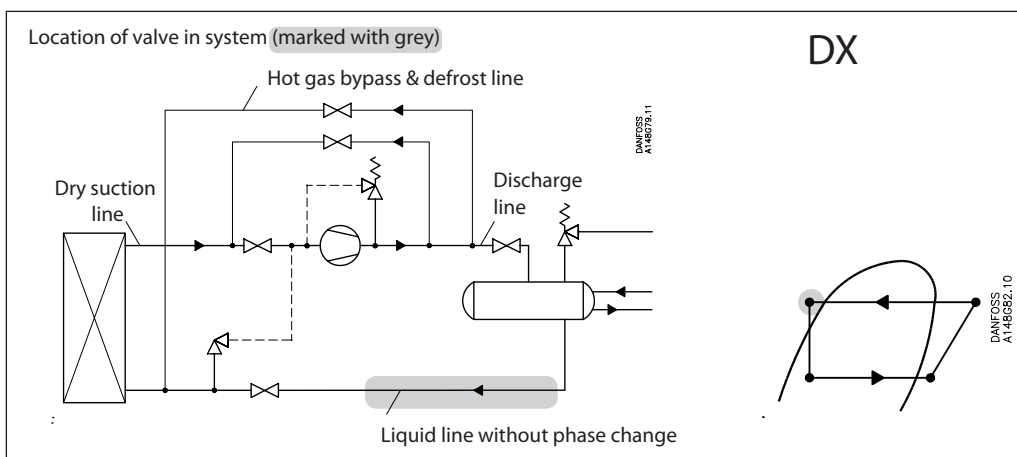
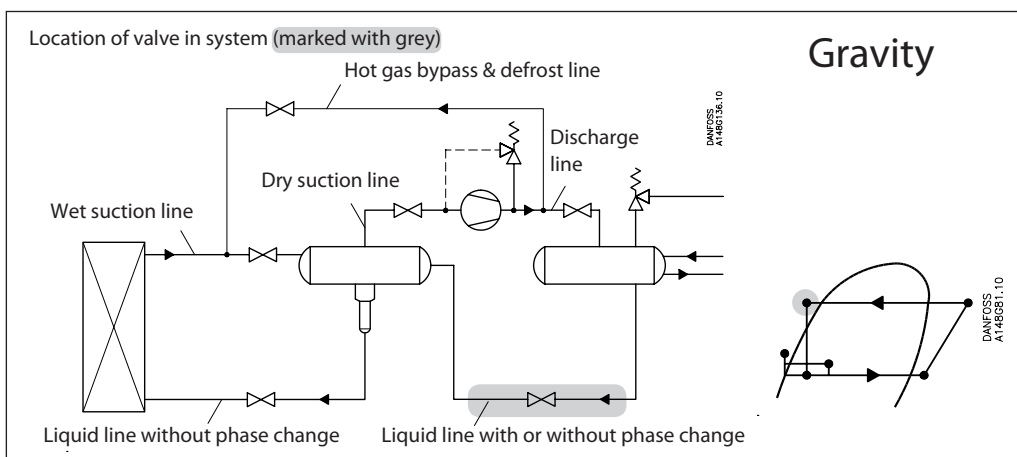
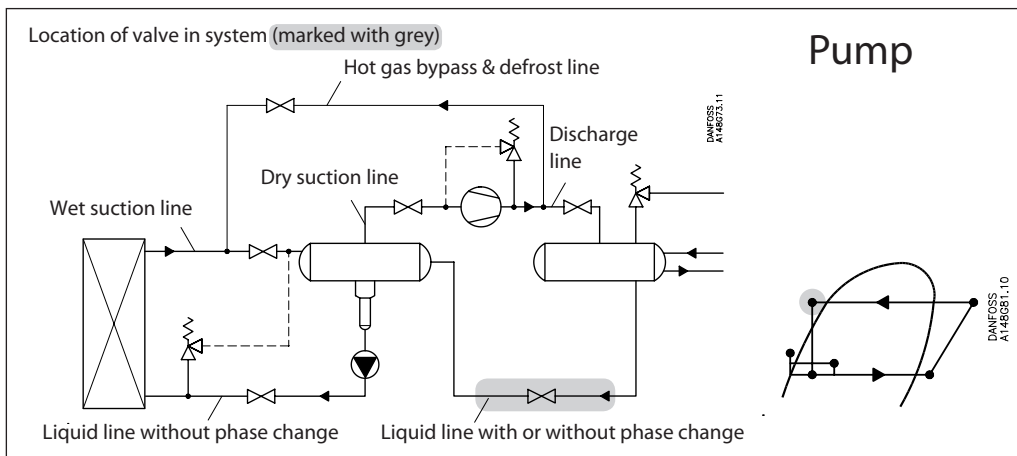


Type	L	L <sub>1</sub> <sup>1)</sup>	B	Weight	
NRVA 15 – 20	[mm]	115	50	80	1.4 kg
	[in]	4.53	1.97	3.15	3.09 lb
NRVA 25 – 32	[mm]	138	74	∅ 83	3.0 kg
	[in]	5.43	2.91	∅ 3.27	6.61 lb
NRVA 40 – 50	[mm]	172	94.5	∅ 103	5.0 kg
	[in]	6.77	3.72	∅ 4.05	11.02 lb
NRVA 65	[mm]	226	124	∅ 185	13.0 kg
	[in]	8.90	4.88	∅ 7.28	28.66 lb

<sup>1)</sup> Without flanges

Nominal capacities

Liquid line with/without phase change



Nominal capacities

Liquid line with / without phase change

SI units

Calculation example (R 134a capacities):

Running conditions in a plant are as follows:

$T_e = -20\text{ °C}$   
 $Q_o = 300\text{ kW}$   
 $T_{liq} = 10\text{ °C}$   
 Max.  $\Delta P = 0.3\text{ bar}$

The capacity table is based on nominal conditions ( $\Delta P = 0.2\text{ bar}$ ,  $T_{liq} = 30\text{ °C}$ ).

The actual capacity must therefore be corrected to a nominal condition by multiplication with correction factors.

Correction factor for  $\Delta P\ 0.3\text{ bar}$   $f_{\Delta P} = 0.82$ .

Correction factor for liquid temperature  $f_{T_{liq}} = 0.82$ .

$$Q_n = Q_o \times f_{\Delta P} \times f_{T_{liq}} = 300 \times 0.82 \times 0.82 = 202\text{ kW.}$$

From the capacity table a NRVA 25 with  $Q_n = 370\text{ kW}$  is the correct selection for the application.

US units

Calculation example (R 134a capacities):

Running conditions in a plant are as follows:

$T_e = -20\text{ °F}$   
 $Q_o = 130\text{ TR}$   
 $T_{liq} = 50\text{ °F}$   
 Max.  $\Delta P = 5\text{ psi}$

The capacity table is based on nominal conditions ( $\Delta P = 3\text{ psi}$ ,  $T_{liq} = 90\text{ °F}$ ).

The actual capacity must therefore be corrected to a nominal condition by multiplication with correction factors.

Correction factor for  $\Delta P\ 5\text{ psi}$ ,  $f_{\Delta P} = 0.79$

Correction factor for liquid temperature  $f_{T_{liq}} = 0.81$ .

$$Q_n = Q_o \times f_{\Delta P} \times f_{T_{liq}} = 130 \times 0.79 \times 0.81 = 83.2\text{ TR}$$

From the capacity table a NRVA 25 with  $Q_n = 100\text{ TR}$  is the correct selection for the application.



## Check valves, type NRVA

### Nominal capacities

### Liquid line with/without phase change

#### R 717

#### SI units

Capacity table for nominal conditions,  $Q_N$  [kW],  
 $T_{liq} = 30\text{ °C}$ ,  
 $\Delta P = 0.2\text{ bar}$

Type	$k_v$ [m <sup>3</sup> /h]	Evaporating temperature $T_e$							
		-50 °C	-40 °C	-30 °C	-20 °C	-10 °C	0 °C	10 °C	20 °C
NRVA 15	5	504	512	519	526	532	537	542	546
NRVA 20	6	605	614	623	631	638	645	651	655
NRVA 25	19	1916	1945	1973	1998	2022	2042	2060	2075
NRVA 32	20	2016	2048	2077	2104	2128	2150	2169	2185
NRVA 40	44	4436	4505	4569	4628	4682	4730	4771	4806
NRVA 50	44	4436	4505	4569	4628	4682	4730	4771	4806
NRVA 65	75	7562	7678	7787	7889	7981	8062	8133	8192

#### Correction factor for $\Delta P$ ( $f_{\Delta P}$ )

$\Delta P$ (bar)	Correction factor
<b>0.2</b>	<b>1.00</b>
0.25	0.89
0.3	0.82
0.4	0.71
0.5	0.63
0.6	0.58

#### Correction factor for liquid temperature ( $T_{liq}$ )

Liquid temperature	Correction factor
-20 °C	0.82
-10 °C	0.86
0 °C	0.88
10 °C	0.92
20 °C	0.96
<b>30 °C</b>	<b>1.00</b>
40 °C	1.04
50 °C	1.09

#### R 717

#### US units

Capacity table for nominal conditions,  $Q_N$  [Tons of Refrigeration],  
 $T_{liq} = 90\text{ °F}$ ,  
 $\Delta P = 3\text{ psi}$

Type	$C_v$ [USgal/min]	Evaporating temperature $T_e$							
		-60 °F*	-40 °F	-20 °F	0 °F	20 °F	40 °F	60 °F	80 °F
NRVA 15	6	143.9	145.9	147.7	149.2	150.6	151.7	152.5	153.0
NRVA 20	7	173	175	177	179	181	182	183	184
NRVA 25	22	547	554	561	567	572	576	580	581
NRVA 32	23	576	583	591	597	602	607	610	612
NRVA 40	51	1266	1284	1300	1313	1325	1335	1342	1347
NRVA 50	51	1266	1284	1300	1313	1325	1335	1342	1347
NRVA 65	87	2158	2188	2215	2239	2259	2276	2288	2295

\* 2 °F below min. operating temperature.

#### Correction factor for $\Delta P$ ( $f_{\Delta P}$ )

$\Delta P$ (psi)	Correction factor
<b>3</b>	<b>1.00</b>
4	0.87
5	0.79
6	0.72
7	0.66
8	0.62

#### Correction factor for liquid temperature ( $T_{liq}$ )

Liquid temperature	Correction factor
-10 °F	0.82
10 °F	0.85
30 °F	0.88
50 °F	0.92
70 °F	0.96
<b>90 °F</b>	<b>1.00</b>
110 °F	1.04
130 °F	1.09

## Check valves, type NRVA

### Nominal capacities

### Liquid line with / without phase change

### SI units

Capacity table for nominal conditions,  $Q_N$  [kW],  
 $T_{liq} = 30\text{ °C}$ ,  
 $\Delta P = 0.2\text{ bar}$

### R 22

Type	$k_v$ [m <sup>3</sup> /h]	Evaporating temperature $T_e$							
		-50 °C	-40 °C	-30 °C	-20 °C	-10 °C	0 °C	10 °C	20 °C
NRVA 15	5	99	102	105	108	111	114	116	118
NRVA 20	6	119	123	126	130	133	136	139	142
NRVA 25	19	376	389	400	411	422	431	440	448
NRVA 32	20	396	409	421	433	444	454	463	472
NRVA 40	44	872	900	927	952	977	999	1020	1038
NRVA 50	44	872	900	927	952	977	999	1020	1038
NRVA 65	75	1486	1534	1580	1623	1665	1703	1738	1769

#### Correction factor for $\Delta P$ ( $f_{\Delta P}$ )

$\Delta P$ (bar)	Correction factor
<b>0.2</b>	<b>1.00</b>
0.25	0.89
0.3	0.82
0.4	0.71
0.5	0.63
0.6	0.58

#### Correction factor for liquid temperature ( $T_{liq}$ )

Liquid temperature	Correction factor
-20 °C	0.71
-10 °C	0.75
0 °C	0.80
10 °C	0.86
20 °C	0.92
<b>30 °C</b>	<b>1.00</b>
40 °C	1.09
50 °C	1.22

### US units

Capacity table for nominal conditions,  $Q_N$  [Tons of Refrigeration],  
 $T_{liq} = 90\text{ °F}$ ,  
 $\Delta P = 3\text{ psi}$

### R 22

Type	$C_v$ [USgal/min]	Evaporating temperature $T_e$							
		-60 °F*	-40 °F	-20 °F	0 °F	20 °F	40 °F	60 °F	80 °F
NRVA 15	6	28	29	30	31	32	32	33	34
NRVA 20	7	34	35	36	37	38	39	40	41
NRVA 25	22	106	110	114	117	120	123	126	129
NRVA 32	23	112	116	120	123	127	130	133	135
NRVA 40	51	246	255	263	271	279	286	292	298
NRVA 50	51	246	255	263	271	279	286	292	298
NRVA 65	87	419	434	449	462	475	487	498	507

\* 2 °F below min. operating temperature.

#### Correction factor for $\Delta P$ ( $f_{\Delta P}$ )

$\Delta P$ (psi)	Correction factor
<b>3</b>	<b>1.00</b>
4	0.87
5	0.79
6	0.72
7	0.66
8	0.62

#### Correction factor for liquid temperature ( $T_{liq}$ )

Liquid temperature	Correction factor
-10 °F	0.73
10 °F	0.77
30 °F	0.82
50 °F	0.87
70 °F	0.93
<b>90 °F</b>	<b>1.00</b>
110 °F	1.09
130 °F	1.20

**Check valves, type NRVA**

**Nominal capacities**

**Liquid line with/without phase change**

**R 134a**

**SI units**

Capacity table for nominal conditions,  $Q_N$  [kW],  
 $T_{liq} = 30\text{ °C}$ ,  
 $\Delta P = 0.2\text{ bar}$

Type	$k_v$ [m <sup>3</sup> /h]	Evaporating temperature $T_e$							
		-50 °C	-40 °C	-30 °C	-20 °C	-10 °C	0 °C	10 °C	20 °C
NRVA 15	5	89	93	97	101	105	109	113	36
NRVA 20	6	107	112	117	122	127	131	136	68
NRVA 25	19	338	354	370	385	401	415	429	90
NRVA 32	20	356	373	390	406	422	437	452	158
NRVA 40	44	783	820	857	893	928	962	994	260
NRVA 50	44	783	820	857	893	928	962	994	389
NRVA 65	75	1335	1398	1461	1522	1582	1639	1695	678

**Correction factor for  $\Delta P$  ( $f_{\Delta P}$ )**

$\Delta P$ (bar)	Correction factor
<b>0.2</b>	<b>1.00</b>
0.25	0.89
0.3	0.82
0.4	0.71
0.5	0.63
0.6	0.58

**Correction factor for liquid temperature ( $T_{liq}$ )**

Liquid temperature	Correction factor
-20 °C	0.66
-10 °C	0.70
0 °C	0.76
10 °C	0.82
20 °C	0.90
<b>30 °C</b>	<b>1.00</b>
40 °C	1.13
50 °C	1.29

**R 134a**

**US units**

Capacity table for nominal conditions,  $Q_N$  [Tons of Refrigeration],  
 $T_{liq} = 90\text{ °F}$ ,  
 $\Delta P = 3\text{ psi}$

Type	$C_v$ [USgal/min]	Evaporating temperature $T_e$							
		-60 °F*	-40 °F	-20 °F	0 °F	20 °F	40 °F	60 °F	80 °F
NRVA 15	6	25	26	28	29	30	32	33	10
NRVA 20	7	30	32	33	35	36	38	39	20
NRVA 25	22	95	100	105	110	115	120	124	26
NRVA 32	23	100	106	111	116	121	126	131	46
NRVA 40	51	220	232	244	255	266	278	288	75
NRVA 50	51	220	232	244	255	266	278	288	112
NRVA 65	87	376	396	416	435	454	473	490	196

\* 2 °F below min. operating temperature.

**Correction factor for  $\Delta P$  ( $f_{\Delta P}$ )**

$\Delta P$ (psi)	Correction factor
<b>3</b>	<b>1.00</b>
4	0.87
5	0.79
6	0.72
7	0.66
8	0.62

**Correction factor for liquid temperature ( $T_{liq}$ )**

Liquid temperature	Correction factor
-10 °F	0.64
10 °F	0.68
30 °F	0.74
50 °F	0.81
70 °F	0.89
<b>90 °F</b>	<b>1.00</b>
110 °F	1.15
130 °F	1.35

## Check valves, type NRVA

### Nominal capacities

### Liquid line with/without phase change

### SI units

Capacity table for nominal conditions,  $Q_N$  [kW],  
 $T_{liq} = 30\text{ °C}$ ,  
 $\Delta P = 0.2\text{ bar}$

#### R 404A

Type	$k_v$ [m <sup>3</sup> /h]	Evaporating temperature $T_e$							
		-50 °C	-40 °C	-30 °C	-20 °C	-10 °C	0 °C	10 °C	20 °C
NRVA 15	5	57.2	61.3	65.3	69.2	73.0	76.6	79.9	82.8
NRVA 20	6	68.7	73.6	78.4	83.1	87.6	91.9	95.8	99.4
NRVA 25	19	217.5	232.9	248.2	263.1	277.4	290.9	303.5	314.7
NRVA 32	20	228.9	245.2	261.3	276.9	292.0	306.3	319.5	331.2
NRVA 40	44	503.6	539.4	574.8	609.2	642.4	673.8	702.8	728.7
NRVA 50	44	503.6	539.4	574.8	609.2	642.4	673.8	702.8	728.7
NRVA 65	75	858.5	919.4	979.7	1038.4	1094.9	1148.5	1198.0	1242.1

#### Correction factor for $\Delta P$ ( $f_{\Delta P}$ )

$\Delta P$ (bar)	Correction factor
<b>0.2</b>	<b>1.00</b>
0.25	0.89
0.3	0.82
0.4	0.71
0.5	0.63
0.6	0.58

#### Correction factor for liquid temperature ( $T_{liq}$ )

Liquid temperature	Correction factor
-20 °C	0.55
-10 °C	0.60
0 °C	0.66
10 °C	0.74
20 °C	0.85
<b>30 °C</b>	<b>1.00</b>
40 °C	1.23
50 °C	1.68

### US units

Capacity table for nominal conditions,  $Q_N$  [Tons of Refrigeration],  
 $T_{liq} = 90\text{ °F}$ ,  
 $\Delta P = 3\text{ psi}$

#### R 404A

Type	$C_v$ [USgal/min]	Evaporating temperature $T_e$							
		-60 °F*	-40 °F	-20 °F	0 °F	20 °F	40 °F	60 °F	80 °F
NRVA 15	6	15.7	17.0	18.2	19.5	20.7	21.8	22.8	23.7
NRVA 20	7	18.8	20.4	21.9	23.4	24.8	26.1	27.4	28.4
NRVA 25	22	59.6	64.5	69.3	74.0	78.5	82.7	86.8	89.9
NRVA 32	23	62.8	67.9	73.0	77.9	82.6	87.0	91.3	94.7
NRVA 40	51	138.1	149.4	160.6	171.4	181.7	191.4	200.9	208.2
NRVA 50	51	138.1	149.4	160.6	171.4	181.7	191.4	200.9	208.2
NRVA 65	87	235.4	254.7	273.7	292.2	309.8	326.3	342.5	355.0

\* 2 °F below min. operating temperature.

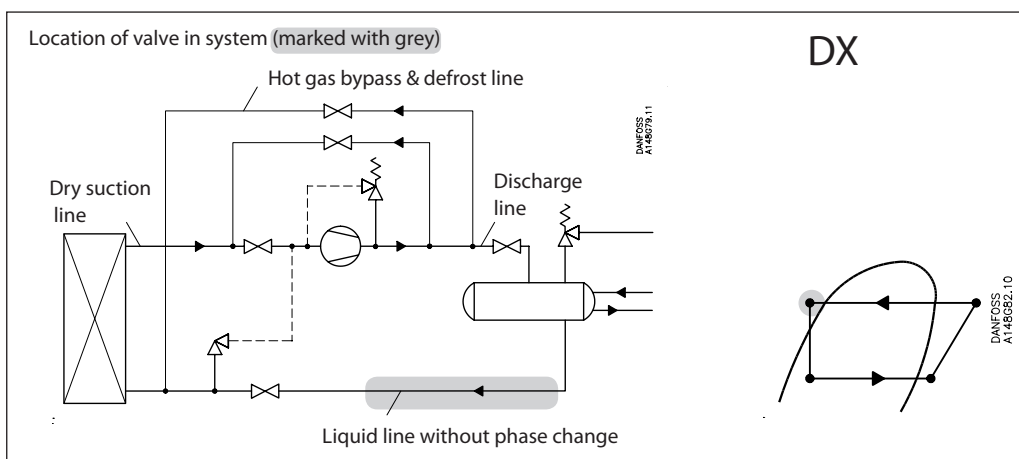
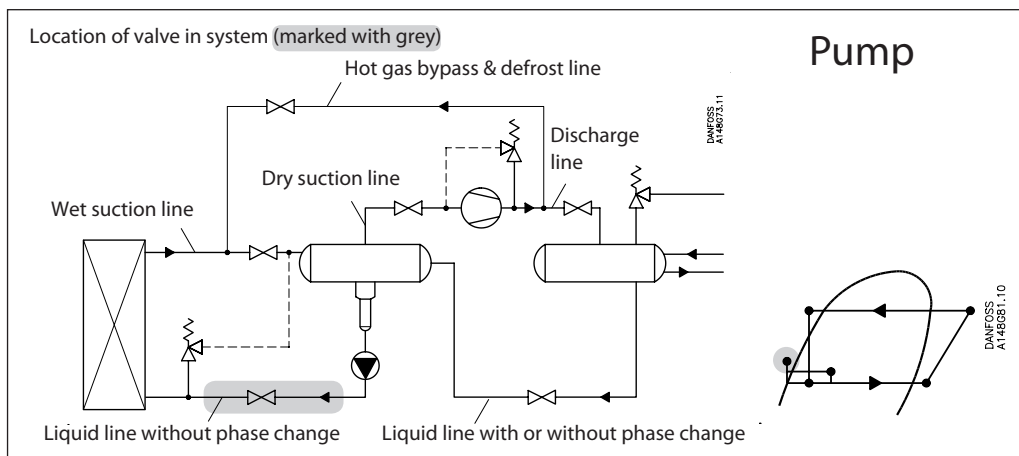
#### Correction factor for $\Delta P$ ( $f_{\Delta P}$ )

$\Delta P$ (psi)	Correction factor
<b>3</b>	<b>1.00</b>
4	0.87
5	0.79
6	0.72
7	0.66
8	0.62

#### Correction factor for liquid temperature ( $T_{liq}$ )

Liquid temperature	Correction factor
-10 °F	0.52
10 °F	0.57
30 °F	0.63
50 °F	0.72
70 °F	0.83
<b>90 °F</b>	<b>1.00</b>
110 °F	1.29
130 °F	1.92

## Liquid line without phase change



**Nominal capacities****Liquid line without phase change****SI units**

Calculation example (R 134a capacities):

Running conditions in a plant are as follows:

$T_e = -20\text{ °C}$   
 $Q_0 = 300\text{ kW}$   
circulation rate = 3  
Max.  $\Delta P = 0.3\text{ bar}$

The capacity table is based on nominal conditions (pressure drop  $\Delta P = 0.2\text{ bar}$ , circulation rate = 4).

The actual capacity must therefore be corrected to a nominal condition by multiplication with correction factors.

Correction factor for  $\Delta P\ 0.3\text{ bar}$   $f_{\Delta P} = 0.82$ Correction factor for circulation rate  $f_{rec} = 0.75$ .

$$Q_n = Q_0 \times f_{\Delta P} \times f_{rec} = 300 \times 0.82 \times 0.75 = 184.5\text{ kW}$$

From the capacity table a NRVA 40 with  $Q_n = 336\text{ kW}$  is the correct selection for the application.

**US units**

Calculation example (R 134a capacities):

Running conditions in a plant are as follows:

$T_e = -20\text{ °F}$   
 $Q_0 = 130\text{ TR}$   
Circulation rate = 3  
Max.  $\Delta P = 5\text{ psi}$

The capacity table is based on nominal conditions (pressure drop  $\Delta p = 3\text{ psi}$ , circulation rate = 4).

The actual capacity must therefore be corrected to a nominal condition by multiplication with correction factors.

Correction factor for  $\Delta P\ 5\text{ psi}$   $f_{\Delta p} = 0.79$ Correction factor for circulation rate  $f_{rec} = 0.75$ .

$$Q_n = Q_0 \times f_{\Delta p} \times f_{circ} = 130 \times 0.79 \times 0.75 = 77.0\text{ TR}$$

From the capacity table a NRVA 40 with  $Q_n = 101\text{ TR}$  is the correct selection for the application.

Check valves, type NRVA

Nominal capacities

Liquid line without phase change

R 717

SI units

Capacity table for nominal conditions,  $Q_N$  [kW], circulation rate = 4,  $\Delta P = 0.2$  bar

Type	$k_v$ [m <sup>3</sup> /h]	Evaporating temperature $T_e$							
		-50 °C	-40 °C	-30 °C	-20 °C	-10 °C	0 °C	10 °C	20 °C
NRVA 15	5	182.5	177.1	171.9	166.4	160.7	154.9	148.8	142.5
NRVA 20	6	219	213	206	200	193	186	179	171
NRVA 25	19	693	673	653	632	611	589	566	541
NRVA 32	20	730	708	687	665	643	620	595	570
NRVA 40	44	1606	1559	1512	1464	1414	1363	1310	1254
NRVA 50	44	1606	1559	1512	1464	1414	1363	1310	1254
NRVA 65	75	2737	2657	2578	2495	2411	2324	2232	2137

Correction factor for  $\Delta P$  ( $f_{\Delta P}$ )

$\Delta P$ (bar)	Correction factor
<b>0.2</b>	<b>1.00</b>
0.25	0.89
0.3	0.82
0.4	0.71
0.5	0.63
0.6	0.58

Correction factor for circulation rate ( $f_{rec}$ )

Circulation rate	Correction factor
2	0.5
3	0.75
<b>4</b>	<b>1</b>
6	1.5
8	2
10	2.5

US units

Capacity table for nominal conditions,  $Q_N$  [Tons of Refrigeration], circulation rate = 4,  $\Delta P = 3$  psi

R 717

Type	$C_v$ [USgal/min]	Evaporating temperature $T_e$							
		-60 °F*	-40 °F	-20 °F	0 °F	20 °F	40 °F	60 °F	80 °F
NRVA 15	6	52.8	51.1	49.5	47.8	45.9	44.0	41.9	39.8
NRVA 20	7	63.3	61.4	59.4	57.4	55.1	52.8	50.3	47.8
NRVA 25	22	200.5	194.4	188.2	181.7	174.5	167.3	159.2	151.4
NRVA 32	23	211	205	198	191	184	176	168	159
NRVA 40	51	464	450	436	421	404	387	369	351
NRVA 50	51	464	450	436	421	404	387	369	351
NRVA 65	87	792	767	743	717	689	660	628	598

\* 2 °F below min. operating temperature.

Correction factor for  $\Delta P$  ( $f_{\Delta P}$ )

$\Delta P$ (psi)	Correction factor
<b>3</b>	<b>1.00</b>
4	0.87
5	0.79
6	0.72
7	0.66
8	0.62

Correction factor for circulation rate ( $f_{rec}$ )

Circulation rate	Correction factor
2	0.5
3	0.75
<b>4</b>	<b>1</b>
6	1.5
8	2
10	2.5

## Check valves, type NRVA

### Nominal capacities

### Liquid line without phase change

### SI units

Capacity table for nominal conditions,  $Q_N$  [kW], circulation rate = 4,  $\Delta P = 0.2$  bar

### R 22

Type	$k_v$ [m <sup>3</sup> /h]	Evaporating temperature $T_e$							
		-50 °C	-40 °C	-30 °C	-20 °C	-10 °C	0 °C	10 °C	20 °C
NRVA 15	5	45	43	41	40	38	36	34	32
NRVA 20	6	53	52	50	48	46	43	41	39
NRVA 25	19	169	163	157	151	144	137	130	122
NRVA 32	20	178	172	166	159	152	145	137	128
NRVA 40	44	392	378	364	350	334	318	301	283
NRVA 50	44	392	378	364	350	334	318	301	283
NRVA 65	75	668	645	621	596	570	542	513	482

#### Correction factor for $\Delta P$ ( $f_{\Delta P}$ )

$\Delta P$ (bar)	Correction factor
<b>0.2</b>	<b>1.00</b>
0.25	0.89
0.3	0.82
0.4	0.71
0.5	0.63
0.6	0.58

#### Correction factor for circulation rate ( $f_{rec}$ )

Circulation rate	Correction factor
2	0.5
3	0.75
<b>4</b>	<b>1</b>
6	1.5
8	2
10	2.5

### US units

Capacity table for nominal conditions,  $Q_N$  [Tons of Refrigeration], circulation rate = 4,  $\Delta P = 3$  psi

### R 22

Type	$C_v$ [USgal/min]	Evaporating temperature $T_e$							
		-60 °F*	-40 °F	-20 °F	0 °F	20 °F	40 °F	60 °F	80 °F
NRVA 15	6	12.9	12.4	11.9	11.4	10.8	10.2	9.5	8.8
NRVA 20	7	15	15	14	14	13	12	11	11
NRVA 25	22	49	47	45	43	41	39	36	34
NRVA 32	23	52	50	48	46	43	41	38	35
NRVA 40	51	114	109	105	100	95	90	84	78
NRVA 50	51	114	109	105	100	95	90	84	78
NRVA 65	87	193	186	179	171	162	153	143	133

\* 2 °F below min. operating temperature.

#### Correction factor for $\Delta P$ ( $f_{\Delta P}$ )

$\Delta P$ (psi)	Correction factor
<b>3</b>	<b>1.00</b>
4	0.87
5	0.79
6	0.72
7	0.66
8	0.62

#### Correction factor for circulation rate ( $f_{rec}$ )

Circulation rate	Correction factor
2	0.5
3	0.75
<b>4</b>	<b>1</b>
6	1.5
8	2
10	2.5



## Check valves, type NRVA

### Nominal capacities

### Liquid line without phase change

### SI units

Capacity table for nominal conditions,  $Q_N$  [kW], circulation rate = 4,  $\Delta P = 0.2$  bar

### R 134a

Type	$k_v$ [m <sup>3</sup> /h]	Evaporating temperature $T_e$							
		-50 °C	-40 °C	-30 °C	-20 °C	-10 °C	0 °C	10 °C	20 °C
NRVA 15	5	41.2	39.7	38.2	36.6	34.8	33.0	31.1	32
NRVA 20	6	49	48	46	44	42	40	37.4	39
NRVA 25	19	157	151	145	139	132	126	118	122
NRVA 32	20	165	159	153	146	139	132	125	128
NRVA 40	44	363	350	336	322	307	291	274	283
NRVA 50	44	363	350	336	322	307	291	274	283
NRVA 65	75	618	596	573	549	523	496	467	482

#### Correction factor for $\Delta P$ ( $f_{\Delta P}$ )

$\Delta P$ (bar)	Correction factor
<b>0.2</b>	<b>1.00</b>
0.25	0.89
0.3	0.82
0.4	0.71
0.5	0.63
0.6	0.58

#### Correction factor for circulation rate ( $f_{rec}$ )

Circulation rate	Correction factor
2	0.5
3	0.75
<b>4</b>	<b>1</b>
6	1.5
8	2
10	2.5

### US units

Capacity table for nominal conditions,  $Q_N$  [Tons of Refrigeration], circulation rate = 4,  $\Delta P = 3$  psi

### R 134a

Type	$C_v$ [USgal/min]	Evaporating temperature $T_e$							
		-60 °F*	-40 °F	-20 °F	0 °F	20 °F	40 °F	60 °F	80 °F
NRVA 15	6	11.9	11.4	10.9	10.4	9.9	9.2	8.6	8.8
NRVA 20	7	14.3	13.7	13.1	12.5	11.8	11.1	10.3	11
NRVA 25	22	45	43	42	40	37	35	33	34
NRVA 32	23	48	46	44	42	39	37	34	35
NRVA 40	51	105	101	96	92	87	81	76	78
NRVA 50	51	105	101	96	92	87	81	76	78
NRVA 65	87	179	172	164	156	148	138	129	133

\* 2 °F below min. operating temperature.

#### Correction factor for $\Delta P$ ( $f_{\Delta P}$ )

$\Delta P$ (psi)	Correction factor
<b>3</b>	<b>1.00</b>
4	0.87
5	0.79
6	0.72
7	0.66
8	0.62

#### Correction factor for circulation rate ( $f_{rec}$ )

Circulation rate	Correction factor
2	0.5
3	0.75
<b>4</b>	<b>1</b>
6	1.5
8	2
10	2.5

## Check valves, type NRVA

### Nominal capacities

### Liquid line without phase change

### SI units

Capacity table for nominal conditions,  $Q_N$  [kW], circulation rate = 4,  $\Delta P = 0.2$  bar

#### R 404A

Type	$k_v$ [m <sup>3</sup> /h]	Evaporating temperature $T_e$							
		-50 °C	-40 °C	-30 °C	-20 °C	-10 °C	0 °C	10 °C	20 °C
NRVA 15	5	36	35	33	31	30	28	26	23
NRVA 20	6	43	42	39	38	35	33	31	28
NRVA 25	19	138	132	125	119	112	105	97	89
NRVA 32	20	145	139	131	125	118	111	102	93
NRVA 40	44	319	306	289	276	260	244	225	205
NRVA 50	44	319	306	289	276	260	244	225	205
NRVA 65	75	543	521	492	470	444	415	384	350

#### Correction factor for $\Delta P$ ( $f_{\Delta P}$ )

$\Delta P$ (bar)	Correction factor
<b>0.2</b>	<b>1.00</b>
0.25	0.89
0.3	0.82
0.4	0.71
0.5	0.63
0.6	0.58

#### Correction factor for circulation rate ( $f_{rec}$ )

Circulation rate	Correction factor
2	0.5
3	0.75
<b>4</b>	<b>1</b>
6	1.5
8	2
10	2.5

### US units

Capacity table for nominal conditions,  $Q_N$  [Tons of Refrigeration], circulation rate = 4,  $\Delta P = 3$  psi

#### R 404A

Type	$C_v$ [USgal/min]	Evaporating temperature $T_e$							
		-60 °F*	-40 °F	-20 °F	0 °F	20 °F	40 °F	60 °F	80 °F
NRVA 15	6	10.5	10.0	9.5	9.0	8.4	7.8	7.0	6.2
NRVA 20	7	13	12	11	11	10	9	8	7
NRVA 25	22	40	38	36	34	32	30	27	24
NRVA 32	23	42	40	38	36	34	31	28	25
NRVA 40	51	92	88	83	79	74	68	62	55
NRVA 50	51	92	88	83	79	74	68	62	55
NRVA 65	87	158	151	142	134	126	117	105	93

\* 2 °F below min. operating temperature.

#### Correction factor for $\Delta P$ ( $f_{\Delta P}$ )

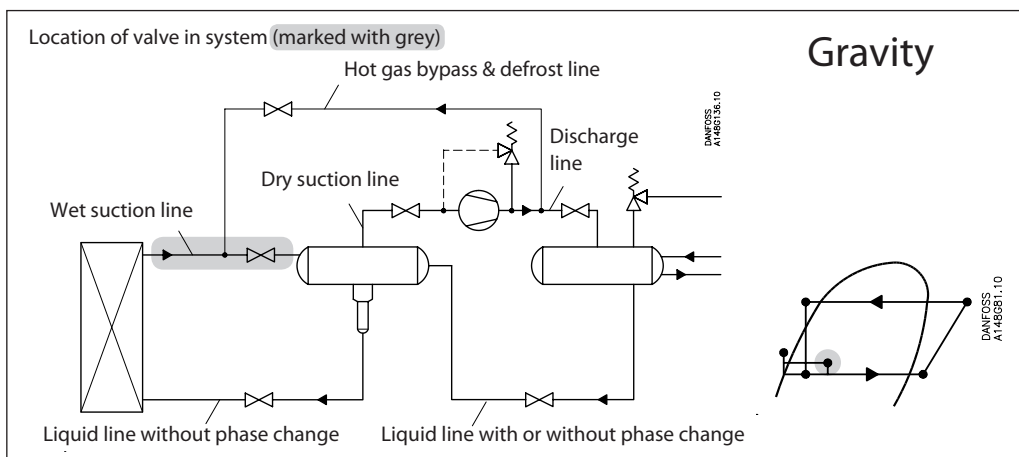
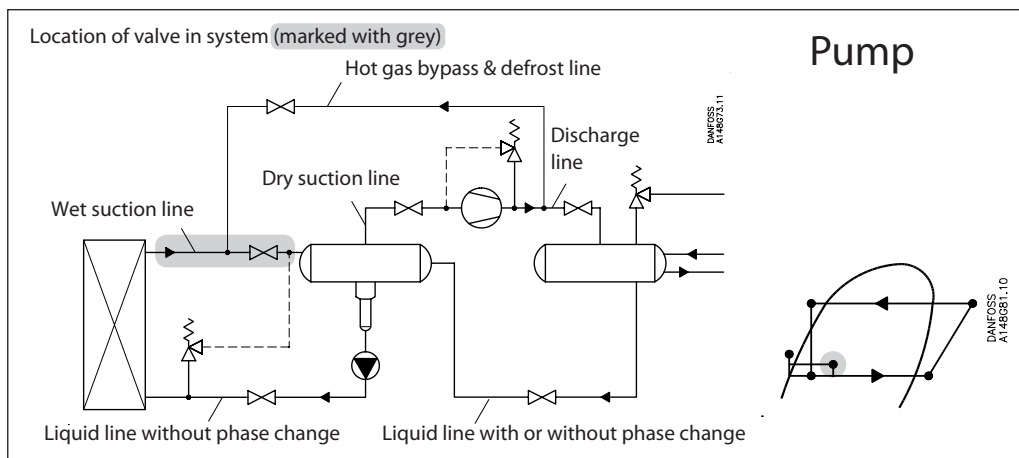
$\Delta P$ (psi)	Correction factor
<b>3</b>	<b>1.00</b>
4	0.87
5	0.79
6	0.72
7	0.66
8	0.62

#### Correction factor for circulation rate ( $f_{rec}$ )

Circulation rate	Correction factor
2	0.5
3	0.75
<b>4</b>	<b>1</b>
6	1.5
8	2
10	2.5

Nominal capacities

Wet suction line



Nominal capacities

Wet suction line

SI units

Calculation example (R 717 capacities):

Running conditions in a plant are as follows:

$T_e = -20\text{ °C}$   
 $Q_0 = 100\text{ kW}$   
 Circulation rate = 3  
 Max.  $\Delta P = 0.3\text{ bar}$

The capacity table is based on nominal conditions (pressure drop  $\Delta P = 0.2\text{ bar}$ , circulation rate = 4).

The actual capacity must therefore be corrected to a nominal condition by multiplication with correction factors.

Correction factor for  $\Delta P\ 0.3\text{ bar}$   $f_{\Delta P} = 0.82$   
 Correction factor for circulation rate  $f_{rec} = 0.9$ .

$$Q_n = Q_0 \times f_{\Delta P} \times f_{rec} = 100 \times 0.82 \times 0.9 = 73,8\text{ kW.}$$

From the capacity table a NRVA 40 with  $Q_n = 157\text{ kW}$  is the correct selection for the application.

Choosing NRVA 32 would give a slightly higher pressure drop than 0.3. Accepting this requires a plant evaluation.

US units

Calculation example (R 717 capacities):

Running conditions in a plant are as follows:

$T_e = -20\text{ °F}$   
 $Q_0 = 10\text{ TR}$   
 Circulation rate = 3  
 Max.  $\Delta P = 5\text{ psi}$

The capacity table is based on nominal conditions (pressure drop  $\Delta P = 3\text{ psi}$ , circulation rate = 4).

The actual capacity must therefore be corrected to a nominal condition by multiplication with correction factors.

Correction factor for  $\Delta P\ 5\text{ psi}$   $f_{\Delta P} = 0.79$   
 Correction factor for circulation rate  $f_{rec} = 0.9$ .

$$Q_n = Q_0 \times f_{\Delta P} \times f_{circ} = 10 \times 0.79 \times 0.9 = 7.1\text{ TR}$$

From the capacity table a NRVA 25 with  $Q_n = 16.5\text{ TR}$  is the correct selection for the application.

## Check valves, type NRVA

### Nominal capacities

### Wet suction line

## SI units

Capacity table for nominal conditions,  $Q_N$  [kW], circulation rate = 4,  $\Delta P = 0.2$  bar

### R 717

Type	$k_v$ [m <sup>3</sup> /h]	Evaporating temperature $T_e$							
		-50 °C	-40 °C	-30 °C	-20 °C	-10 °C	0 °C	10 °C	20 °C
NRVA 15	5	9.1	11.8	14.7	17.9	21.3	24.9	28.7	32.6
NRVA 20	6	11.0	14.2	17.6	21.4	25.5	29.9	34.5	39.2
NRVA 25	19	34.7	45.0	55.9	67.9	80.9	94.7	109.1	124.0
NRVA 32	20	36.6	47.3	58.8	71.5	85.1	99.7	115	131
NRVA 40	44	80.4	104.1	129.4	157	187	219	253	287
NRVA 50	44	80.4	104	129	157	187	219	253	287
NRVA 65	75	137	178	221	268	319	374	431	490

#### Correction factor for $\Delta P$ ( $f_{\Delta P}$ )

$\Delta P$ (bar)	Correction factor
<b>0.2</b>	<b>1.00</b>
0.25	0.89
0.3	0.82
0.4	0.71
0.5	0.63
0.6	0.58

#### Correction factor for circulation rate ( $f_{rec}$ )

Circulation rate	Correction factor
2	0.77
3	0.90
<b>4</b>	<b>1</b>
6	1.13
8	1.20
10	1.25

## US units

Capacity table for nominal conditions,  $Q_N$  [Tons of Refrigeration], circulation rate = 4,  $\Delta P = 3$  psi

### R 717

Type	$C_v$ [USgal/min]	Evaporating temperature $T_e$							
		-60 °F*	-40 °F	-20 °F	0 °F	20 °F	40 °F	60 °F	80 °F
NRVA 15	6	2.5	3.4	4.3	5.4	6.5	7.7	8.9	10.1
NRVA 20	7	3.1	4.1	5.2	6.5	7.8	9.2	10.7	12.1
NRVA 25	22	9.7	13.0	16.5	20.5	24.7	29.2	33.8	38.5
NRVA 32	23	10.2	13.7	17.3	21.6	26.0	30.8	35.5	40.5
NRVA 40	51	22.4	30.1	38.1	47.5	57.2	67.7	78.2	89.1
NRVA 50	51	22.4	30.1	38.1	47.5	57.2	67.7	78.2	89.1
NRVA 65	87	38.2	51.3	65.0	80.9	97.6	115	133	152

\* 2 °F below min. operating temperature.

#### Correction factor for $\Delta P$ ( $f_{\Delta P}$ )

$\Delta P$ (psi)	Correction factor
<b>3</b>	<b>1.00</b>
4	0.87
5	0.79
6	0.72
7	0.66
8	0.62

#### Correction factor for circulation rate ( $f_{rec}$ )

Circulation rate	Correction factor
2	0.77
3	0.90
<b>4</b>	<b>1</b>
6	1.13
8	1.20
10	1.25

## Check valves, type NRVA

### Nominal capacities

### Wet suction line

### SI units

Capacity table for nominal conditions,  $Q_N$  [kW], circulation rate = 4,  $\Delta P = 0.2$  bar

### R 22

Type	$k_v$ [m <sup>3</sup> /h]	Evaporating temperature $T_e$							
		-50 °C	-40 °C	-30 °C	-20 °C	-10 °C	0 °C	10 °C	20 °C
NRVA 15	5	4.5	5.5	6.5	7.7	8.9	10.0	11.2	12.4
NRVA 20	6	5.3	6.6	7.9	9.2	10.6	12.1	13.5	14.9
NRVA 25	19	16.9	21	25	29	34	38	43	47
NRVA 32	20	17.8	22	26	31	35	40	45	50
NRVA 40	44	39	48	58	68	78	88	99	109
NRVA 50	44	39	48	58	68	78	88	99	109
NRVA 65	75	67	82	98	115	133	151	168	186

#### Correction factor for $\Delta P$ ( $f_{\Delta P}$ )

$\Delta P$ (bar)	Correction factor
<b>0.2</b>	<b>1.00</b>
0.25	0.89
0.3	0.82
0.4	0.71
0.5	0.63
0.6	0.58

#### Correction factor for circulation rate ( $f_{rec}$ )

Circulation rate	Correction factor
2	0.77
3	0.90
<b>4</b>	<b>1</b>
6	1.13
8	1.20
10	1.25

### US units

Capacity table for nominal conditions,  $Q_N$  [Tons of Refrigeration], circulation rate = 4,  $\Delta P = 3$  psi

### R 22

Type	$C_v$ [USgal/min]	Evaporating temperature $T_e$							
		-60 °F*	-40 °F	-20 °F	0 °F	20 °F	40 °F	60 °F	80 °F
NRVA 15	6	1.3	1.6	1.9	2.3	2.7	3.0	3.4	3.8
NRVA 20	7	1.5	1.9	2.3	2.7	3.2	3.6	4.1	4.6
NRVA 25	22	4.8	6.0	7.3	8.7	10.1	11.5	13.1	14.4
NRVA 32	23	5.0	6.3	7.7	9.2	10.6	12.2	13.8	15.2
NRVA 40	51	11.1	13.9	16.9	20	23	27	30	33
NRVA 50	51	11.1	13.9	16.9	20	23	27	30	33
NRVA 65	87	18.9	24	29	34	40	46	52	57

\* 2 °F below min. operating temperature.

#### Correction factor for $\Delta P$ ( $f_{\Delta P}$ )

$\Delta P$ (psi)	Correction factor
<b>3</b>	<b>1.00</b>
4	0.87
5	0.79
6	0.72
7	0.66
8	0.62

#### Correction factor for circulation rate ( $f_{rec}$ )

Circulation rate	Correction factor
2	0.77
3	0.90
<b>4</b>	<b>1</b>
6	1.13
8	1.20
10	1.25

## Check valves, type NRVA

### Nominal capacities

### Wet suction line

## SI units

Capacity table for nominal conditions,  $Q_N$  [kW], circulation rate = 4,  $\Delta P = 0.2$  bar

### R 134a

Type	$k_v$ [m <sup>3</sup> /h]	Evaporating temperature $T_e$							
		-50 °C	-40 °C	-30 °C	-20 °C	-10 °C	0 °C	10 °C	20 °C
NRVA 15	5	3.3	4.6	5.7	6.7	7.7	8.8	9.8	12.4
NRVA 20	6	4.0	5.5	6.8	8.0	9.3	10.5	11.8	14.9
NRVA 25	19	12.6	17.3	22	25	29	33	37	47
NRVA 32	20	13.3	18.2	23	27	31	35	39	50
NRVA 40	44	29	40.1	50	59	68	77	87	109
NRVA 50	44	29	40.1	50	59	68	77	87	109
NRVA 65	75	50	68.4	85	100	116	132	148	186

#### Correction factor for $\Delta P$ ( $f_{\Delta P}$ )

$\Delta P$ (bar)	Correction factor
<b>0.2</b>	<b>1.00</b>
0.25	0.89
0.3	0.82
0.4	0.71
0.5	0.63
0.6	0.58

#### Correction factor for circulation rate ( $f_{rec}$ )

Circulation rate	Correction factor
2	0.77
3	0.90
<b>4</b>	<b>1</b>
6	1.13
8	1.20
10	1.25

## US units

Capacity table for nominal conditions,  $Q_N$  [Tons of Refrigeration], circulation rate = 4,  $\Delta P = 3$  psi

### R 134a

Type	$C_v$ [USgal/min]	Evaporating temperature $T_e$							
		-60 °F*	-40 °F	-20 °F	0 °F	20 °F	40 °F	60 °F	80 °F
NRVA 15	6	1.0	1.3	1.7	2.0	2.4	2.7	3.1	3.8
NRVA 20	7	1.2	1.6	2.0	2.4	2.8	3.3	3.7	4.6
NRVA 25	22	3.7	5.1	6.4	7.7	9.0	10.3	11.6	14.4
NRVA 32	23	3.8	5.4	6.8	8.1	9.4	10.9	12.2	15.2
NRVA 40	51	8.5	11.8	14.9	17.8	21	24	27	33
NRVA 50	51	8.5	11.8	14.9	17.8	21	24	27	33
NRVA 65	87	14.4	20	25	30	35	41	46	57

\* 2 °F below min. operating temperature.

#### Correction factor for $\Delta P$ ( $f_{\Delta P}$ )

$\Delta P$ (psi)	Correction factor
<b>3</b>	<b>1.00</b>
4	0.87
5	0.79
6	0.72
7	0.66
8	0.62

#### Correction factor for circulation rate ( $f_{rec}$ )

Circulation rate	Correction factor
2	0.77
3	0.90
<b>4</b>	<b>1</b>
6	1.13
8	1.20
10	1.25

## Check valves, type NRVA

### Nominal capacities

### Wet suction line

### SI units

Capacity table for nominal conditions,  $Q_N$  [kW], circulation rate = 4,  $\Delta P = 0.2$  bar

### R 404A

Type	$k_v$ [m <sup>3</sup> /h]	Evaporating temperature $T_e$							
		-50 °C	-40 °C	-30 °C	-20 °C	-10 °C	0 °C	10 °C	20 °C
NRVA 15	5	4.6	5.5	6.5	7.6	8.7	9.8	10.8	11.7
NRVA 20	6	5.5	6.7	7.8	9.1	10.4	11.7	12.9	14.0
NRVA 25	19	17.4	21.1	24.7	28.9	33.0	37.1	40.9	44.4
NRVA 32	20	18.3	22.2	26.1	30.4	34.7	39.0	43.1	46.7
NRVA 40	44	40.3	48.8	57.3	66.9	76.4	85.8	94.8	102.8
NRVA 50	44	40.3	48.8	57.3	66.9	76.4	85.8	94.8	102.8
NRVA 65	75	68.7	83.2	97.7	114.0	130.3	146.3	161.6	175.3

#### Correction factor for $\Delta P$ ( $f_{\Delta P}$ )

$\Delta P$ (bar)	Correction factor
<b>0.2</b>	<b>1.00</b>
0.25	0.89
0.3	0.82
0.4	0.71
0.5	0.63
0.6	0.58

#### Correction factor for circulation rate ( $f_{rec}$ )

Circulation rate	Correction factor
2	0.77
3	0.90
<b>4</b>	<b>1</b>
6	1.13
8	1.20
10	1.25

### US units

Capacity table for nominal conditions,  $Q_N$  [Tons of Refrigeration], circulation rate = 4,  $\Delta P = 3$  psi

### R 404A

Type	$C_v$ [USgal/min]	Evaporating temperature $T_e$							
		-60 °F*	-40 °F	-20 °F	0 °F	20 °F	40 °F	60 °F	80 °F
NRVA 15	6	1.3	1.6	1.9	2.3	2.6	2.9	3.3	3.5
NRVA 20	7	1.6	1.9	2.3	2.7	3.1	3.5	3.9	4.2
NRVA 25	22	4.9	6.1	7.3	8.6	9.9	11.2	12.4	13.4
NRVA 32	23	5.2	6.4	7.7	9.0	10.4	11.8	13.1	14.1
NRVA 40	51	11.4	14.1	16.9	19.9	22.9	25.9	28.8	31.1
NRVA 50	51	11.4	14.1	16.9	19.9	22.9	25.9	28.8	31.1
NRVA 65	87	19.4	24.1	28.8	33.9	39.1	44.1	49.1	52.9

\* 2 °F below min. operating temperature.

#### Correction factor for $\Delta P$ ( $f_{\Delta P}$ )

$\Delta P$ (psi)	Correction factor
<b>3</b>	<b>1.00</b>
4	0.87
5	0.79
6	0.72
7	0.66
8	0.62

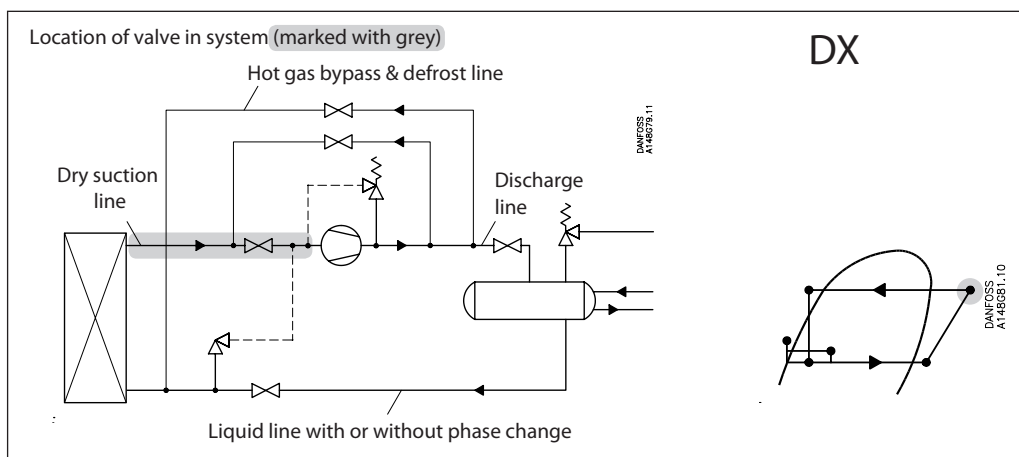
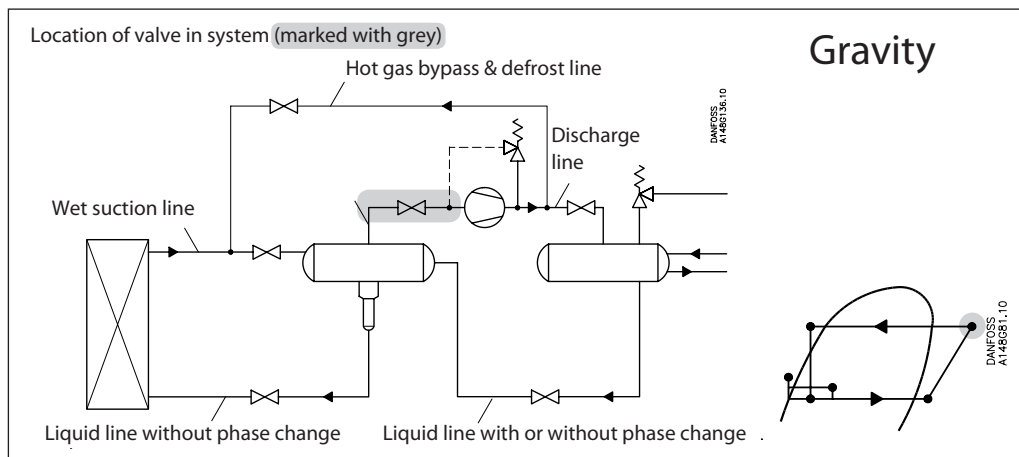
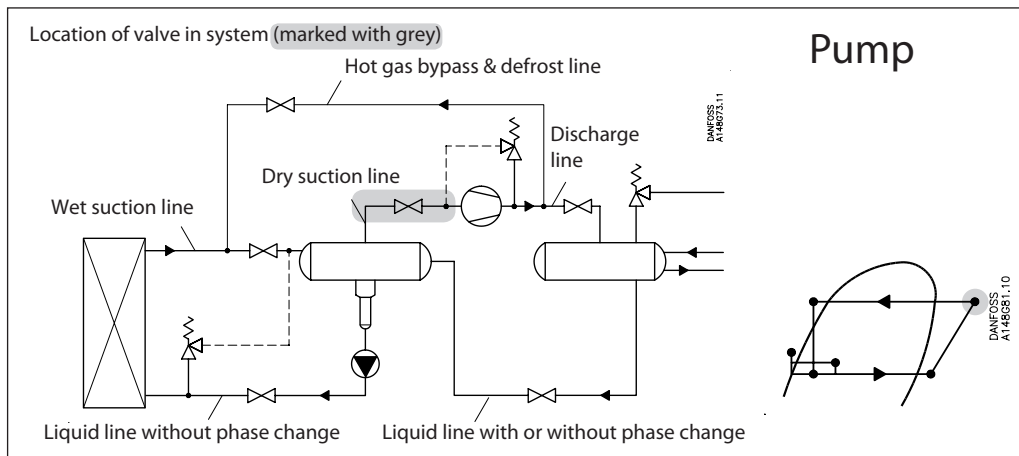
#### Correction factor for circulation rate ( $f_{rec}$ )

Circulation rate	Correction factor
2	0.77
3	0.90
<b>4</b>	<b>1</b>
6	1.13
8	1.20
10	1.25



Nominal capacities

Dry suction line



Nominal capacities

Dry suction line

SI units

Calculation example (R 134a capacities):

Running conditions in a plant are as follows:

$$\begin{aligned} T_e &= -20\text{ }^\circ\text{C} \\ Q_0 &= 90\text{ kW} \\ T_{liq} &= 10\text{ }^\circ\text{C} \\ T_s &= 6\text{ }^\circ\text{C} \\ \text{Max. } \Delta P &= 0.3\text{ bar} \end{aligned}$$

The capacity table is based on nominal conditions (pressure drop  $\Delta P = 0.2\text{ bar}$ ,  $T_{liq} = 30\text{ }^\circ\text{C}$ ),  $T_s = 10\text{ }^\circ\text{C}$

The actual capacity must therefore be corrected to a nominal condition by multiplication with correction factors.

Correction factor for  $\Delta P 0.3\text{ bar}$   $f_{\Delta P} = 0.82$

Correction factor for liquid temperature  $f_{T_{liq}} = 0.82$

Correction factor for superheat ( $T_s$ ) = 1,0

$$\begin{aligned} Q_n &= Q_0 \times f_{\Delta P} \times f_{T_{liq}} \times f_{T_s} \\ &= 90 \times 0.82 \times 0.82 \times 1.0 = 60.5\text{ kW} \end{aligned}$$

From the capacity table a NRVA 40 or NRVA 50 with  $Q_n = 65\text{ kW}$  is the correct selection depending on connections for the application.

US units

Calculation example (R 134a capacities):

Running conditions in a plant are as follows:

$$\begin{aligned} T_e &= 0\text{ }^\circ\text{F} \\ Q_0 &= 23\text{ TR} \\ T_{liq} &= 50\text{ }^\circ\text{F} \\ T_s &= 10\text{ }^\circ\text{F} \\ \text{Max. } \Delta P &= 5\text{ psi} \end{aligned}$$

The capacity table is based on nominal conditions (pressure drop  $\Delta P = 3\text{ psi}$ ,  $T_{liq} = 90\text{ }^\circ\text{F}$ ),  $T_s = 14\text{ }^\circ\text{F}$

The actual capacity must therefore be corrected to a nominal condition by multiplication with correction factors.

Correction factor for  $\Delta P 5\text{ psi}$   $f_{\Delta P} = 0.79$

Correction factor for liquid temperature  $f_{T_{liq}} = 0.81$

Correction factor for superheat ( $T_s$ ) = 1,0

$$\begin{aligned} Q_n &= Q_0 \times f_{\Delta P} \times f_{T_{liq}} \times f_{T_s} = \\ &23 \times 0.79 \times 0.81 \times 1.0 = 14.7\text{ TR} \end{aligned}$$

From the capacity table a NRVA 40 or NRVA 50 with  $Q_n = 19.3\text{ TR}$  is the correct selection depending on connections for the application.

## Check valves, type NRVA

### Nominal capacities

### Dry suction line

## R 717

### SI units

Capacity table for nominal conditions,  $Q_N$  [kW],  
 $T_{liq} = 30\text{ °C}$ ,  
 $\Delta P = 0.2\text{ bar}$

Type	$k_v$ [m <sup>3</sup> /h]	Evaporating temperature $T_e$							
		-50 °C	-40 °C	-30 °C	-20 °C	-10 °C	0 °C	10 °C	20 °C
NRVA 15	5	12.9	17.0	21.8	27.5	33.7	41.0	49.0	57.9
NRVA 20	6	15.5	20.4	26.2	32.9	40.5	49.2	58.9	69.5
NRVA 25	19	49.0	64.7	82.8	104.3	128.2	155.7	186	220
NRVA 32	20	51.6	68.1	87.2	109.8	135	164	196	232
NRVA 40	44	113.5	149.7	192	242	297	361	432	510
NRVA 50	44	113	150	192	242	297	361	432	510
NRVA 65	75	193	255	327	412	506	615	736	869

#### Correction factor for $\Delta P$ ( $f_{\Delta P}$ )

$\Delta P$ (bar)	Correction factor
<b>0.2</b>	<b>1.00</b>
0.25	0.89
0.3	0.82
0.4	0.71
0.5	0.63
0.6	0.58

#### Correction factor for superheat ( $T_s$ )

$T_s$	Correction factor
6 °C	1.00
8 °C	1.00
10 °C	1.00
12 °C	1.00

#### Correction factor for liquid temperature ( $T_{liq}$ )

Liquid temperature	Correction factor
-20 °C	0.82
-10 °C	0.86
0 °C	0.88
10 °C	0.92
20 °C	0.96
<b>30 °C</b>	<b>1.00</b>
40 °C	1.04
50 °C	1.09

## R 717

### US units

Capacity table for nominal conditions,  $Q_N$  [Tons of Refrigeration],  
 $T_{liq} = 90\text{ °F}$ ,  
 $\Delta P = 3\text{ psi}$

Type	$C_v$ [USgal/min]	Evaporating temperature $T_e$							
		-60 °F*	-40 °F	-20 °F	0 °F	20 °F	40 °F	60 °F	80 °F
NRVA 15	6	3.6	4.9	6.4	8.2	10.4	12.8	15.4	18.3
NRVA 20	7	4.3	5.9	7.7	9.8	12.4	15.4	18.5	22.0
NRVA 25	22	13.6	18.7	24.4	31.2	39.4	48.6	58.5	69.7
NRVA 32	23	14.3	19.7	25.7	32.8	41.4	51.2	61.5	73.3
NRVA 40	51	31.5	43.2	56.5	72.2	91.2	112.6	135.4	161
NRVA 50	51	31.5	43.2	56.5	72.2	91.2	113	135	161
NRVA 65	87	53.6	73.7	96.3	123	155	192	231	275

\* 2 °F below min. operating temperature.

#### Correction factor for $\Delta P$ ( $f_{\Delta P}$ )

$\Delta P$ (psi)	Correction factor
<b>3</b>	<b>1.00</b>
4	0.87
5	0.79
6	0.72
7	0.66
8	0.62

#### Correction factor for superheat ( $T_s$ )

$T_s$	Correction factor
10 °F	1.00
14 °F	1.00
18 °F	1.00
20 °F	1.00

#### Correction factor for liquid temperature ( $T_{liq}$ )

Liquid temperature	Correction factor
-10 °F	0.82
10 °F	0.85
30 °F	0.88
50 °F	0.92
70 °F	0.96
<b>90 °F</b>	<b>1.00</b>
110 °F	1.04
130 °F	1.09

## Check valves, type NRVA

### Nominal capacities

### Dry suction line

### SI units

Capacity table for nominal conditions,  $Q_N$  [kW],  
 $T_{liq} = 30\text{ °C}$ ,  
 $\Delta P = 0.2\text{ bar}$

### R 22

Type	$k_v$ [m <sup>3</sup> /h]	Evaporating temperature $T_e$							
		-50 °C	-40 °C	-30 °C	-20 °C	-10 °C	0 °C	10 °C	20 °C
NRVA 15	5	5.1	6.6	8.3	10.4	12.7	15.3	18.2	21.4
NRVA 20	6	6.1	7.9	10.0	12.5	15.2	18.3	22	26
NRVA 25	19	19.3	25	32	40	48	58	69	81
NRVA 32	20	20	26	33	42	51	61	73	85
NRVA 40	44	45	58	73	92	112	134	160	188
NRVA 50	44	45	58	73	92	112	134	160	188
NRVA 65	75	76	99	125	156	190	229	272	320

#### Correction factor for $\Delta P$ ( $f_{\Delta P}$ )

$\Delta P$ (bar)	Correction factor
<b>0.2</b>	<b>1.00</b>
0.25	0.89
0.3	0.82
0.4	0.71
0.5	0.63
0.6	0.58

#### Correction factor for superheat ( $T_s$ )

$T_s$	Correction factor
6 °C	1.00
8 °C	1.00
10 °C	1.00
12 °C	1.00

#### Correction factor for liquid temperature ( $T_{liq}$ )

Liquid temperature	Correction factor
-20 °C	0.71
-10 °C	0.75
0 °C	0.80
10 °C	0.86
20 °C	0.92
<b>30 °C</b>	<b>1.00</b>
40 °C	1.09
50 °C	1.22

### US units

Capacity table for nominal conditions,  $Q_N$  [Tons of Refrigeration],  
 $T_{liq} = 90\text{ °F}$ ,  
 $\Delta P = 3\text{ psi}$

### R 22

Type	$C_v$ [USgal/min]	Evaporating temperature $T_e$							
		-60 °F*	-40 °F	-20 °F	0 °F	20 °F	40 °F	60 °F	80 °F
NRVA 15	6	1.4	1.9	2.4	3.1	3.8	4.7	5.7	6.8
NRVA 20	7	1.7	2.2	2.9	3.7	4.6	5.6	6.8	8.1
NRVA 25	22	5.3	7.1	9.2	11.7	14.5	17.7	22	26
NRVA 32	23	5.6	7.5	9.7	12.3	15.3	18.6	23	27
NRVA 40	51	12.3	16.4	21	27	34	41	50	60
NRVA 50	51	12.3	16.4	21	27	34	41	50	60
NRVA 65	87	21	28	36	46	57	70	86	102

\* 2 °F below min. operating temperature.

#### Correction factor for $\Delta P$ ( $f_{\Delta P}$ )

$\Delta P$ (psi)	Correction factor
<b>3</b>	<b>1.00</b>
4	0.87
5	0.79
6	0.72
7	0.66
8	0.62

#### Correction factor for superheat ( $T_s$ )

$T_s$	Correction factor
10 °F	1.00
14 °F	1.00
18 °F	1.00
20 °F	1.00

#### Correction factor for liquid temperature ( $T_{liq}$ )

Liquid temperature	Correction factor
-10 °F	0.73
10 °F	0.77
30 °F	0.82
50 °F	0.87
70 °F	0.93
<b>90 °F</b>	<b>1.00</b>
110 °F	1.09
130 °F	1.20

## Check valves, type NRVA

### Nominal capacities

### Dry suction line

### SI units

Capacity table for nominal conditions,  $Q_N$  [kW],  
 $T_{liq} = 30\text{ °C}$ ,  
 $\Delta P = 0.2\text{ bar}$

### R 134a

Type	$k_v$ [m <sup>3</sup> /h]	Evaporating temperature $T_e$							
		-50 °C	-40 °C	-30 °C	-20 °C	-10 °C	0 °C	10 °C	20 °C
NRVA 15	5	4.3	5.7	7.4	9.4	11.7	14.3	17.3	21.4
NRVA 20	6	5.2	6.9	8.9	11.2	14.0	17.2	21	26
NRVA 25	19	16.4	22	28	36	44	54	66	81
NRVA 32	20	17.3	23	30	37	47	57	69	85
NRVA 40	44	38	50	65	82	103	126	153	188
NRVA 50	44	38	50	65	82	103	126	153	188
NRVA 65	75	65	86	111	140	175	215	260	320

#### Correction factor for $\Delta P$ ( $f_{\Delta P}$ )

$\Delta P$ (bar)	Correction factor
<b>0.2</b>	<b>1.00</b>
0.25	0.89
0.3	0.82
0.4	0.71
0.5	0.63
0.6	0.58

#### Correction factor for superheat ( $T_s$ )

$T_s$	Correction factor
6 °C	1.00
8 °C	1.00
10 °C	1.00
12 °C	1.00

#### Correction factor for liquid temperature ( $T_{liq}$ )

Liquid temperature	Correction factor
-20 °C	0.66
-10 °C	0.70
0 °C	0.76
10 °C	0.82
20 °C	0.90
<b>30 °C</b>	<b>1.00</b>
40 °C	1.13
50 °C	1.29

### US units

Capacity table for nominal conditions,  $Q_N$  [Tons of Refrigeration],  
 $T_{liq} = 90\text{ °F}$ ,  
 $\Delta P = 3\text{ psi}$

### R 134a

Type	$C_v$ [USgal/min]	Evaporating temperature $T_e$							
		-60 °F*	-40 °F	-20 °F	0 °F	20 °F	40 °F	60 °F	80 °F
NRVA 15	6	1.2	1.7	2.2	2.8	3.6	4.6	5.6	6.8
NRVA 20	7	1.5	2.0	2.6	3.4	4.3	5.5	6.7	8.1
NRVA 25	22	4.6	6.3	8.3	10.8	13.7	17.3	21	26
NRVA 32	23	4.9	6.6	8.8	11.4	14.4	18.3	22	27
NRVA 40	51	10.7	14.6	19.3	25	32	40	49	60
NRVA 50	51	10.7	14.6	19.3	25	32	40	49	60
NRVA 65	87	18.3	25	33	43	54	68	84	102

\* 2 °F below min. operating temperature.

#### Correction factor for $\Delta P$ ( $f_{\Delta P}$ )

$\Delta P$ (psi)	Correction factor
<b>3</b>	<b>1.00</b>
4	0.87
5	0.79
6	0.72
7	0.66
8	0.62

#### Correction factor for superheat ( $T_s$ )

$T_s$	Correction factor
10 °F	1.00
14 °F	1.00
18 °F	1.00
20 °F	1.00

#### Correction factor for liquid temperature ( $T_{liq}$ )

Liquid temperature	Correction factor
-10 °F	0.64
10 °F	0.68
30 °F	0.74
50 °F	0.81
70 °F	0.89
<b>90 °F</b>	<b>1.00</b>
110 °F	1.15
130 °F	1.35

## Check valves, type NRVA

### Nominal capacities

### Dry suction line

### SI units

Capacity table for nominal conditions,  $Q_N$  [kW],

$T_{liq} = 30\text{ °C}$ ,  
 $\Delta P = 0.2\text{ bar}$

### R 404A

Type	$k_v$ [m <sup>3</sup> /h]	Evaporating temperature $T_e$							
		-50 °C	-40 °C	-30 °C	-20 °C	-10 °C	0 °C	10 °C	20 °C
NRVA 15	5	3.8	5.1	6.7	8.6	10.7	13.2	16.1	19.4
NRVA 20	6	4.6	6.1	8.0	10.3	12.8	15.8	19.3	23.3
NRVA 25	19	14.5	19.4	25.3	32.5	40.6	50.2	61.2	73.7
NRVA 32	20	15.3	20.4	26.7	34.3	42.8	52.8	64.4	77.6
NRVA 40	44	33.6	44.9	58.7	75.4	94	116	142	171
NRVA 50	44	33.6	44.9	59	75	94	116	142	171
NRVA 65	75	57.3	77	100	128	160	198	241	291

#### Correction factor for $\Delta P$ ( $f_{\Delta P}$ )

$\Delta P$ (bar)	Correction factor
<b>0.2</b>	<b>1.00</b>
0.25	0.89
0.3	0.82
0.4	0.71
0.5	0.63
0.6	0.58

#### Correction factor for superheat ( $T_s$ )

$T_s$	Correction factor
6 °C	1.00
8 °C	1.00
10 °C	1.00
12 °C	1.00

#### Correction factor for liquid temperature ( $T_{liq}$ )

Liquid temperature	Correction factor
-20 °C	0.55
-10 °C	0.60
0 °C	0.66
10 °C	0.74
20 °C	0.85
<b>30 °C</b>	<b>1.00</b>
40 °C	1.23
50 °C	1.68

### US units

Capacity table for nominal conditions,  $Q_N$  [Tons of Refrigeration],

$T_{liq} = 90\text{ °F}$ ,  
 $\Delta P = 3\text{ psi}$

### R 404A

Type	$C_v$ [USgal/min]	Evaporating temperature $T_e$							
		-60 °F*	-40 °F	-20 °F	0 °F	20 °F	40 °F	60 °F	80 °F
NRVA 15	6	1.0	1.4	1.9	2.5	3.2	4.0	5.1	6.2
NRVA 20	7	1.2	1.7	2.3	3.0	3.8	4.8	6.1	7.4
NRVA 25	22	3.9	5.4	7.3	9.5	12.2	15.3	19.3	23.5
NRVA 32	23	4.1	5.7	7.6	10.0	12.8	16.1	20.3	24.7
NRVA 40	51	9.1	12.5	16.8	22.0	28.2	35.4	44.6	54.4
NRVA 50	51	9.1	12.5	16.8	22.0	28.2	35.4	44.6	54.4
NRVA 65	87	15.5	21.4	28.7	37.5	48.0	60	76	93

\* 2 °F below min. operating temperature.

#### Correction factor for $\Delta P$ ( $f_{\Delta P}$ )

$\Delta P$ (psi)	Correction factor
<b>3</b>	<b>1.00</b>
4	0.87
5	0.79
6	0.72
7	0.66
8	0.62

#### Correction factor for superheat ( $T_s$ )

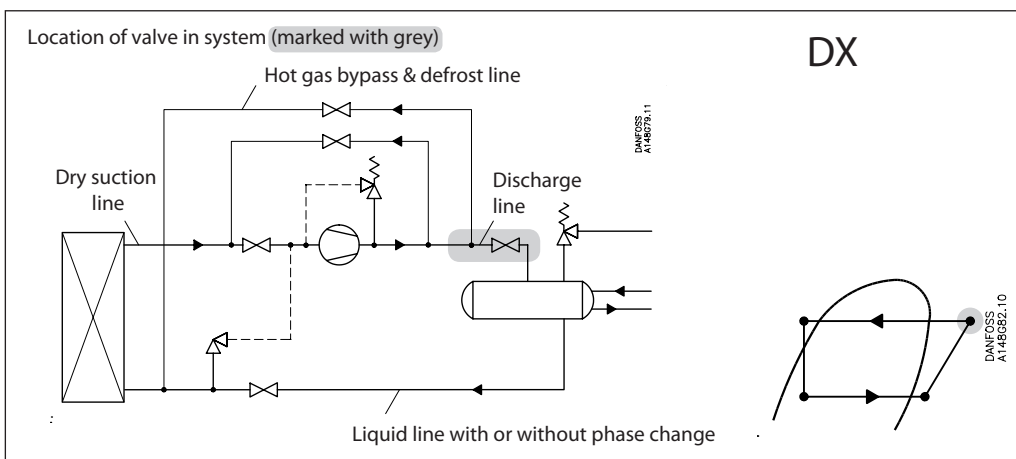
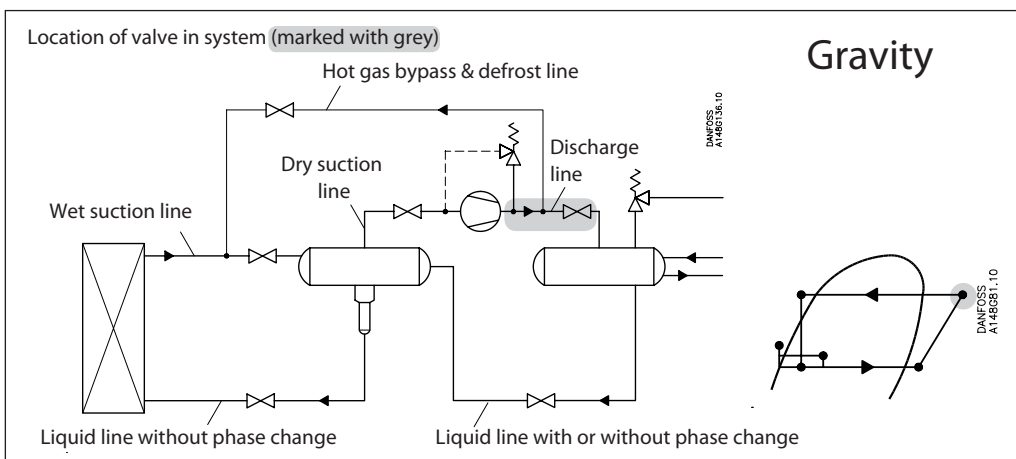
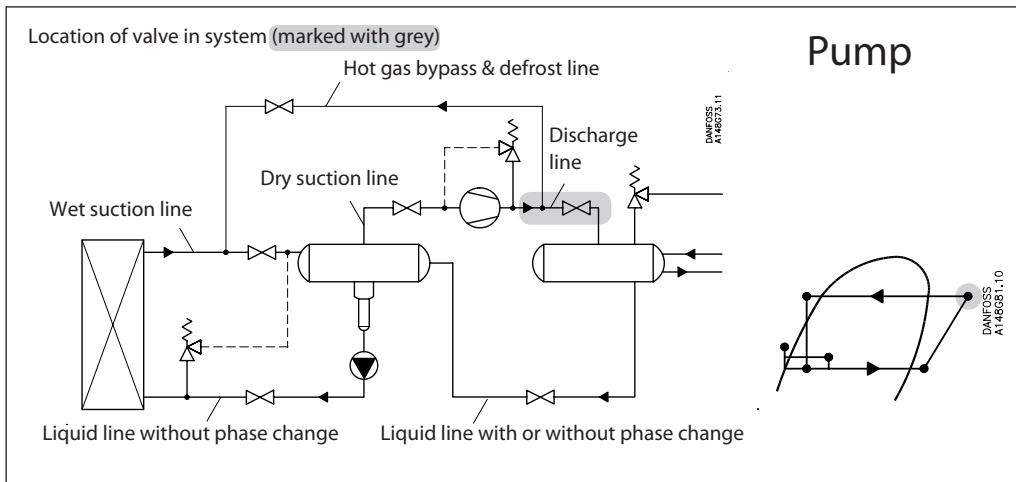
$T_s$	Correction factor
10 °F	1.00
14 °F	1.00
18 °F	1.00
20 °F	1.00

#### Correction factor for liquid temperature ( $T_{liq}$ )

Liquid temperature	Correction factor
-10 °F	0.52
10 °F	0.57
30 °F	0.63
50 °F	0.72
70 °F	0.83
<b>90 °F</b>	<b>1.00</b>
110 °F	1.29
130 °F	1.92

Nominal capacities

Discharge line



Nominal capacities

Discharge line

SI units

Calculation example (R 717 capacities):

Running conditions in a plant are as follows:

$$\begin{aligned} T_e &= -20\text{ }^\circ\text{C} \\ Q_o &= 90\text{ kW} \\ T_{liq} &= 10\text{ }^\circ\text{C} \\ \text{Max. } \Delta P &= 0.4\text{ bar} \\ T_{disch} &= 60\text{ }^\circ\text{C} \end{aligned}$$

The capacity table is based on nominal conditions ( $\Delta P = 0.2\text{ bar}$ ,  $T_{liq} = 30\text{ }^\circ\text{C}$ ,  $P_{disch} = 12\text{ bar}$ ,  $T_{disch} = 80\text{ }^\circ\text{C}$ ).

The actual capacity must therefore be corrected to a nominal condition by multiplication with correction factors.

Correction factor for  $\Delta P$  0.4 bar  $f_{\Delta P} = 0.72$ .

Correction factor for liquid temperature  $f_{T_{liq}} = 0.92$ .

Correction factor for  $T_{disch}$  60  $^\circ\text{C}$ ,  $f_{disch} = 0.97$ .

Correction factor for  $P_{disch}$  12 bar,  $f_{pdisch} = 1.0$ .

$$\begin{aligned} Q_n &= Q_o \times f_{\Delta P} \times f_{T_{liq}} \times f_{T_{disch}} \times f_{pdisch} \\ &= 90 \times 0.72 \times 0.92 \times 0.97 \times 1.0 = 58\text{ kW} \end{aligned}$$

From the capacity table a NRVA 20 with  $Q_n = 67.5\text{ kW}$  is the correct selection for the application.

US units

Calculation example (R 717 capacities):

Running conditions in a plant are as follows:

$$\begin{aligned} T_e &= 0\text{ }^\circ\text{F} \\ Q_o &= 18\text{ TR} \\ T_{liq} &= 50\text{ }^\circ\text{F} \\ \text{Max. } \Delta P &= 7\text{ psi} \\ T_{disch} &= 120\text{ }^\circ\text{F} \end{aligned}$$

The capacity table is based on nominal conditions ( $\Delta P = 3\text{ psi}$ ,  $T_{liq} = 90\text{ }^\circ\text{F}$ ,  $P_{disch} = 185\text{ psi}$ ,  $T_{disch} = 180\text{ }^\circ\text{F}$ ).

The actual capacity must therefore be corrected to a nominal condition by multiplication with correction factors.

Correction factor for  $\Delta P$  7 psi  $f_{\Delta P} = 0.67$ .

Correction factor for liquid temperature  $f_{T_{liq}} = 0.92$ .

Correction factor for  $T_{disch}$  120  $^\circ\text{F}$ ,  $f_{disch} = 0.95$ .

Correction factor for  $P_{disch}$  185 psi,  $f_{pdisch} = 1.0$ .

$$\begin{aligned} Q_n &= Q_o \times f_{\Delta P} \times f_{T_{liq}} \times f_{circ} \times f_{pdisch} \\ &= 18 \times 0.67 \times 0.92 \times 0.95 \times 1.0 = 10.5\text{ TR} \end{aligned}$$

From the capacity table a NRVA 15 with  $Q_n = 16.4\text{ TR}$  is the correct selection for the application.



## Check valves, type NRVA

### Nominal capacities

### Discharge line

## SI units

Capacity table for nominal conditions,  $Q_N$  [kW],

$T_{liq} = 30\text{ °C}$ ,  
 $P_{disch} = 12\text{ bar}$ ,  
 $\Delta P = 0.2\text{ bar}$ ,  
 $T_{disch} = 80\text{ °C}$

### R 717

Type	$k_v$ [m <sup>3</sup> /h]	Evaporating temperature $T_e$							
		-50 °C	-40 °C	-30 °C	-20 °C	-10 °C	0 °C	10 °C	20 °C
NRVA 15	5	53.9	54.8	55.5	56.3	56.9	57.5	58.0	58.4
NRVA 20	6	64.7	65.7	66.6	67.5	68.3	69.0	69.6	70.1
NRVA 25	19	205	208	211	214	216	218	220	222
NRVA 32	20	216	219	222	225	228	230	232	234
NRVA 40	44	475	482	489	495	501	506	510	514
NRVA 50	44	475	482	489	495	501	506	510	514
NRVA 65	75	809	821	833	844	854	862	870	876

Correction factor for discharge pressure ( $P_{disch}$ )

$P_{disch}$ (bar)	Correction factor
<b>12</b>	<b>1.00</b>
16	0.87
20	0.78

Correction factor for  $\Delta P$  ( $f_{\Delta P}$ )

$\Delta P$ (bar)	Correction factor
<b>0.2</b>	<b>1.00</b>
0.4	0.72
0.6	0.59
0.8	0.52
1	0.46
1.5	0.39
2	0.34
4	0.27

Correction factor for discharge temperature ( $T_{disch}$ )

Discharge temperature	Correction factor
50 °C	0.96
60 °C	0.97
<b>80 °C</b>	<b>1.00</b>
90 °C	1.01
100 °C	1.03
110 °C	1.04
120 °C	1.06

Correction factor for liquid temperature ( $T_{liq}$ )

Liquid temperature	Correction factor
-20 °C	0.82
-10 °C	0.86
0 °C	0.88
10 °C	0.92
20 °C	0.96
<b>30 °C</b>	<b>1.00</b>
40 °C	1.04
50 °C	1.09

## US units

Capacity table for nominal conditions,  $Q_N$  [Tons of Refrigeration],

$T_{liq} = 90\text{ °F}$ ,  
 $\Delta P = 3\text{ psi}$ ,  
 $P_{disch} = 185\text{ psi}$ ,  
 $T_{disch} = 180\text{ °F}$

### R 717

Type	$C_v$ [USgal/min]	Evaporating temperature $T_e$							
		-60 °F*	-40 °F	-20 °F	0 °F	20 °F	40 °F	60 °F	80 °F
NRVA 15	6	15.8	16.0	16.3	16.4	16.5	16.7	16.7	16.8
NRVA 20	7	19.0	19.2	19.5	19.7	19.8	20.1	20.1	20.2
NRVA 25	22	60.1	60.9	61.8	62.3	62.8	63.5	63.6	63.9
NRVA 32	23	63	64	65	66	66	67	67	67
NRVA 40	51	139	141	143	144	145	147	147	148
NRVA 50	51	139	141	143	144	145	147	147	148
NRVA 65	87	237	241	244	246	248	251	251	252

\* 2 °F below min. operating temperature.

Correction factor for discharge pressure ( $P_{disch}$ )

$P_{disch}$ (psi)	Correction factor
<b>185</b>	<b>1.00</b>
240	0.87
300	0.78

Correction factor for  $\Delta P$  ( $f_{\Delta P}$ )

$\Delta P$ (psi)	Correction factor
<b>3</b>	<b>1.00</b>
5	0.79
7	0.67
10	0.56
15	0.47
20	0.41
30	0.35
60	0.28

Correction factor for discharge temperature ( $T_{disch}$ )

Discharge temperature	Correction factor
120 °F	0.95
140 °F	0.97
<b>180 °F</b>	<b>1.00</b>
200 °F	1.02
210 °F	1.02
230 °F	1.04
250 °F	1.06

Correction factor for liquid temperature ( $T_{liq}$ )

Liquid temperature	Correction factor
-10 °F	0.82
10 °F	0.85
30 °F	0.88
50 °F	0.92
70 °F	0.96
<b>90 °F</b>	<b>1.00</b>
110 °F	1.04
130 °F	1.09

## Check valves, type NRVA

### Nominal capacities

### Discharge line

### SI units

Capacity table for nominal conditions,  $Q_N$  [kW],

$T_{liq} = 30\text{ °C}$ ,  
 $P_{disch} = 12\text{ bar}$ ,  
 $\Delta P = 0.2\text{ bar}$ ,  
 $T_{disch} = 80\text{ °C}$

### R 22

Type	$k_v$ [m <sup>3</sup> /h]	Evaporating temperature $T_e$							
		-50 °C	-40 °C	-30 °C	-20 °C	-10 °C	0 °C	10 °C	20 °C
NRVA 15	5	17.3	17.9	18.4	18.9	19.4	19.8	20	21
NRVA 20	6	21	21	22	23	23	24	24	25
NRVA 25	19	66	68	70	72	74	75	77	78
NRVA 32	20	69	71	74	76	78	79	81	82
NRVA 40	44	152	157	162	166	171	175	178	181
NRVA 50	44	152	157	162	166	171	175	178	181
NRVA 65	75	260	268	276	284	291	297	304	309

Correction factor for discharge pressure ( $P_{disch}$ )

$P_{disch}$ (bar)	Correction factor
<b>12</b>	<b>1.00</b>
16	0.87
20	0.78

Correction factor for  $\Delta P$  ( $f_{\Delta P}$ )

$\Delta P$ (bar)	Correction factor
<b>0.2</b>	<b>1.00</b>
0.4	0.72
0.6	0.59
0.8	0.52
1	0.46
1.5	0.39
2	0.34
4	0.27

Correction factor for discharge temperature ( $T_{disch}$ )

Discharge temperature	Correction factor
50 °C	0.96
60 °C	0.97
<b>80 °C</b>	<b>1.00</b>
90 °C	1.01
100 °C	1.03
110 °C	1.04
120 °C	1.06

Correction factor for liquid temperature ( $T_{liq}$ )

Liquid temperature	Correction factor
-20 °C	0.71
-10 °C	0.75
0 °C	0.80
10 °C	0.86
20 °C	0.92
<b>30 °C</b>	<b>1.00</b>
40 °C	1.09
50 °C	1.22

### US units

Capacity table for nominal conditions,  $Q_N$  [Tons of Refrigeration],

$T_{liq} = 90\text{ °F}$ ,  
 $\Delta P = 3\text{ psi}$ ,  
 $P_{disch} = 185\text{ psi}$ ,  
 $T_{disch} = 180\text{ °F}$

### R 22

Type	$C_v$ [USgal/min]	Evaporating temperature $T_e$							
		-60 °F*	-40 °F	-20 °F	0 °F	20 °F	40 °F	60 °F	80 °F
NRVA 15	6	5.0	5.1	5.3	5.5	5.6	5.8	5.9	6.0
NRVA 20	7	5.9	6.2	6.4	6.6	6.7	6.9	7.1	7.2
NRVA 25	22	18.8	19.5	20	21	21	22	22	23
NRVA 32	23	19.8	21	21	22	22	23	24	24
NRVA 40	51	44	45	47	48	49	51	52	53
NRVA 50	51	44	45	47	48	49	51	52	53
NRVA 65	87	74	77	79	82	84	86	88	90

\* 2 °F below min. operating temperature.

Correction factor for discharge pressure ( $P_{disch}$ )

$P_{disch}$ (psi)	Correction factor
<b>185</b>	<b>1.00</b>
240	0.87
300	0.78

Correction factor for  $\Delta P$  ( $f_{\Delta P}$ )

$\Delta P$ (psi)	Correction factor
<b>3</b>	<b>1.00</b>
5	0.79
7	0.67
10	0.56
15	0.47
20	0.41
30	0.35
60	0.28

Correction factor for discharge temperature ( $T_{disch}$ )

Discharge temperature	Correction factor
120 °F	0.95
140 °F	0.97
<b>180 °F</b>	<b>1.00</b>
200 °F	1.02
210 °F	1.02
230 °F	1.04
250 °F	1.06

Correction factor for liquid temperature ( $T_{liq}$ )

Liquid temperature	Correction factor
-10 °F	0.73
10 °F	0.77
30 °F	0.82
50 °F	0.87
70 °F	0.93
<b>90 °F</b>	<b>1.00</b>
110 °F	1.09
130 °F	1.20

## Check valves, type NRVA

### Nominal capacities

### Discharge line

### SI units

Capacity table for nominal conditions,  $Q_N$  [kW],

$T_{liq} = 30\text{ °C}$ ,  
 $P_{disch.} = 12\text{ bar}$ ,  
 $\Delta P = 0.2\text{ bar}$ ,  
 $T_{disch.} = 80\text{ °C}$

### R 134a

Type	$k_v$ [m <sup>3</sup> /h]	Evaporating temperature $T_e$						
		-40 °C	-30 °C	-20 °C	-10 °C	0 °C	10 °C	20 °C
NRVA 15	5	13.5	14.2	14.8	15.4	16.0	16.6	17.2
NRVA 20	6	16.2	17.0	17.7	18.5	19.2	19.9	21
NRVA 25	19	51	54	56	59	61	63	65
NRVA 32	20	54	57	59	62	64	66	69
NRVA 40	44	119	125	130	136	141	146	151
NRVA 50	44	119	125	130	136	141	146	151
NRVA 65	75	203	212	222	231	240	249	257

Correction factor for discharge pressure ( $P_{disch}$ )

$P_{disch}$ (bar)	Correction factor
<b>8</b>	<b>1.00</b>
12	0.82
16	0.70
20	0.62

Correction factor for  $\Delta P$  ( $f_{\Delta P}$ )

$\Delta P$ (bar)	Correction factor
<b>0.2</b>	<b>1.00</b>
0.4	0.72
0.6	0.59
0.8	0.52
1	0.46
1.5	0.39
2	0.34
4	0.27

Correction factor for discharge temperature ( $T_{disch}$ )

Discharge temperature	Correction factor
50 °C	0.96
60 °C	0.97
<b>80 °C</b>	<b>1.00</b>
90 °C	1.01
100 °C	1.03
110 °C	1.04
120 °C	1.06

Correction factor for liquid temperature ( $T_{liq}$ )

Liquid temperature	Correction factor
-20 °C	0.66
-10 °C	0.70
0 °C	0.76
10 °C	0.82
20 °C	0.90
<b>30 °C</b>	<b>1.00</b>
40 °C	1.13
50 °C	1.29

### US units

Capacity table for nominal conditions,  $Q_N$  [Tons of Refrigeration],

$T_{liq} = 90\text{ °F}$ ,  
 $\Delta P = 3\text{ psi}$ ,  
 $P_{disch.} = 185\text{ psi}$ ,  
 $T_{disch.} = 180\text{ °F}$

### R 134a

Type	$C_v$ [USgal/min]	Evaporating temperature $T_e$						
		-40 °F	-20 °F	0 °F	20 °F	40 °F	60 °F	80 °F
NRVA 15	6	3.9	4.1	4.4	4.6	4.7	5.0	5.1
NRVA 20	7	4.7	5.0	5.2	5.5	5.7	5.9	6.2
NRVA 25	22	14.9	15.7	16.5	17.3	18.0	18.8	19.5
NRVA 32	23	15.7	16.6	17.4	18.2	19.0	19.8	21
NRVA 40	51	35	36	38	40	42	44	45
NRVA 50	51	35	36	38	40	42	44	45
NRVA 65	87	59	62	65	68	71	74	77

\* 2 °F below min. operating temperature.

Correction factor for discharge pressure ( $P_{disch}$ )

$P_{disch}$ (psi)	Correction factor
<b>120</b>	<b>1.00</b>
185	0.83
240	0.71
300	0.64

Correction factor for  $\Delta P$  ( $f_{\Delta P}$ )

$\Delta P$ (psi)	Correction factor
<b>3</b>	<b>1.00</b>
5	0.79
7	0.67
10	0.56
15	0.47
20	0.41
30	0.35
60	0.28

Correction factor for discharge temperature ( $T_{disch}$ )

Discharge temperature	Correction factor
120 °F	0.95
140 °F	0.97
<b>180 °F</b>	<b>1.00</b>
200 °F	1.02
210 °F	1.02
230 °F	1.04
250 °F	1.05

Correction factor for liquid temperature ( $T_{liq}$ )

Liquid temperature	Correction factor
-10 °F	0.64
10 °F	0.68
30 °F	0.74
50 °F	0.81
70 °F	0.89
<b>90 °F</b>	<b>1.00</b>
110 °F	1.15
130 °F	1.35

## Check valves, type NRVA

### Nominal capacities

### Discharge line

### SI units

Capacity table for nominal conditions,  $Q_N$  [kW],

$T_{liq} = 30\text{ °C}$ ,  
 $P_{disch.} = 12\text{ bar}$ ,  
 $\Delta P = 0.2\text{ bar}$ ,  
 $T_{disch.} = 80\text{ °C}$

### R 404A

Type	$k_v$ [m <sup>3</sup> /h]	Evaporating temperature $T_e$							
		-50 °C	-40 °C	-30 °C	-20 °C	-10 °C	0 °C	10 °C	20 °C
NRVA 15	5	12.6	13.5	14.4	15.3	16.1	16.9	17.6	18.3
NRVA 20	6	15.2	16.2	17.3	18.4	19.4	20.3	21.2	22.0
NRVA 25	19	48.0	51.5	54.8	58.1	61.3	64.3	67.0	69.5
NRVA 32	20	50.6	54.2	57.7	61.2	64.5	67.7	70.6	73.2
NRVA 40	44	111.3	119.2	127.0	134.6	141.9	148.9	155.3	161.0
NRVA 50	44	111.3	119.2	127.0	134.6	141.9	148.9	155.3	161.0
NRVA 65	75	189.7	203.1	216.4	229.4	241.9	253.7	264.7	274.4

Correction factor for discharge pressure ( $P_{disch.}$ )

$P_{disch.}$ (bar)	Correction factor
12	1
16	0.87
20	0.78

Correction factor for  $\Delta P$  ( $f_{\Delta P}$ )

$\Delta P$ (bar)	Correction factor
0.2	1.00
0.4	0.72
0.6	0.59
0.8	0.52
1	0.46
1.5	0.39
2	0.34
4	0.27

Correction factor for discharge temperature ( $T_{disch.}$ )

Discharge temperature	Correction factor
50 °C	0.96
60 °C	0.97
80 °C	1.00
90 °C	1.01
100 °C	1.03
110 °C	1.04
120 °C	1.06

Correction factor for liquid temperature ( $T_{liq.}$ )

Liquid temperature	Correction factor
-20 °C	0.55
-10 °C	0.60
0 °C	0.66
10 °C	0.74
20 °C	0.85
30 °C	1.00
40 °C	1.23
50 °C	1.68

### US units

Capacity table for nominal conditions,  $Q_N$  [Tons of Refrigeration],

$T_{liq} = 90\text{ °F}$ ,  
 $\Delta P = 3\text{ psi}$ ,  
 $P_{disch.} = 185\text{ psi}$ ,  
 $T_{disch.} = 180\text{ °F}$

### R 404A

Type	$C_v$ [USgal/min]	Evaporating temperature $T_e$							
		-60 °F*	-40 °F	-20 °F	0 °F	20 °F	40 °F	60 °F	80 °F
NRVA 15	6	3.5	3.8	4.0	4.3	4.6	4.8	5.1	5.3
NRVA 20	7	4.2	4.5	4.9	5.2	5.5	5.8	6.1	6.3
NRVA 25	22	13.2	14.3	15.4	16.4	17.4	18.3	19.3	20.0
NRVA 32	23	13.9	15.1	16.2	17.3	18.3	19.3	20.3	21.0
NRVA 40	51	30.7	33.2	35.6	38.0	40.3	42.5	44.6	46.2
NRVA 50	51	30.7	33.2	35.6	38.0	40.3	42.5	44.6	46.2
NRVA 65	87	52.2	56.5	60.7	64.8	68.7	72.4	76.0	78.8

\* 2 °F below min. operating temperature.

Correction factor for discharge pressure ( $P_{disch.}$ )

$P_{disch.}$ (psi)	Correction factor
185	1
240	0.87
300	0.78

Correction factor for  $\Delta P$  ( $f_{\Delta P}$ )

$\Delta P$ (psi)	Correction factor
3	1.00
5	0.79
7	0.67
10	0.56
15	0.47
20	0.41
30	0.35
60	0.28

Correction factor for discharge temperature ( $T_{disch.}$ )

Discharge temperature	Correction factor
120 °F	0.95
140 °F	0.97
180 °F	1.00
200 °F	1.02
210 °F	1.02
230 °F	1.04
250 °F	1.05

Correction factor for liquid temperature ( $T_{liq.}$ )

Liquid temperature	Correction factor
-10 °F	0.52
10 °F	0.57
30 °F	0.63
50 °F	0.72
70 °F	0.83
90 °F	1.00
110 °F	1.29
130 °F	1.92

# Check valve

## Type NRVS

### Contents

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## Check valve

### Type NRVS



Check valve type NRVS has no damping feature and therefore can only be used for liquid line applications. NRVS is designed to be mounted directly to PM or solenoid valves EVRA / EVRAT.

#### Features

- Ensures correct direction of flow
- Applicable to HCFC, HFC and R717 (Ammonia)
- Classification: DNV, CRN, BV, EAC etc.  
To get an updated list of certification on the products please contact your local Danfoss Sales Company

#### Technical data

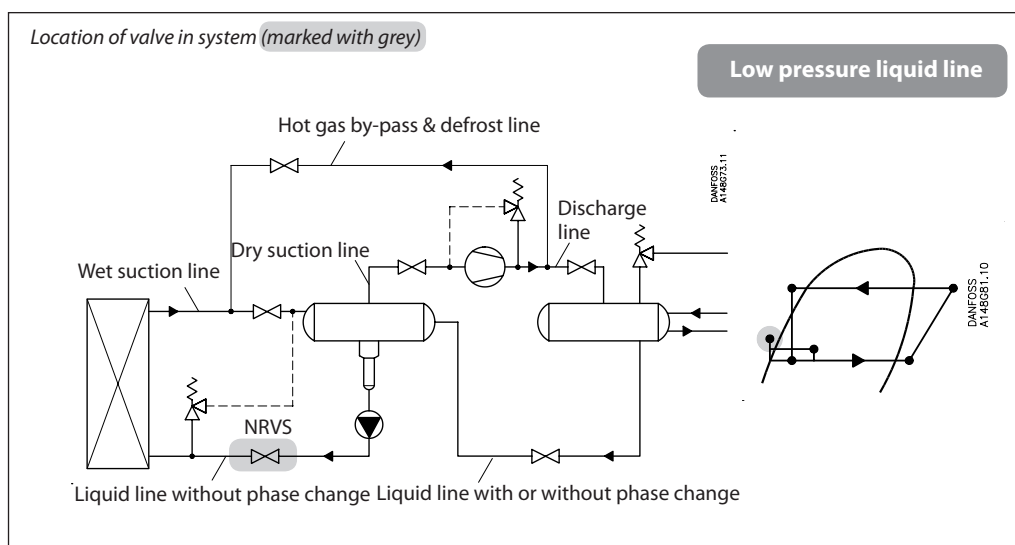
- Temperature of medium:  
-50 °C – 140 °C
- Maximum working pressure:  
PS = 28 bar / 406 psig

#### Materials

- Valve housing made of Stainless Steel
- Gaskets are non-asbestos

## Check valve, type NRVS

### Capacities



Valve combination	EVRA/EVRAT 10 + NRVS 15	EVRA/EVRAT 15 + NRVS 15	EVRA/EVRAT 20 + NRVS 25	EVRA + NRVS 25
$k_v$ [m <sup>3</sup> /h]	1.4	2.2	4.1	7.0

Evaporating temperature $T_e$	Pressure $\Delta p$ [bar]	Capacities (kW) $Q_0$ at circulation rate 1 R717			
-40 °C	0.15	172	270	504	960
	0.25	222	349	650	1110
	0.30	243	382	713	1216
	0.40	281	441	823	1405
	0.50	314	493	920	1570
-30 °C	0.15	167	262	489	835
	0.25	215	338	631	1078
	0.30	236	371	691	1180
	0.40	273	428	798	1363
	0.50	305	479	893	1524
-20 °C	0.15	161	254	473	808
	0.25	208	327	610	1042
	0.30	228	359	669	1142
	0.40	264	414	772	1319
	0.50	295	463	863	1475
-10 °C	0.15	156	245	456	780
	0.25	201	316	589	1005
	0.30	220	346	645	1102
	0.40	254	399	745	1271
	0.50	284	447	833	1422

Note: The capacities in the table must be divided by the actual circulation rate, or the evaporator capacities must be multiplied with the actual circulation rate.

Minimum opening differential pressure:

EVRA/EVRAT 10 – 20 + NRVS	0.07 bar
EVRA/EVRAT 25 + NRVS	0.11 bar

#### Example

An application has the following operating conditions:

Refrigerant: ..... R717  
 Evaporating temperature: ..... -30 °C  
 Evaporator capacity ( $Q_0$ ): ..... 290 kW  
 Circulation rate: ..... 4  
 $\Delta p \leq 0.3$  bar

#### Solution

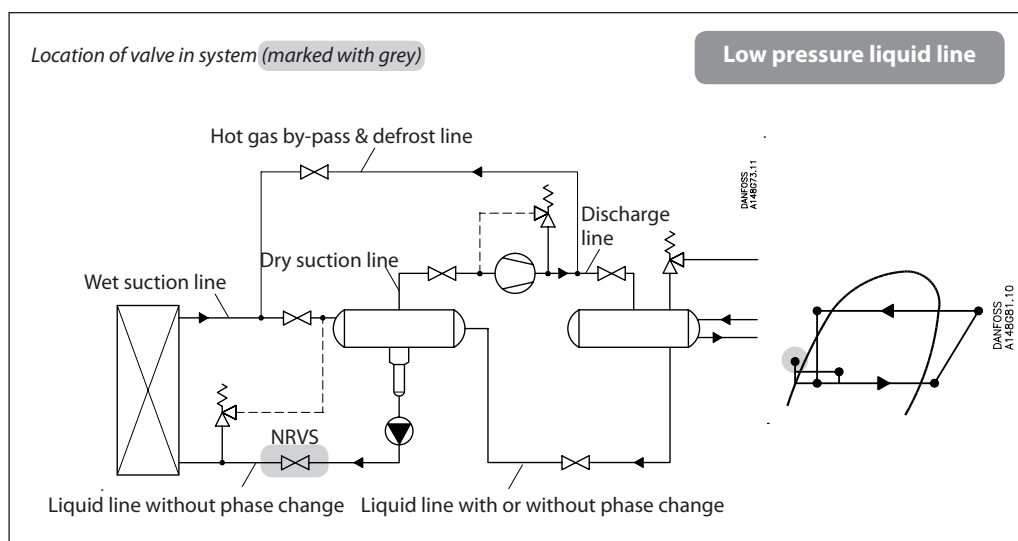
$290 \times 4 = 1160$  kW  
 EVRAT 25 + NRVS 25:  $Q_0 = 1180$  kW, at  
 $\Delta p = 0.3$  bar is chosen.

Precise valve capacities can be calculated for various refrigerants by using the "DIRcalc™" (Danfoss Industrial Refrigeration calculation programme).



## Check valve, type NRVS

### Capacities (continued)



Valve combination	PM 15	PM 20	PM 25
	NRVS 25	NRVS 25	NRVS 25
$k_v$ [m <sup>3</sup> /h]	4.0	6.0	7.5

Evaporating temperature $T_e$	Pressure $\Delta p$ (bar)	Capacities (kW) $Q_0$ at circulation rate 1 R717		
-50 °C	0.15	–	–	–
	0.25	653	979	1224
	0.30	715	1072	1340
	0.40	825	1238	1547
	0.50	923	1384	1730
-40 °C	0.15	–	–	–
	0.25	635	951	1188
	0.30	695	1043	1303
	0.40	803	1204	1506
	0.50	897	1346	1683
-30 °C	0.15	–	–	–
	0.25	615	922	1152
	0.30	675	1011	1265
	0.40	779	1169	1460
	0.50	871	1306	1632
-20 °C	0.15	–	–	–
	0.25	595	894	1114
	0.30	653	979	1224
	0.40	753	1130	1412
	0.50	852	1264	1580
-10 °C	0.15	–	–	–
	0.25	575	862	1075
	0.30	629	944	1180
	0.40	727	1090	1362
	0.50	812	1219	1523

Note: The capacities in the table must be divided by the actual circulation rate, or the evaporator capacities must be multiplied with the actual circulation rate.

*Minimum opening differential pressure:*  
PM + NRVS will be fully open at  $\Delta p = 0.25$  bar.

Precise valve capacities can be calculated for various refrigerants by using the "DIRcalc™" (Danfoss Industrial Refrigeration calculation programme).

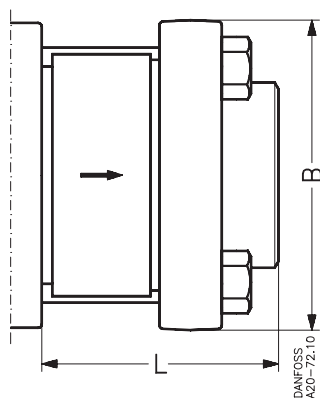
**Ordering**

Check valve				Flanges, gasket and bolts <sup>1)</sup>		
Valve type	Code. no.	For valve type	Code no.	Weight <sup>2)</sup> [kg]	Flange type	Connection size
NRVS 15	<b>020-2032</b>	EVRA / T 10, EVRA / T 15	<b>027N1255</b>	0.7		¾ in
NRVS 25	<b>020-2033</b>	EVRA / T 20, EVRA / T 25, PM 15, PM 20, PM 25	<b>027N1254</b>	1.1		1 in
			Flanges, gaskets and bolts for NRVS stand alone <sup>3)</sup>			
			<b>Code no.</b>	<b>Weight<sup>2)</sup> [kg]</b>	<b>Flange type</b>	<b>Connection size</b>
			<b>027N1256</b>	0.256		¾ in
			<b>027N1257</b>	0.443		1 in

- <sup>1)</sup> Consists of one standard and one special flange, one gasket and 2 bolts.
- <sup>2)</sup> Flange and bolts only.
- <sup>3)</sup> Consist of flanges, gaskets, bolts and nuts only.  
One standard flange and one special flange, two gasket, 2 bolts and 2 nuts.

**Dimensions and weights**

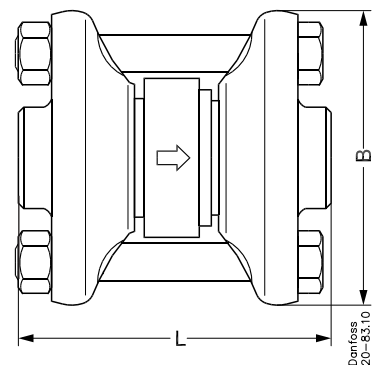
NRVS on valve



Type	L [mm]	B [mm]	Weight <sup>1)</sup> kg
NRVS 15	47.5	78.0	0.1
NRVS 25	60.5	96.0	0.25

<sup>1)</sup> NRVS without flanges and bolts

NRVS stand alone



Type	L [mm]	B [mm]	Weight <sup>1)</sup> kg
NRVS 15	78	80	0.1
NRVS 25	98	96	0.25

<sup>1)</sup> NRVS without flanges and bolts

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